

Article

Statistics of Heat Transfer in Two-Dimensional Turbulent Rayleigh-Bénard Convection at Various Prandtl Number

Hui Yang ^{1,2} , Yikun Wei ^{1,2,*}, Zuchao Zhu ^{1,2}, Huashu Dou ^{1,2} and Yuehong Qian ³

¹ Faculty of Mechanical Engineering and Automation, Zhejiang Sci-Tech University, Hangzhou 310018, China; yanghui@zstu.edu.cn (H.Y.); zhuzuchao@zstu.edu.cn (Z.Z.); huashudou@zstu.edu.cn (H.D.)

² State-Province Joint Engineering Lab of Fluid Transmission System Technology, Hangzhou 310018, China

³ School of Mathematic Science, Soochow University, Suzhou 215006, China; yuehongqian@suda.edu.cn

* Correspondence: yikunwei@zstu.edu.cn; Tel.: +86-0571-8684-3661

Received: 22 June 2018; Accepted: 6 August 2018; Published: 7 August 2018



Abstract: Statistics of heat transfer in two-dimensional (2D) turbulent Rayleigh-Bénard (RB) convection for $Pr = 6, 20, 100$ and 10^6 are investigated using the lattice Boltzmann method (LBM). Our results reveal that the large scale circulation is gradually broken up into small scale structures plumes with the increase of Pr , the large scale circulation disappears with increasing Pr , and a great deal of smaller thermal plumes vertically rise and fall from the bottom to top walls. It is further indicated that vertical motion of various plumes gradually plays main role with increasing Pr . In addition, our analysis also shows that the thermal dissipation is distributed mainly in the position of high temperature gradient, the thermal dissipation rate ε_θ already increasingly plays a dominant position in the thermal transport, ε_u can have no effect with increase of Pr . The kinematic viscosity dissipation rate and the thermal dissipation rate gradually decrease with increasing Pr . The energy spectrum significantly decreases with the increase of Pr . A scope of linear scaling arises in the second order velocity structure functions, the temperature structure function and mixed structure function (temperature-velocity). The value of linear scaling and the 2nd-order velocity decrease with increasing Pr , which is qualitatively consistent with the theoretical predictions.

Keywords: thermal dissipation rate; turbulence; Prandtl number; lattice Boltzmann method

1. Introduction

Thermal convection generally occurs in natural world and industrial field. Hartmann et al. 2001 [1] argued that for weather predictions the flow of atmosphere and thermal convection flow are not only related with smaller length scales and time scales, but also is closely greater scales for climate forecast. Marshall et al. (1999) [2] have investigated a key enforcing mechanical properties of ocean circulation in the ocean. Cardin and Olson (1994) [3] have studied that the enforced convection arises in the earth outer core. In general, the effect of rotation, the changing phases, complex boundary conditions and nonlinear dynamic can play a main role in many thermal convections. Lohse and Xia (2010) [4] and Chilla and Schumacher (2012) [5] respectively introduced research processes for turbulent RB convection. Turbulent RB convection is the most common phenomenon in natural convection [6]. Scheel et al. [7] presented the direct numerical calculations in a cylinder, which mainly focuses on the optimal scales of turbulent convective, especially, the analysis of the kinetic energy rates and thermal dissipation rates in the whole cell [7]. Hu [8] argued that the critical Ra (Rayleigh number) decreases for the beginning of convection, and the aspect ratio effects the critical value with increasing density inversion parameter in RB convection. Zhang [9] have studied the topic of the buoyancy ratio enhancing the fluid stability, and the critical Ra also gradually enhances with increasing

value of the buoyant force ratio in thermal convection. Turbulent RB convection [10–19] has been studied numerically, experimentally and analytically. Shishkina [15] reported that massive thermal plumes rising in turbulent RB convection are analysed on account of 3D numerical calculations, which indicates that the thermal boundary layers are crucial to the temperature fields and velocity fields.

In RB convection, the Ra (a measure of the buoyant force), and the Prandtl number $Pr = \nu/\kappa$ (the kinematic viscosity divides the thermal diffusivity) are important dimensionless numbers. Krishnamurti [20,21] performed extensive convection experiments on mercury ($Pr \sim 0.02$), air ($Pr \sim 0.7$), water ($Pr \sim 6.8$), freon ($Pr \sim 7$), and silicon oil ($Pr \sim 100$). Busse and Whitehead [22] also reported the jagged instability and cross-roll instability of silicon oil in experiment, which indicated that the results of two-dimensional (2D) convection are closely similar to that of 3D convection for large Pr convection [10,11].

This survey to investigate the bifurcation and chaos in convection with large Pr and different Pr using a low-dimensional model containing is exploited in this paper. The main purpose of our paper is to offer ‘reference’ cases for comparison with a host of various flows. In general, the laboratory experiments are performed by using fluids with Pr up to 10^4 behave. However, a similar flow for infinite Pr does not exist. Although a model of a plume is not investigated in the Earth’s mantle, the flow possessing overwhelmingly large Pr is close to the mantle investigations since the mantle possesses a Pr of 10^6 . Our results mainly appraise the variety of physical mechanism phenomenon about the kinematic viscosity dissipation, thermal dissipation, energy spectra, temperature spectra and the 2nd structure function with increasing Pr at the same Ra . Our studies mainly focus on the characteristics of the above physical mechanism phenomena with increasing Pr , the characteristics of flow and scale properties in turbulent RB system at large Prandtl number. In addition, the Bolgiano-Obukhov-like (BO59) scaling is used to explore the profound insight of the velocity fluctuation and the temperature fluctuation with the increase of Pr in turbulent RB convection.

The lattice Boltzmann scheme is performed to simulate in all numerical examples. The lattice Boltzmann method (LBM) had possessed latent advantages in previous studies to multiphase, single, heat and mass transfer hydrodynamic problems [23–36]. The LBM is particularly propitious to attack complex boundary conditions. It is a attractive topic that the turbulent flows are simulated by the LBM [28]. The LBM on account of Direct Numerical Simulations (DNS), Large Eddy Simulations (LES) also possess great success in turbulence predictions [34]. In general, in turbulent RB convection, Rayleigh number (Ra) is a very important dimensionless parameter. When Ra is less than 10^6 , the flow state is laminar RB convection. When Ra is between 10^6 and 10^9 , the flow state is soft turbulent RB convection. However, when Ra is greater than 10^9 , the flow state is full turbulent RB convection.

The main structure of the paper is introduced. Firstly, a thermal lattice Boltzmann model is introduced. Secondly, the numerical verifications are presented. Thirdly, the result analysis and discussions are provided. Finally, some conclusions are provided.

2. Mathematical Equation of Fluid and Lattice Boltzmann Method

The discrete kinetic model is based on LBM. A double-population approach using the lattice Boltzmann equation is proposed by Shan [35]. The lattice Boltzmann equation of computing dynamics and the lattice Boltzmann equation of computing advection equation are described by the following expressions, correspondingly [26,32]:

$$f_i(x_\alpha + c_{i\alpha}\delta t, t + \delta t) - f_i(x_\alpha, t) = -\omega_1 \left[f_i(x_\alpha, t) - f_i^{(eq)}(x_\alpha, t) \right] + F_i \quad (1)$$

$$g_i(x_\alpha + c_{i\alpha}\delta t, t + \delta t) - g_i(x_\alpha, t) = -\omega_2 \left[g_i(x_\alpha, t) - g_i^{(eq)}(x_\alpha, t) \right] \quad (2)$$

where f_i, g_i denote the probability density functions at (x, t) , c_i belongs to a discrete velocity, F_i is the mesoscopic buoyant body force, ω_1 is the flow relaxation time and ω_2 is the temperature relaxation

time in the above equations, respectively. The local kinetic equilibrium f_i^{eq} is equilibrium function for flow, and g_i^{eq} is the equilibrium function for temperature [32].

$$f_i^{eq}(x_\alpha, t) = w_i \rho \left\{ 1 + \frac{c_{i\alpha} u_\alpha}{c_s^2} + \frac{u_\alpha u_\beta}{2c_s^2} \left(\frac{c_{i\alpha} c_{i\beta}}{c_s^2} - \delta_{\alpha\beta} \right) \right\} \tag{3}$$

$$g_i^{eq}(x_\alpha, t) = w_i \theta \left\{ 1 + \frac{c_{i\alpha} u_\alpha}{c_s^2} + \frac{u_\alpha u_\beta}{2c_s^2} \left(\frac{c_{i\alpha} c_{i\beta}}{c_s^2} - \delta_{\alpha\beta} \right) \right\} \tag{4}$$

where c_s is the sound speed and w_i denotes the weight coefficients.

$$c_s = \frac{1}{\sqrt{3}} \frac{\delta x}{\delta t}, \quad w_i = \begin{cases} \frac{4}{9} & i = 0 \\ \frac{1}{9} & i = 1 \sim 4 \\ \frac{1}{36} & i = 5 \sim 8 \end{cases} \tag{5}$$

The relation between the relaxation parameter ω_1 and the kinematic viscosity ν is presented and the relaxation is also presented between the parameter ω_2 and the fluid thermal diffusivity κ .

$$\nu = c_s^2 \left(\frac{1}{\omega_1} - \frac{1}{2} \right) \delta t, \quad \kappa = c_s^2 \left(\frac{1}{\omega_2} - \frac{1}{2} \right) \delta t \tag{6}$$

The mesoscopic buoyant body force with the Boussinesq approximation is formulated by the following equation

$$F_i = 3w_i \rho g \theta \beta c_{i\alpha} \tag{7}$$

in which g denotes the gravity acceleration, β denotes the coefficient of thermal expansion, and $c_{i\alpha}$ denotes the y -component of c_i correspondingly.

The relations are defined as coarse-grained (in velocity space) fields of the distribution functions for the macroscopical density, momentum, and temperature, which are given by

$$\rho = \sum_i f_i, \quad \rho u_\alpha = \sum_i f_i c_{i\alpha}, \quad \theta = \sum_i g_i \tag{8}$$

The Equations (1) and (2) are respectively expanded by a Chapman-Enskog approach, which leads to the macroscopical equations of fluid. The inertial terms are reproduced by the streaming step on the left-hand side in the hydrodynamical equations, whereas the kinematic viscosity coefficient and the coefficient of thermal diffusion are respectively connected to the relaxation (towards equilibrium) properties in the right hand side.

$$\partial_t \rho + \partial_\alpha (\rho u_\alpha) = 0 \tag{9}$$

$$\partial_t (\rho u_\alpha) + \partial_\beta (\rho u_\alpha u_\beta) = -\partial_\alpha (P) + \partial_\beta (2\rho \nu S_{\alpha\beta}) - g \beta \Delta \theta \tag{10}$$

$$\partial_t (\theta) + u_\alpha \partial_\alpha (\theta) = \kappa \partial_\alpha \partial_\beta (\theta) \tag{11}$$

The Ra is an important variable in the natural convection. The definition of Ra is

$$Ra = \frac{\beta \Delta \theta g H^3}{\nu \kappa} \tag{12}$$

in which ν is the kinematic viscosity, κ is the thermal diffusivity and β is the coefficient of isobaric thermal expansion, $\Delta \theta$ is the temperature difference between the bottom boundary and top boundary in cavity, g is the gravity acceleration, and H is the height of cavity.

The perturbed is given in the initial stage of simulation. Once RB convection is taken shape, the heat transfer near wall is overwhelmingly strengthened. The Nusselt number denotes the enhancement of the heat transfer. The expression of Nu is presented in our simulations.

$$Nu = 1 + \frac{\langle u_y \theta \rangle}{(\kappa \Delta \theta / H)} \quad (13)$$

in which u_y denotes the vertical velocity and $\langle \rangle$ is the spatial average in the whole flow domain.

3. Calculation Results and Discussions

In the present study, numerical calculations in 2D turbulent RB convection for $Pr = 6, 20, 100$ and 10^6 are carried out at $Ra = 5.4 \times 10^9$. The computing grid is set to 2012×2012 . The no-slip boundary condition is performed on top boundary and on the bottom boundary. And left and right boundary conditions are also performed by the no-slip boundary condition in all numerical calculations. The initial dimensionless temperature in bottom boundary is 1, and the initial dimensionless temperature of top boundary is 0, respectively. Meanwhile, a linear distribution of the dimensionless temperature from 0 to 1 is performed between top boundary and bottom boundary.

The budget relation of instantaneous kinetic energy is used to test and verify the accuracy of the numerical calculations.

$$-\frac{dP(t)}{dt} = \frac{dE(t)}{dt} + \varepsilon(t) \quad (14)$$

where $P(t) = -\beta g \iint y \theta(x, y, t) dx dy$ is the total potential energy, $E(t) = \iint 0.5[u(x, y, t)^2 + v(x, y, t)^2] dx dy$ denotes the total kinetic energy and $\varepsilon(t) = \iint \nu [\partial_i u_j(x, y, t)]^2 dx dy$ denotes the dissipation rate of total kinetic energy. The ratio of the right-hand side to the left-hand side of Equation (14) as a relation of the normalized time t/τ is presented in Figure 1. One can see that the difference within only 0.6% at all times is achieved at the energy balance equation, which is indicated that the accuracy of LBM is reliable.

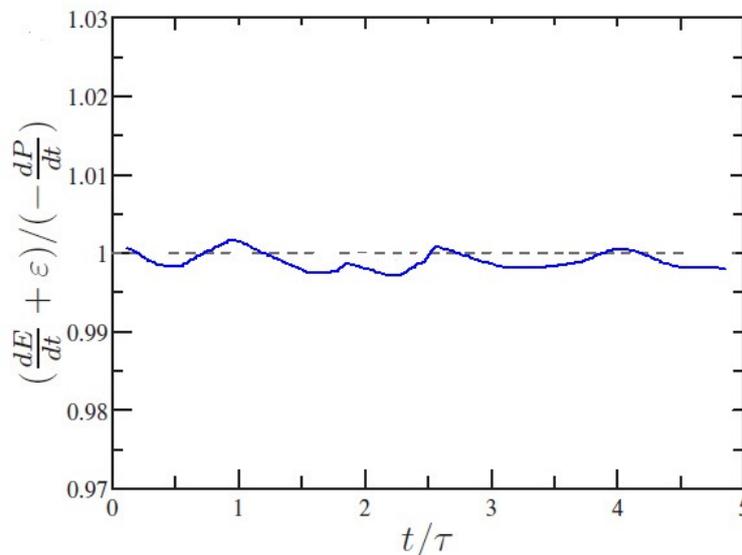


Figure 1. Validation of the energy balance relation (14) for the LBM scheme.

3.1. Global Quantities of Turbulent RB Convection

In Figure 2, the temperature distribution with superimposed temperature fields at $Pr = 6, 20, 100, 10^6$ (from a to d), and $Ra = 5.4 \times 10^9$ is displayed for several elective coarseness types, where is the flow characteristic of RB convection system, the blue regions denote cold fluid, and the red regions correspond

to hot fluid. One can see that large-scale circulations are obtained in the center of the cavity at $Pr = 6$. A large number of thermal plumes are predominantly rising in corners of the cavity, and the cold plumes are falling in corners of the cavity, which can be main reason owing to a large scale circulation that is guided along one of diagonals of the cavity. It is demonstrated that large-scale circulations of the fluid in cavity are decomposed gradually with the increase of Pr , which is consistent with the experiment for large Pr [4]. It is also showed that vertical motion of various plumes gradually plays main role with increasing Pr . Respectively, a large number of small-scale thermal plumes vertically rise from the bottom wall to top wall, a large number of small-scale cold plumes vertically fall from the top boundary to the bottom boundary, and a great number of small eddies appear at $Pr = 10^6$. The longitudinal velocity play a predominant role in cavity with increasing Pr . It is further found that the average time of achieving steady-state increase overwhelmingly with increasing Pr .

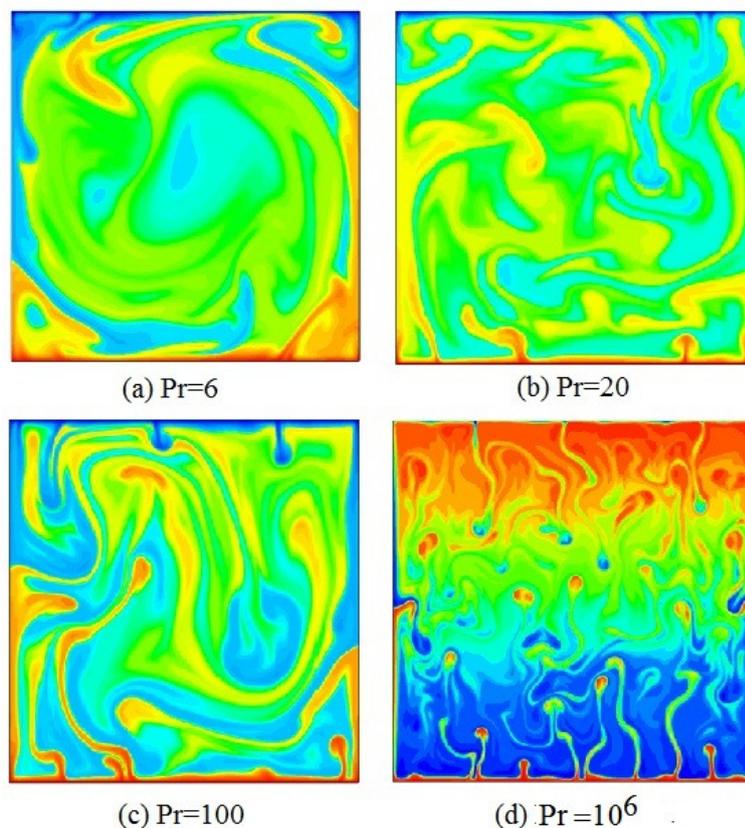


Figure 2. Temperature distributions with steady flow at $Pr = 6, 20, 100, 10^6$ (a–d), and $Ra = 5.4 \times 10^9$.

In the following section, Grossmann -Lohse theory for is used to investigate the dissipation rate of kinetic-energy rate and the thermal dissipation rate, which is the following equations [6]

$$\varepsilon_u(t) = \langle v[\partial u_i(x, y, t)]^2 \rangle_V = \frac{\nu^3}{L^4} (Nu - 1) Ra Pr^{-2} \quad (15)$$

$$\varepsilon_\theta(t) = \langle \kappa[\partial \theta_i(x, y, t)]^2 \rangle_V = \kappa \frac{\Delta^2 \theta}{L^2} Nu \quad (16)$$

The relations of Equations (15) and (16) are able to be derived from the Boussinesq equations [6].

The distributions of kinetic-energy dissipation rate at $Pr = 6, 20, 100, 10^6$ (from a to d), and $Ra = 5.4 \times 10^9$ are shown in Figure 3. It is shown that the value of kinetic-energy dissipation rate decreases with the increase of Pr in cavity. The kinetic-energy dissipation rate at $Pr = 6$ plays a major

role around cavity. The kinetic-energy dissipation rate is occupied gradually in the interior of cavity with increasing Pr . The kinetic-energy dissipation rate becomes gradually dispersed at $Pr = 10^6$.

The distributions of thermal dissipation rate at $Pr = 6, 20, 100, 10^6$ (from a to d) are shown in Figure 4, respectively. One can see that the value of thermal dissipation rate also decreases with the increase of Pr in cavity. The thermal dissipation rate at $Pr = 6$ plays a major role around cavity, similarly. The thermal dissipation rate gradually expands in the interior of cavity with increasing Pr . A large number of thermal dissipation emerge in the whole domain at $Pr = 10^6$. From a detailed comparison of Figure 3 with Figure 4, we can see that the thermal dissipation is distributed mainly in the position of high temperature gradient. In other word, the intense thermal dissipation events mainly concentrate on the interfaces of hot and cold fluids and these interfaces between the hot fluid and the cold fluid develop to complex associate structures with large intricate.

Figures 5 and 6 display the mean vertical dissipation rate profiles of kinetic-energy $\langle \varepsilon_u \rangle_x$ and the mean vertical thermal dissipation rate profiles $\langle \varepsilon_\theta \rangle_x$ for $Pr = 6, 20, 100, 10^6$, respectively, where $\langle \dots \rangle_x$ represents a horizontal average. As observed in Figures 5 and 6, the mean vertical dissipation rate profiles of kinetic-energy and the mean vertical thermal dissipation rate profiles significantly decrease with increasing Pr . The strong dissipation events mainly arises near the top and bottom boundary in the turbulent range. It is further seen that the thermal dissipation rate ε_θ already plays a key role in the thermal energy transport, thus ε_u may be neglected in virtue of inverse cascade of kinetic energy in thermal convection.

The contrast of the temperature on the midline ($y = H/2$) at $Pr = 6, 20, 100, 10^6$, and $Ra = 5.4 \times 10^9$ is displayed in Figure 7. Plotted in Figure 7, it is noted that the relative magnitude of temperature difference is increased overwhelmingly with increasing Pr , and the variety of temperature is also enhanced drastically.

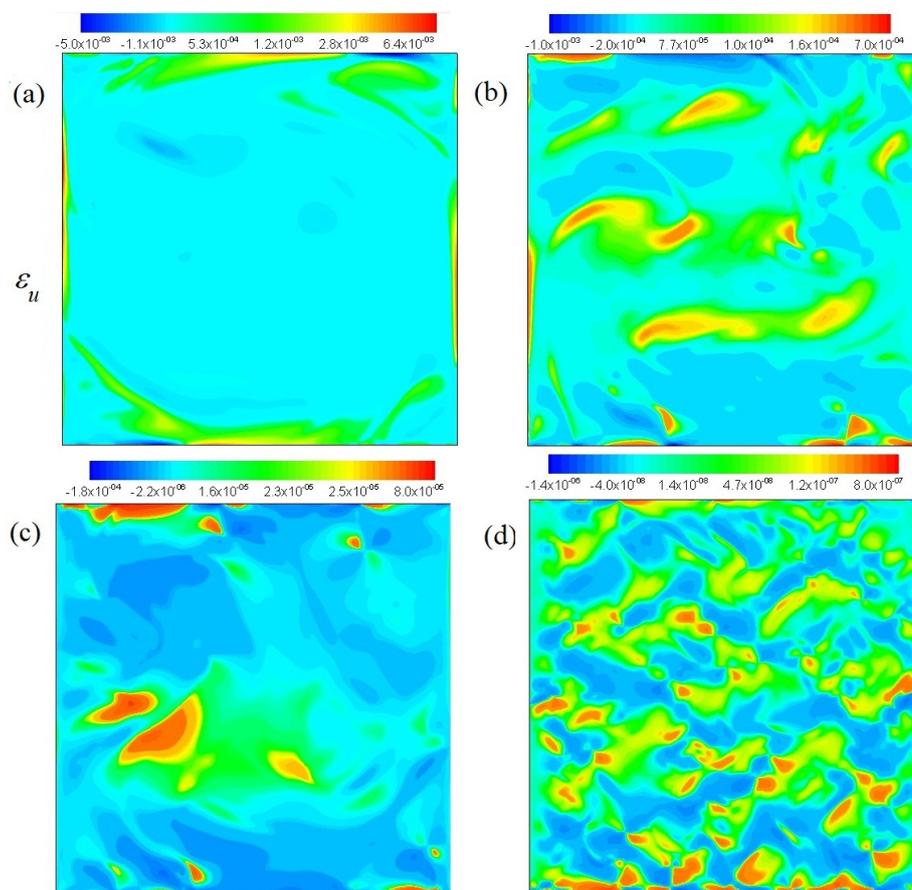


Figure 3. Kinetic energy dissipation rates $Pr = 6, 20, 100, 10^6$ (a–d), and $Ra = 5.4 \times 10^9$.

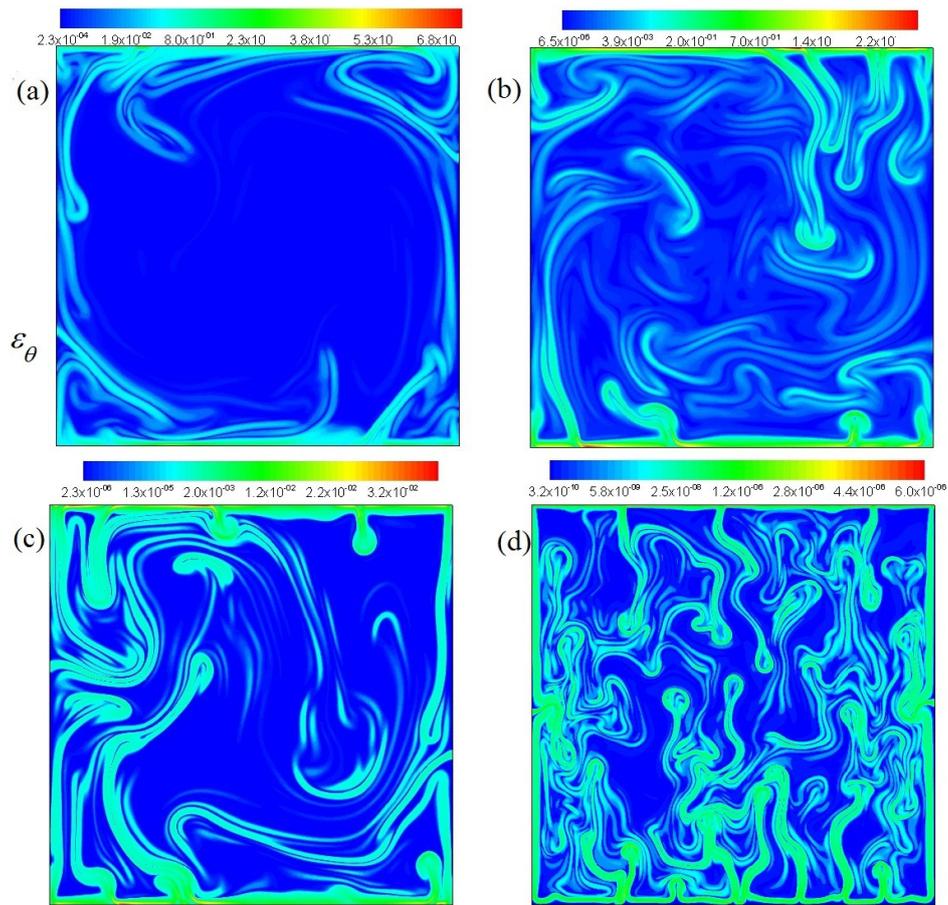


Figure 4. Thermal energy dissipation rates at $Pr = 6, 20, 100, 10^6$ (a–d), and $Ra = 5.4 \times 10^9$.

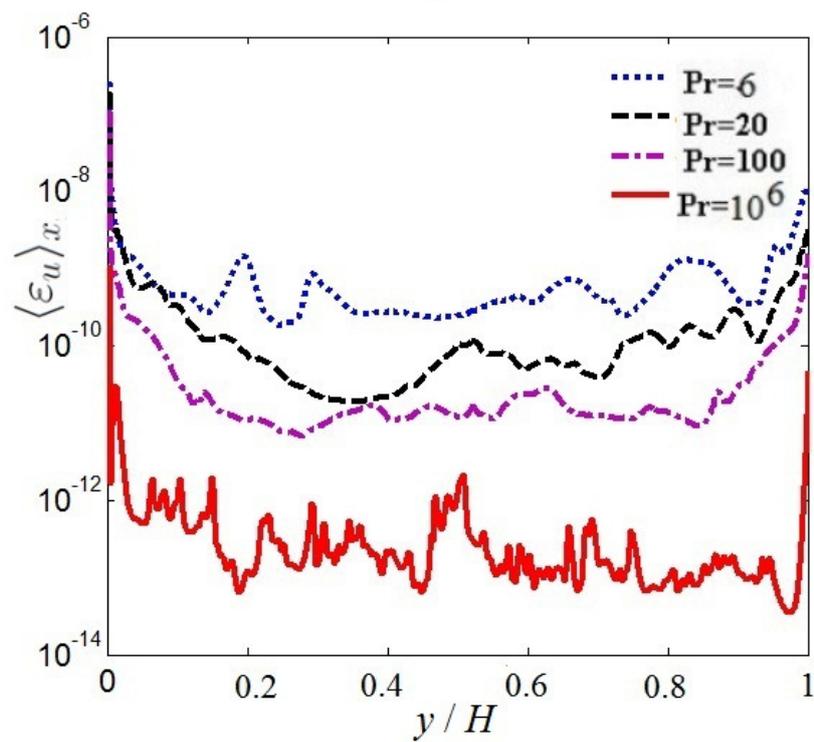


Figure 5. Mean vertical kinetic-energy dissipation rate profiles.

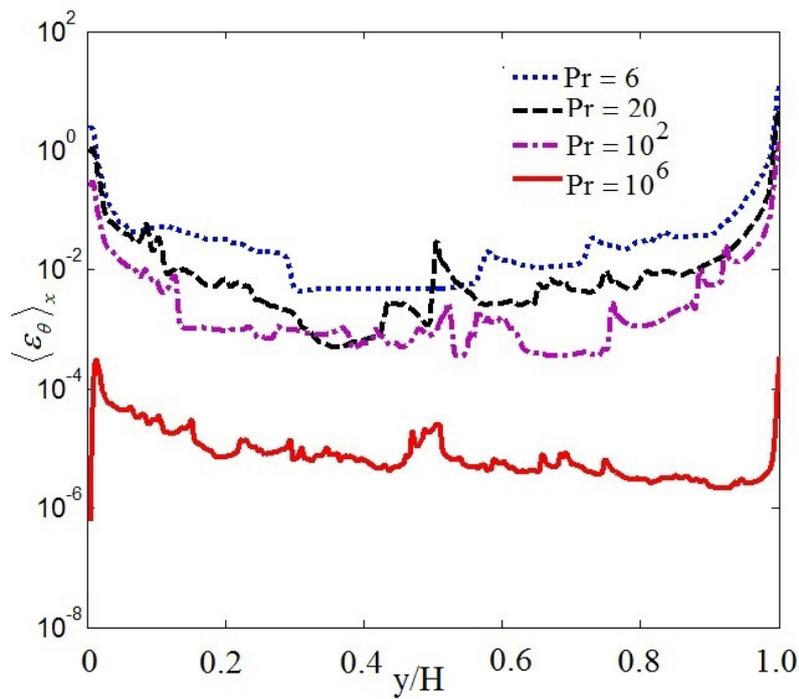


Figure 6. Mean vertical thermal dissipation rate profiles.

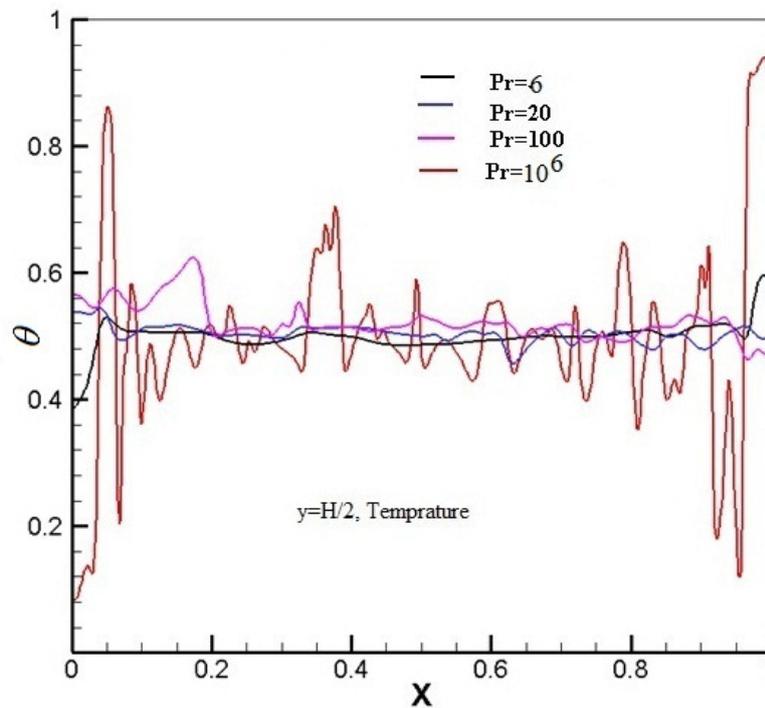


Figure 7. Instantaneous temperature distributions with superimposed temperature fields at $Pr = 6, 20, 100, 10^6$, and $Ra = 5.4 \times 10^9$.

The Bolgiano-Obukhov scaling is used to judge the dissipation scale in 2D turbulence thermal convection. The rigorous relations are obtained by assuming spatial homogeneity, within the Boussinesq approximations equation [4].

$$\langle \varepsilon_u \rangle_V = \frac{Nu - 1}{\sqrt{RaPr}} \tag{17}$$

$$\langle \varepsilon_\theta \rangle_V = \frac{Nu}{\sqrt{RaPr}} \tag{18}$$

The time and volume -averaged kinetic dissipation rates versus the Rayleigh number Ra , the time and volume-averaged thermal dissipation rates versus the Ra and Nusselt number Nu as a function of Ra at $Pr = 6, 20, 100,$ and 10^6 between numerical results and theoretical values are given in Figures 8–10. Figure 8 represents the so-called volume and time-averaged kinetic dissipation rates versus the Rayleigh number Ra . Figure 9 represents the thermal dissipation rates versus the Ra in the so-called volume and time-averaged. The solid lines represent the theoretical relation as relations (17) and (18). The dispersed points are the results of the present LBM. It is mainly demonstrated that the numerical calculation results of the LBM are excellently consistent with the theoretical value for time-averaged kinetic dissipation rates and thermal dissipation rates versus the Ra in Figures 8 and 9.

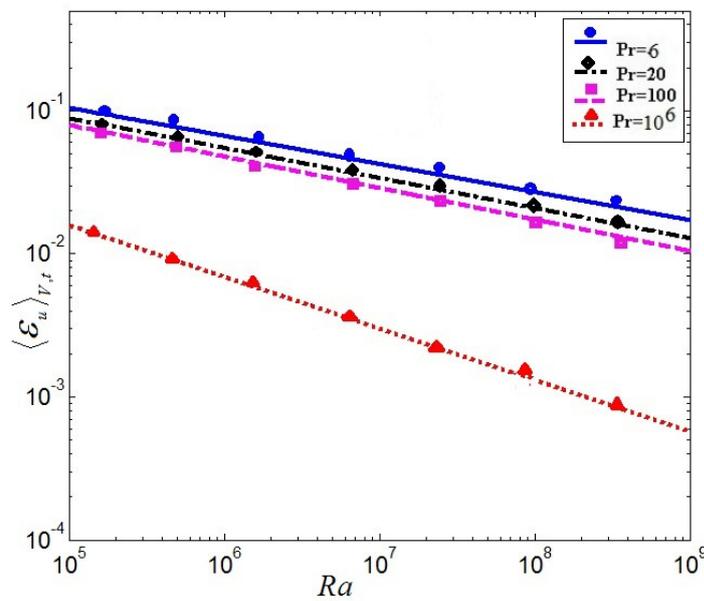


Figure 8. Volume and time-averaged kinetic dissipation rates versus the Rayleigh number Ra .

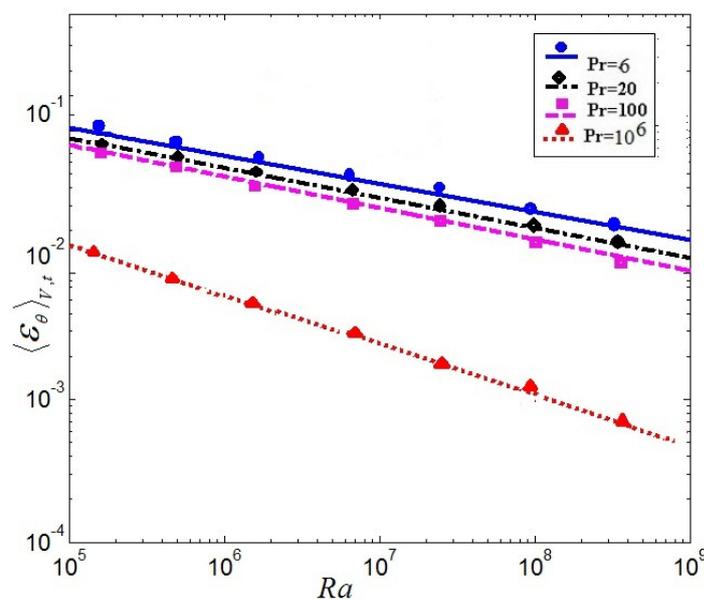


Figure 9. Volume and time-averaged thermal dissipation rates versus the Rayleigh number Ra .

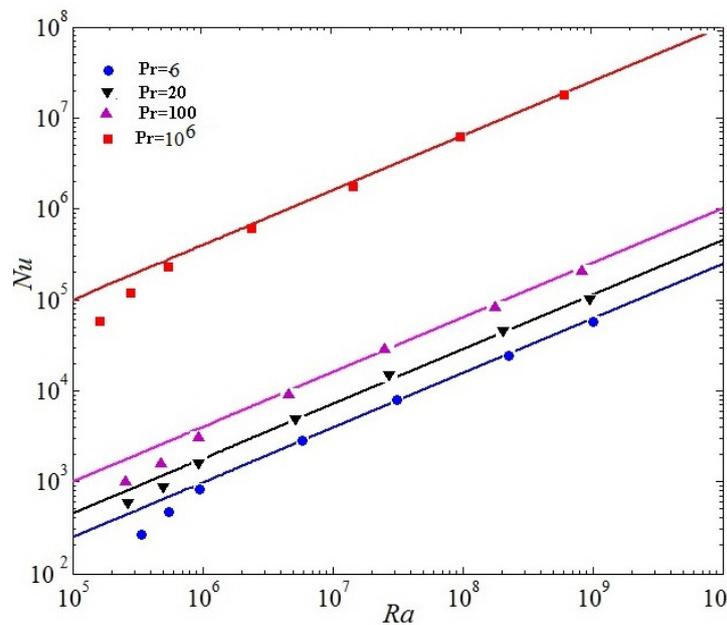


Figure 10. Nusselt number as a function of Rayleigh number at $Pr = 6, 20, 100,$ and 10^6 .

The relation of turbulent heat flux and the relation of the kinetic energy will be discussed, respectively. Figure 10 demonstrates the Nusselt number as a relation of Rayleigh number at $Pr = 6, 20, 100,$ and 10^6 . Figure 11 manifests the Reynolds number (Re) as a relation of Rayleigh number, respectively. Nusselt is wall averaged Nusselt number in the whole computational domain. The Grossmann-Lohse theory had offered a good insight for the of comprehension of $Nu(Ra, Pr), Re(Ra, Pr)$ (See Equations (19) and (20)) and even allowed multifarious predictions where the bulk turbulence plays an important role both the holistic kinetic dissipation and the system thermal dissipation [6].

$$Nu \sim Ra^{0.5} Pr^{0.5} \tag{19}$$

$$Re \sim Ra^{0.5} Pr^{-0.5} \tag{20}$$

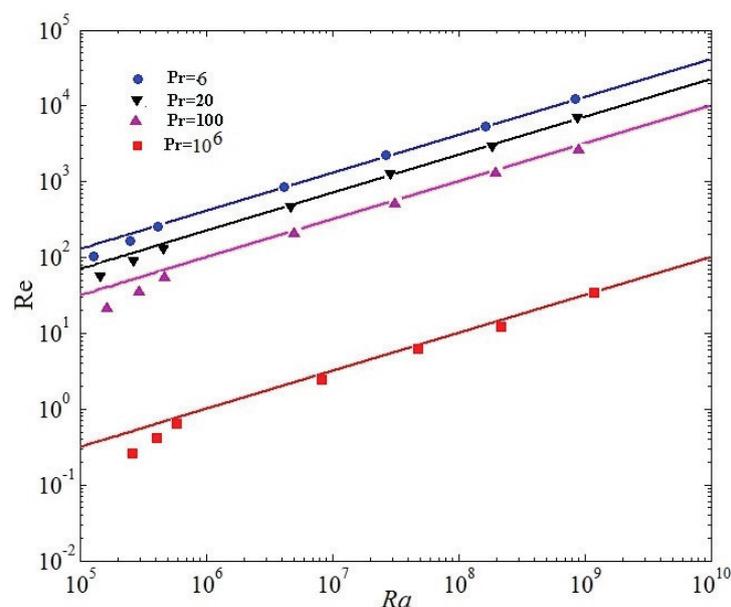


Figure 11. Reynolds number as a function of Rayleigh number at $Pr = 6, 20, 100,$ and 10^6 .

The relations (19) and (20) respectively represent the steady state regime of RB turbulence, which was proposed for turbulent RB convection at overwhelmingly high Ra by Kraichnan, and then developed by Grossmann and Lohse in their $Pr - Ra$ relations [6]. The ultimate state scaling was observed numerically [37] and experimentally [38,39], where the ultimate regime scaling is achieved when the solid boundaries are lacked. Plotted in Figures 10 and 11, it is noted that a linear scaling can be presented for both $Nu(Ra)$ and $Re(Ra)$ for nearly four decades from Ra 10^6 to 10^{10} . It is validated that the energy spectrum significantly decreases with the increase of the Pr . Our results further demonstrate that the numerical calculation results of the LBM are well consistent with the Grossmann-Lohse relations for $Nu(Pr, Ra)$ and $Re(Pr, Ra)$ [6] from $Ra = 10^6$ to 10^{10} in Figures 10 and 11.

3.2. Scaling of Energy Spectra, Fluxes and Spatial Intermittency

The scaling of energy spectra and fluxes will be discussed in the following section. For passive scalars, the value $5/3$ is in agreement with Obukhov-Corrsin scaling [6], and consistent with experimental findings of Kolmogorov scaling along the center line of turbulent convection [9]. Temperature power spectra have been investigated previously by some researchers [37,38].

$$E_u(k) \sim \varepsilon^{\frac{2}{3}} k^{-\frac{5}{3}} F(\eta k) \quad (21)$$

and

$$E_\theta(k) \sim (\beta g)^{-\frac{2}{5}} \varepsilon_\theta^{\frac{4}{5}} k^{-\frac{7}{5}} \quad (22)$$

in which $F(\cdot)$ denotes a single dimensionless relation of a dimensionless argument. The kinetic spectra and temperature spectra in central point ($N_x/2, N_y/2$) at time scales are showed in Figures 12 and 13, respectively. These results demonstrate that the energy spectrum is significantly decreased by the increase of the Pr in Figure 12. For the dimensionless inertial range ($0.03 < k\eta < 0.05$), the numerical results are consistent with Kolmogorov's $5/3$ spectrum at $Pr = 6$. For $Pr = 20$, the numerical results well agree with Kolmogorov's $5/3$ spectrum at the dimensionless inertial range ($0.04 < k\eta < 0.1$). For the dimensionless inertial range ($0.04 < k\eta < 0.16$), the numerical results are consistent with Kolmogorov's $5/3$ spectrum at $Pr = 100$. For $Pr = 10^6$, excellent agreement between the numerical results and Kolmogorov's $5/3$ spectrum is presented at the dimensionless inertial range ($0.06 < k\eta < 0.21$). It is found that the dimensionless inertial range is enlarged with increasing Pr , which is demonstrated that the energy dissipation rate scaling rises ($\varepsilon_u \sim \nu^3 Re^3 / L^4$) and the thermal dissipation rate ($\varepsilon_\theta \sim \kappa \Delta \theta^2 Re Pr / L^2$) increases gradually with increasing Pr . It is also demonstrated that current results could be explained near $7/5$ at low and near $5/3$ at lightly higher frequencies, respectively, agree with the collapse well on top of each other in the Bolgiano-Obukhov-like scaling [4,6]. To investigate the spatial intermittency effects of turbulent RB convection for different Prandtl numbers, the longitudinal velocity (See Equation (19)) and the structure function of temperature (See Equation (20)) over horizontal separations are regarded. The 2nd-order structure functions of velocity fluctuations and the 2nd-order structure functions of temperature fluctuations are hoped to next expressions, which are the most-studied quantities in buoyancy-driven turbulence [4].

$$S_2(r, t) \equiv \langle |\delta u_r(t)|^2 \rangle_V \equiv \frac{\nu^2}{L^4} (Nu - 1) Ra Pr^{-2} \quad (23)$$

It is found that the value of linear scaling decreases with the increase of Pr .

$$R_2(r, t) \equiv \langle |\delta \theta_r(t)|^2 \rangle_V \equiv \frac{\Delta^2}{H^2} Nu \quad (24)$$

in which Δ denotes the difference between the top wall and the bottom wall, and H denotes height of cavity. These relations can be easily derived from the Boussinesq equations and the corresponding

boundary conditions [6]. Secondly, the mixed velocity-temperature structure function is expected to following expression

$$M(r, t) \equiv \langle |\delta u_r(t) \delta \theta_r(t)| \rangle_V \tag{25}$$

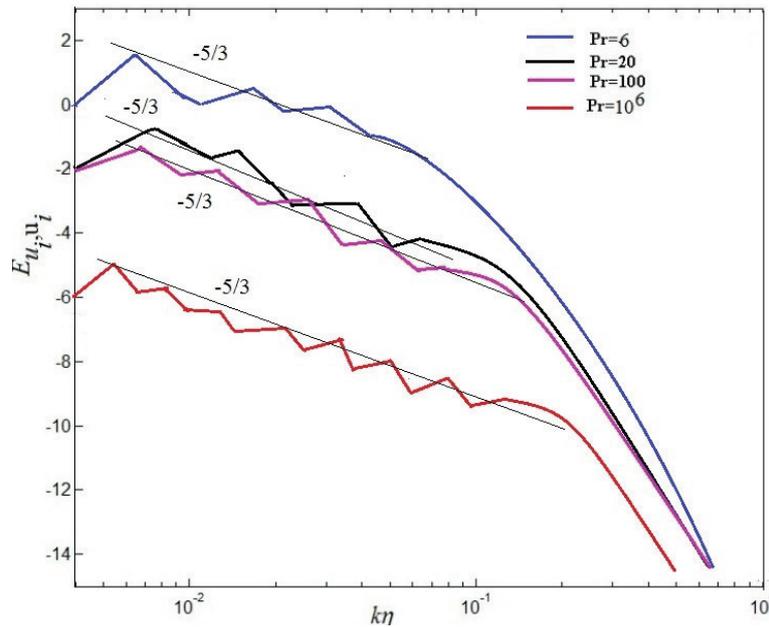


Figure 12. Kinetic energy spectra at different *Pr*.

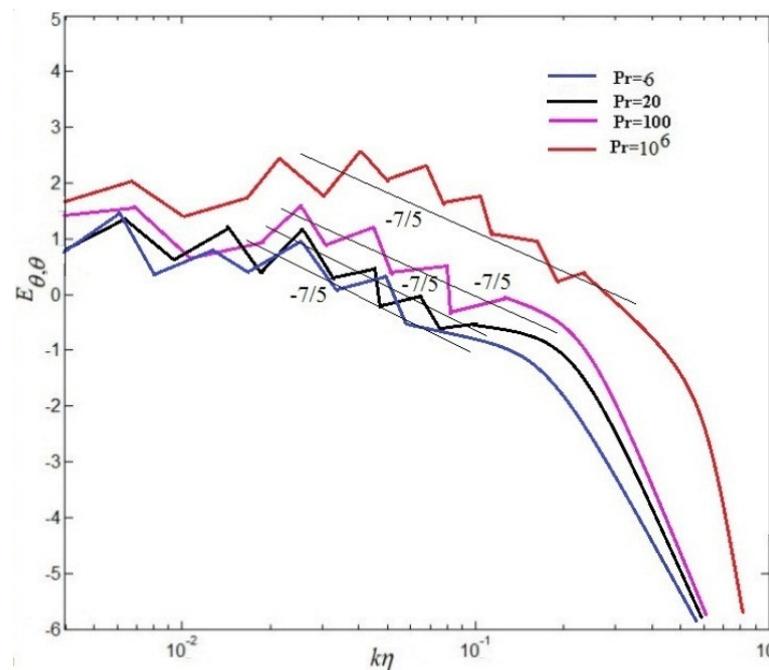


Figure 13. Temperature spectra at different *Pr*.

Figures 14–16 demonstrate respectively the second order structure function of velocity $S_2(r)$, structure function of temperature $R_2(r)$ and the mixed structure function (velocity-temperature) $M(r)$ at the whole computational domain computed at a late stage of the self-similar regime. As can be seen from Figure 14, as the *Pr* increases, the 2nd-order velocity decreases, which is qualitatively consistent with the theoretical predictions. It is validated that the 2nd-order velocity structure functions display

a series of linear scaling that extends to larger scales for different Prandtl numbers, i.e, $5 \leq r/\eta \leq 50$ for $Pr = 6$, $1 \leq r/\eta \leq 35$ for $Pr = 20$, $1 \leq r/\eta \leq 30$ for $Pr = 100$ and $0.1 \leq r/\eta \leq 10$ for $Pr = 10^6$ in Figure 14. It is validated that the value of linear scaling decreases with the increase of Pr , which may be given rise to large-scale circulation disappearing, the secondary eddies arising, and the dissipation of energy playing a major role at $Pr = 10^6$ in cavity, respectively. Noting that as the Pr increases, the 2nd-order velocity decreases, which is qualitatively consistent with the theoretical predictions (See Equation (19)). It is also demonstrated that a range of linear scaling emerges in the 2nd-order structure functions of velocity fluctuations, the 2nd-order structure functions fluctuations of temperature and the 2nd-order structure functions of mixed structure function, which may be in virtue of the small-scale temperature structures, like the thermal spikes or plumes that possess strong corrections. Plotted in Figures 15 and 16, the 2nd-order structure functions of temperature and the mixed structure function are also qualitative in agreement with those observed in Figure 14.

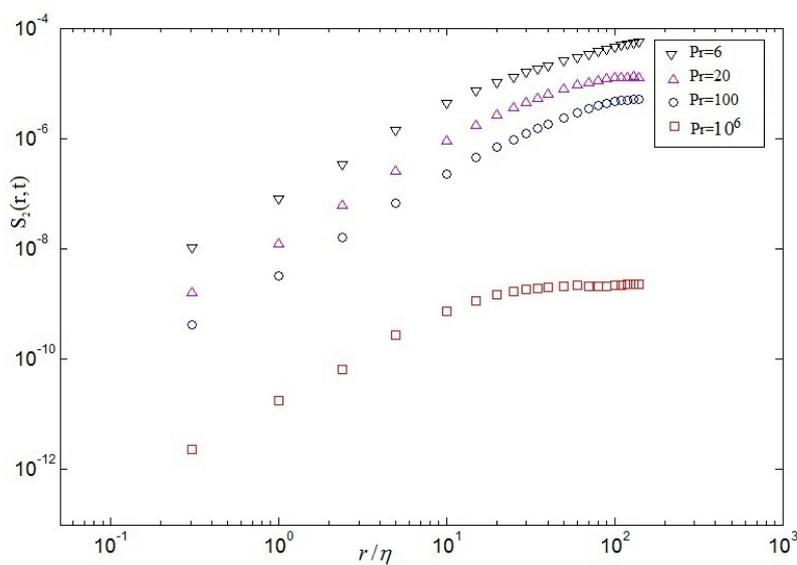


Figure 14. 2nd-order velocity structure functions at different Pr .

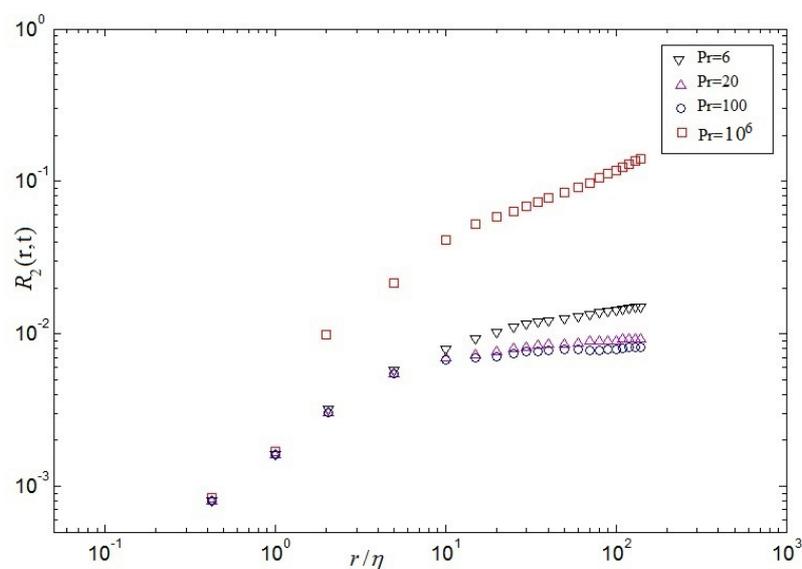


Figure 15. 2nd-order temperature structure functions at different Pr .

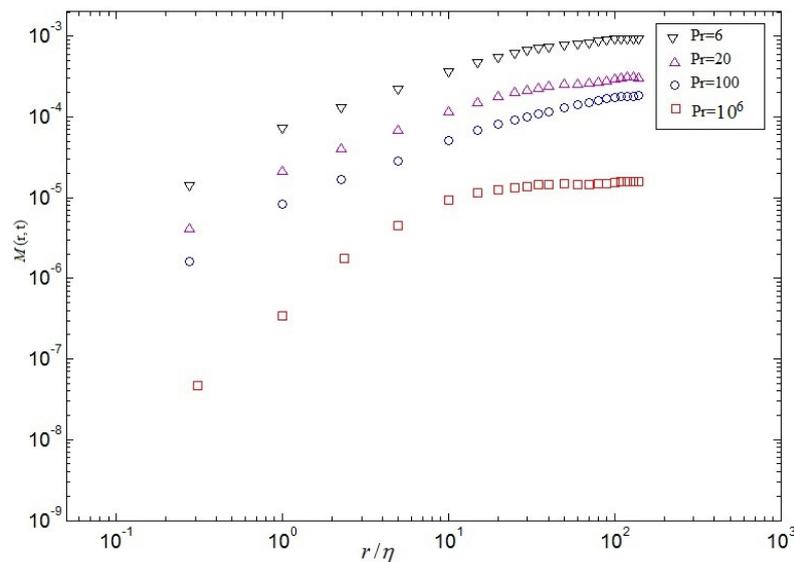


Figure 16. 2nd-order mixed velocity-temperature structure function at different Pr .

4. Conclusions

Numerical calculations of two-dimensional turbulent RB convection at large Prandtl number are investigated using LBM. Our results demonstrate that the variation characteristics of physical mechanism phenomenon about the kinematic viscosity dissipation, thermal dissipation, energy spectra, temperature spectra and the 2nd structure function with increasing Pr at the same Ra . The main conclusions are as follows:

Firstly, the large scale circulation in cavity is gradually broken up into small scale structures that thermal plumes rise and fall from the bottom to top walls with increasing Pr , which agrees with the visualization of the experiment. The large-scale circulations of the fluid are decomposed gradually with the increase of Pr . It is found that the vertical motion of various plumes gradually play a main role with increasing Pr . Especially, a large number of small-scale thermal plumes vertically rise from the bottom wall to top wall, a large number of small-scale cold plumes vertically fall from the top wall to the bottom wall, and a great deal of small eddies appear at $Pr = 10^6$. Secondly, the kinematic viscosity dissipation rate and the thermal dissipation rate gradually decrease with increasing Pr , which is qualitatively consistent with the theoretical predictions. The intense thermal dissipation events mainly concentrate on the interfaces of hot fluid and cold fluid. The thermal dissipation rate ε_θ already plays a key role in the thermal energy transport, thus ε_u can have no effect in virtue of inverse cascade of kinetic energy in thermal convection. It is also demonstrated that the numerical calculation results of the LBM are excellently consistent with the theoretical value for time-averaged kinetic and thermal dissipation rates versus the Ra . In addition, the energy spectrum significantly decreases with increasing Pr , which indicates that the numerical results of the LBM agree with the Grossmann-Lohse theory for $Nu(Pr, Ra)$ and $Ra(Pr, Ra)$ [6] from $Ra 10^6$ to 10^{10} . Finally, the 2nd-order velocity decreases with increasing Pr , which is qualitatively consistent with the theoretical value. It is also found that a scope of linear scaling appears in the second order structure functions of velocity fluctuations, the second order structure functions of temperature fluctuations and mixed structure function, which may be in virtue of the small-scale temperature structures, like the thermal plumes or spikes.

Due to natural parallelism of the LBM, the LBM may have potential prospects to simulate turbulent RB convection. Even though the results of two-dimensional cases are reported in this paper, similar scaling laws may appear (the Kolmogorov-Obukhov scenario) in 3D and it might be crucial to modify parametric assemblies in numerical simulations. Accordingly, allowed us to evaluate the importance of the Kolmogorov-Obukhov scenario in three dimensions at large Pr . Our results

discussed in this paper provide insights into the flow dynamics of RB convection. These results will be useful in modelling convective flows in the atmospheres and interiors of stars and planets, as well as in the applications of engineer.

Author Contributions: Conceptualization, H.Y. and Y.W.; Methodology, Y.W.; Software, Z.Z.; Validation, H.Y., Y.W. and H.D.; Formal Analysis, Y.W.; Investigation, H.Y.; Resources, H.Y.; Data Curation, Y.W.; Writing—Original Draft Preparation, H.Y.; Writing—Review & Editing, Y.W.; Visualization, H.Y.; Supervision, Y.W.; Project Administration, Y.W.; Funding Acquisition, H.Y.

Funding: This work was supported by the National Natural Science Foundation of China 1502237, 51536008; Natural Science Foundation of Zhejiang Province LY18A020010; Natural Science Fund project of Jiangsu Province BK20140585; Zhejiang Province Science and Technology Plan Project 2017C34007; and Young Researchers Foundation of Zhejiang Provincial Top Key Academic Discipline of Mechanical Engineering of Zhejiang Sci-Tech University ZSTUME02B06.

Acknowledgments: We sincerely appreciate Hui Xu for interesting discussions, which helps us to improve our code. Financial support from National Natural Science Foundation is gratefully acknowledged. The simulations were implemented on resources provided by computing center of Zhejiang Sci-Tech University.

Conflicts of Interest: The authors declare no conflict of interest.

References

- Hartmann, D.L.; Moy, L.A.; Fu, Q. Tropical convection and the energy balance at the top of the atmosphere. *J. Clim.* **2011**, *14*, 4495–4511. [[CrossRef](#)]
- Marshall, J.; Schott, F. Open-Ocean convection: Observations, theory, and models. *Rev. Geophys.* **1999**, *37*, 1–64. [[CrossRef](#)]
- Cardin, P.; Olson, P. Chaotic thermal convection in a rapidly rotating spherical shell: Consequences for flow in the outer core. *Phys. Earth Planet. Inter.* **1994**, *82*, 235–259. [[CrossRef](#)]
- Lohse, D.; Xia, K.Q. Small-Scale properties of turbulent Rayleigh–Bénard convection. *Annu. Rev. Fluid. Mech.* **2010**, *42*, 335–364. [[CrossRef](#)]
- Chilla, F.; Schumacher, J. New perspectives in turbulent Rayleigh–Bénard convection. *Eur. Phys. J. E* **2012**, *35*, 58–82. [[CrossRef](#)] [[PubMed](#)]
- Ahlers, G.; Grossmann, S.; Lohse, D. Heat transfer and large scale dynamics in turbulent Rayleigh–Bénard convection. *Rev. Mod. Phys.* **2009**, *81*, 503–537. [[CrossRef](#)]
- Scheel, J.D.; Emran, M.S.; Schumacher, J. Resolving the fine-scale structure in turbulent Rayleigh–Bénard convection. *New J. Phys.* **2013**, *15*, 113063–113075. [[CrossRef](#)]
- Hu, Y.P. Flow pattern and heat transfer in Rayleigh–Bénard convection of cold water near its density maximum in a rectangular cavity. *Int. J. Heat Mass Trans.* **2017**, *107*, 1065–1075. [[CrossRef](#)]
- Zhang, L.; Li, Y.R.; Zhang, H. Onset of double-diffusive Rayleigh–Bénard convection of a moderate Prandtl number binary mixture in cylindrical enclosures. *Int. J. Heat Mass Trans.* **2017**, *107*, 500–509. [[CrossRef](#)]
- Vincent, A.P.; Yuen, D.A. Transition to turbulent thermal convection beyond $Ra = 10^{10}$ detected in numerical simulations. *Phys. Rev. E* **2007**, *61*, 5241–5249. [[CrossRef](#)]
- Schmalzl, J.; Breuer, M.; Hansen, U. On the validity of two-dimensional numerical approaches to time-dependent thermal convection. *Europhys. Lett.* **2004**, *67*, 390–399. [[CrossRef](#)]
- Zhong, J.Q.; Ahlers, G. Heat transport and the large-scale circulation in rotating Turbulent Rayleigh–Bénard convection. *J. Fluid Mech.* **2014**, *665*, 300–333. [[CrossRef](#)]
- Puthenveetil, B.A.; Arakeri, J.H. Plume structure in Rayleigh-number convection. *J. Fluid Mech.* **2005**, *542*, 217–249. [[CrossRef](#)]
- Shishkina, O.; Wagner, C. Local heat fluxes in turbulent Rayleigh–Bénard convection. *Phys. Fluids* **2007**, *9*, 0851071–08510713. [[CrossRef](#)]
- Shishkina, O.; Wagner, C. Analysis of sheet like thermal plumes in turbulent Rayleigh–Bénard convection. *J. Fluid Mech.* **2012**, *599*, 383–404. [[CrossRef](#)]
- Kaczorowski, M.; Wagner, C. Analysis of the thermal plumes in turbulent Rayleigh–Bénard convection based on well-resolved numerical simulations. *J. Fluid Mech.* **2011**, *618*, 89–112. [[CrossRef](#)]
- Kaczorowski, M.; Chong, K.L.; Xia, K.Q. Turbulent flow in the bulk of Rayleigh–Bénard convection: Aspect-ratio dependence of the small-scale properties. *J. Fluid Mech.* **2014**, *747*, 73–102. [[CrossRef](#)]

18. Zhou, Q.; Xia, K.Q. Aspect ratio dependence of heat transport by turbulent Rayleigh–Bénard convection in rectangular cells. *J. Fluid Mech.* **2012**, *710*, 260–276. [[CrossRef](#)]
19. Xu, H.; Sagaut, P. Optimal low-dispersion low-dissipation LBM schemes for computational aeroacoustics. *J. Comput. Phys.* **2011**, *230*, 5353–5382. [[CrossRef](#)]
20. Krishnamurti, R. On the transition to turbulent convection. Part 1. The transition from two- to three-dimensional flow. *J. Fluid Mech.* **1970**, *42*, 295–307. [[CrossRef](#)]
21. Krishnamurti, R. On the transition to turbulent convection. Part 2. The transition to time-dependent flow. *J. Fluid Mech.* **1970**, *42*, 309–320. [[CrossRef](#)]
22. Busse, F.H.; Whitehead, J.A. Instabilities of convection rolls in a high Prandtl number fluid. *J. Fluid. Mech.* **1971**, *47*, 305–320. [[CrossRef](#)]
23. Succi, S. *The Lattice Boltzmann Equation: For Complex States Flowing Matter*; Oxford University Press: Oxford, UK, 2018.
24. Qian, Y.H.; d’Humières, D.; Lallemand, P. Lattice BGK Models for Navier-Stokes Equation. *Europhys. Lett.* **1992**, *17*, 479–484. [[CrossRef](#)]
25. Liu, H.H.; Zhang, Y.H.; Valocchi, A.J. Modeling and Simulation of Thermocapillary Flows Using Lattice Boltzmann Method. *J. Comput. Phys.* **2012**, *231*, 4433–4453. [[CrossRef](#)]
26. Wei, Y.K.; Wang, Z.D.; Yang, J.F.; Dou, H.S.; Qian, Y.H. A simple lattice Boltzmann model for turbulence Rayleigh–Bénard thermal convection. *Comput. Fluids* **2015**, *118*, 167–171. [[CrossRef](#)]
27. Wei, Y.K.; Dou, H.S.; Yang, H. Characteristics of heat transfer with different dimensionless distance in an enclosure. *Mod. Phys. Lett. B* **2016**, *30*, 1650364–1650369. [[CrossRef](#)]
28. Chen, H.; Kandasamy, S.; Orszag, S.; Shock, R. Extended Boltzmann kinetic equation for turbulent flows. *Science* **2003**, *301*, 633–636. [[CrossRef](#)] [[PubMed](#)]
29. Liang, H.; Shi, B.C.; Chai, Z.H. An efficient phase-field-based multiple-relaxation-time lattice Boltzmann model for three-dimensional multiphase flows. *Comput. Math. Appl.* **2017**, *73*, 1524–1538. [[CrossRef](#)]
30. Liang, H.; Shi, B.C.; Chai, Z.H. Lattice Boltzmann simulation of three-dimensional Rayleigh–Taylor instability. *Phys. Rev. E* **2016**, *93*, 033113–033119. [[CrossRef](#)] [[PubMed](#)]
31. Montessoria, A.; Prestininzi, P.; Rocca, M.L.; Falcucci, G.; Succi, S.; Kaxiras, E. Effects of Knudsen diffusivity on the effective reactivity of nanoporous catalyst media. *J. Comput. Sci.* **2016**, *17*, 377–383. [[CrossRef](#)]
32. Xu, H.; Malaspina, O.; Sagaut, P. Sensitivity analysis and determination of free relaxation parameters for the weakly-compressible MRT-LBM schemes. *J. Comput. Phys.* **2012**, *231*, 7335–7367. [[CrossRef](#)]
33. Liu, H.H.; Valocchi, A.J.; Zhang, Y.H. Lattice Boltzmann Phase Field Modeling Thermocapillary Flows in a Confined Microchannel. *J. Comput. Phys.* **2014**, *256*, 334–356. [[CrossRef](#)]
34. Aidun, C.K. Lattice-Boltzmann Method for Complex Flows. *Annu. Rev. Fluid Mech.* **2010**, *42*, 439–472. [[CrossRef](#)]
35. Shan, X. Simulation of Rayleigh–Bénard convection using a lattice Boltzmann method. *Phys. Rev. E* **1997**, *55*, 2780–2788. [[CrossRef](#)]
36. Krastev, V.K.; Falcucci, G. Simulating Engineering Flows through Complex Porous Media via the Lattice Boltzmann Method. *Energies* **2018**, *11*, 715. [[CrossRef](#)]
37. Lohse, D.; Toschi, F. Ultimate state of thermal convection. *Phys. Rev. Lett.* **2003**, *90*, 034502–034507. [[CrossRef](#)] [[PubMed](#)]
38. Gibert, H.; Pabiou, F.; Castaing, B. High-Rayleigh-number convection in a vertical channel. *Phys. Rev. Lett.* **2006**, *96*, 084501–084510. [[CrossRef](#)] [[PubMed](#)]
39. Shang, X.D.; Tong, P.; Xia, K.Q. Scaling of the local convective heat flux in turbulent Rayleigh–Bénard convection. *Phys. Rev. Lett.* **2008**, *100*, 244503–244510. [[CrossRef](#)] [[PubMed](#)]

