

Modeling Binary and Multicomponent Systems Containing Supercritical CO₂ with Polyethylene Glycols and Compounds Relevant to the Biodiesel Production

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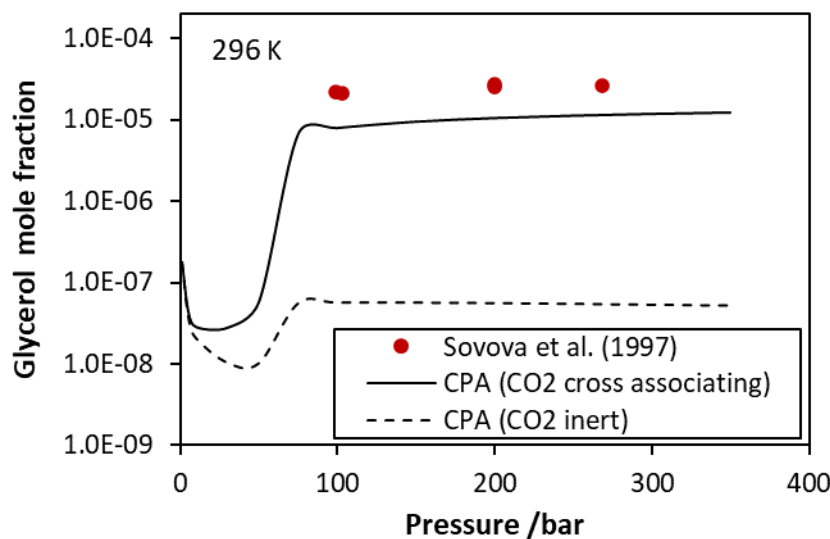


Figure S1. CO₂ - glycerol VLE. Glycerol mole fraction in the vapor phase. Experimental data [40] and CPA correlations using the interaction parameters of Table 4 of the main article.

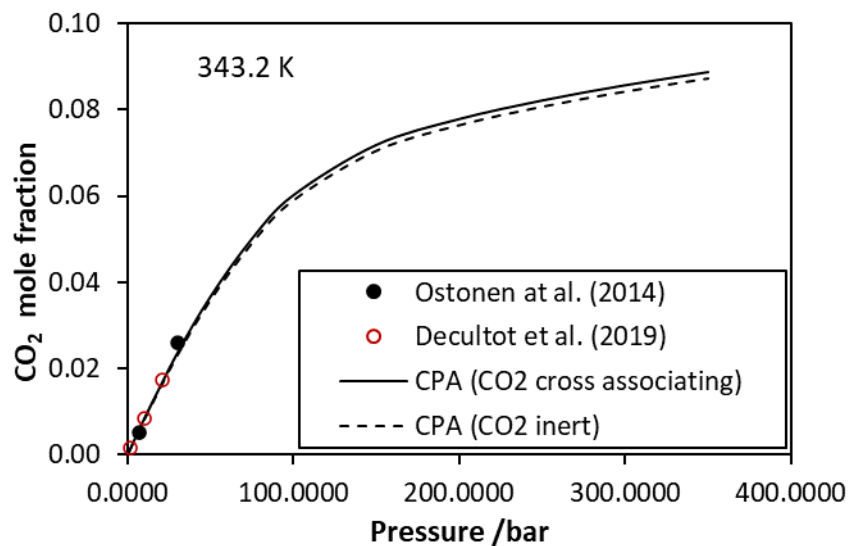


Figure S2. CO₂ - glycerol VLE. CO₂ mole fraction in the liquid phase. Experimental data [41,42] and CPA correlations using the interaction parameters of Table 4 of the main article.

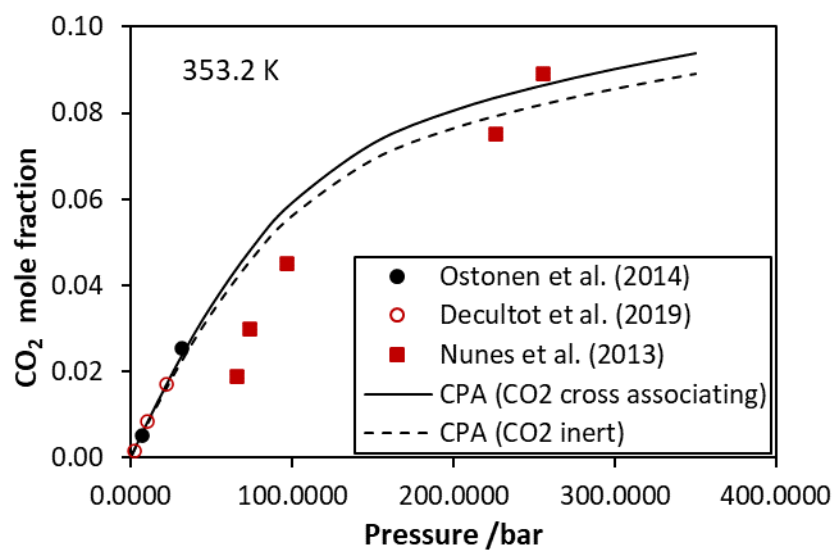


Figure S3. CO₂ - glycerol VLE. CO₂ mole fraction in the liquid phase. Experimental data [39,41,42] and CPA correlations using the interaction parameters of Table 4 of the main article.

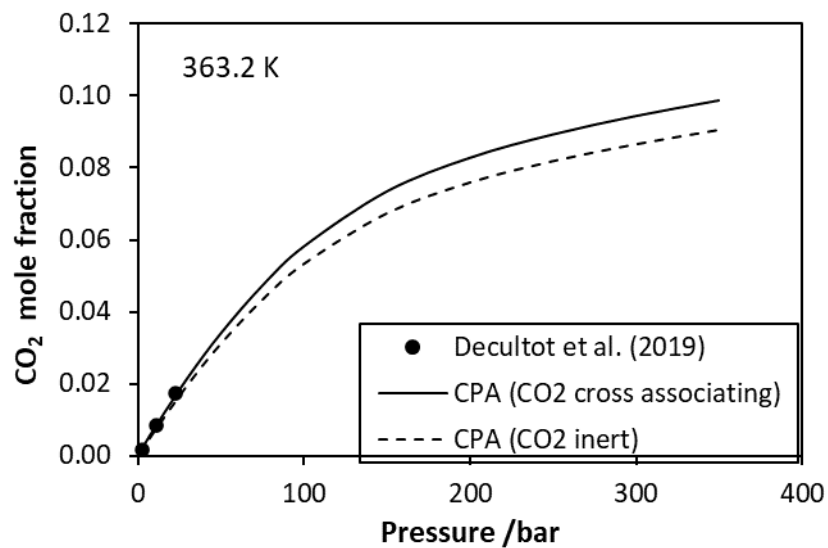


Figure S4. CO₂ - glycerol VLE. CO₂ mole fraction in the liquid phase. Experimental data [42] and CPA correlations using the interaction parameters of Table 4 of the main article.

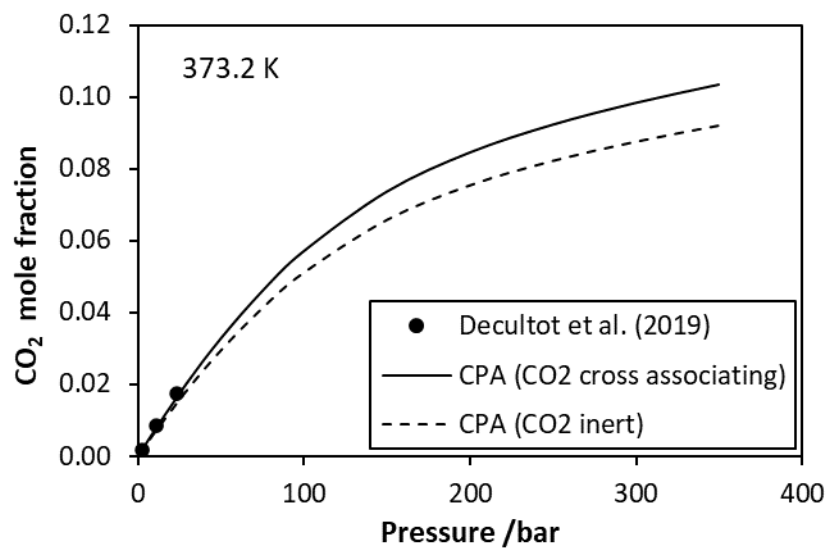


Figure S5. CO₂ - glycerol VLE. CO₂ mole fraction in the liquid phase. Experimental data [42] and CPA correlations using the interaction parameters of Table 4 of the main article.

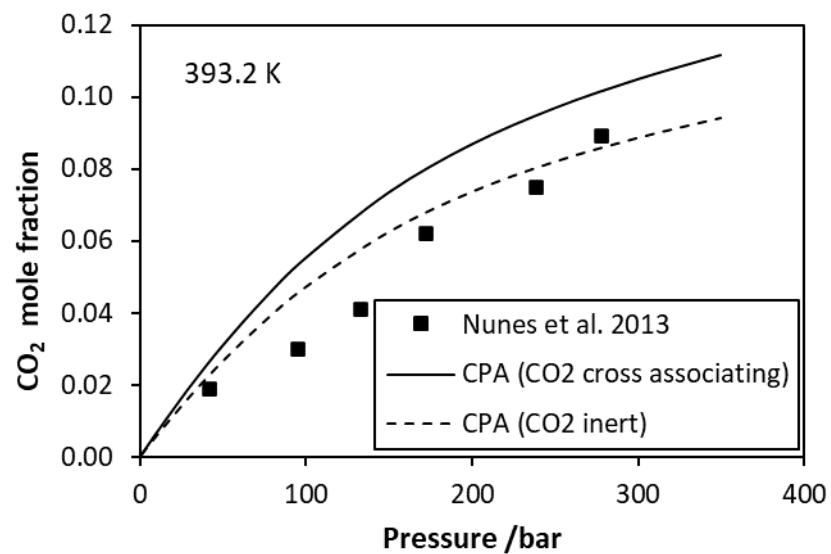


Figure S6. CO₂ - glycerol VLE. CO₂ mole fraction in the liquid phase. Experimental data [39] and CPA correlations using the interaction parameters of Table 4 of the main article.

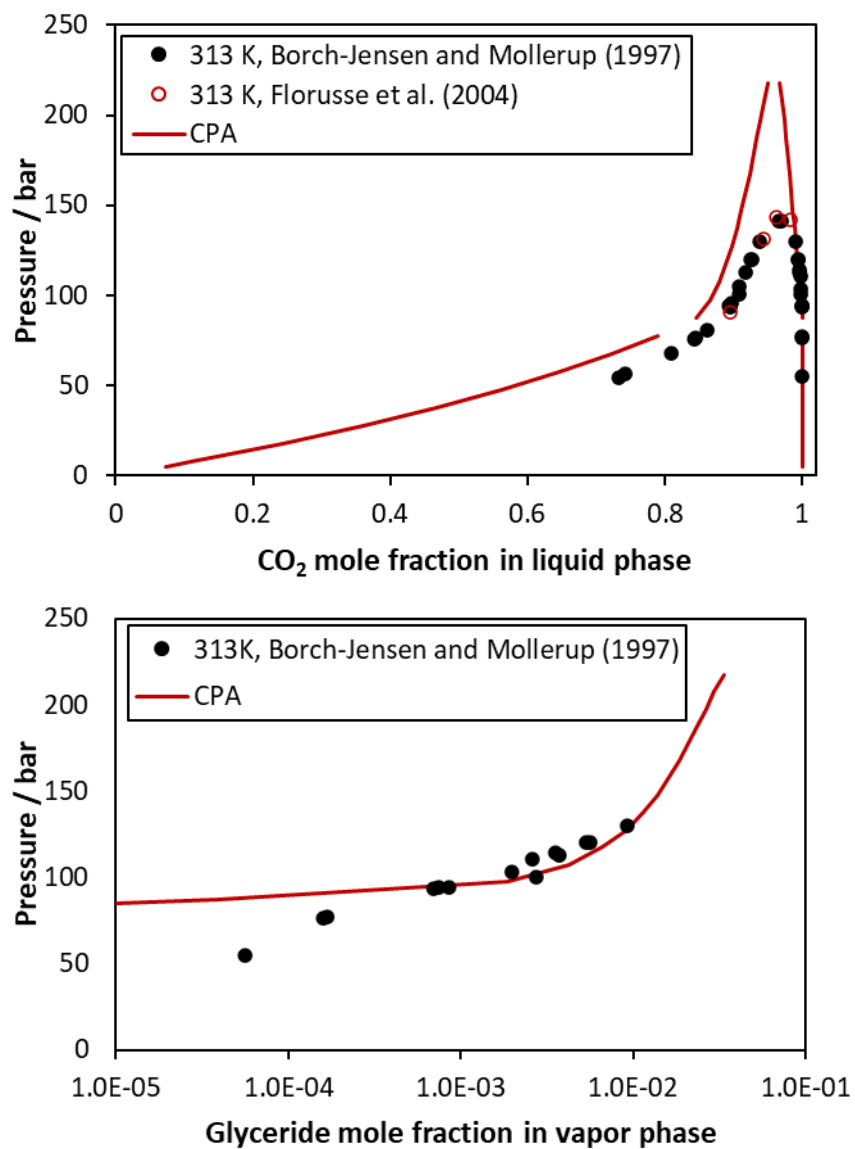


Figure S7. CO₂ - tricaprilyn VLE at 313 K. Experimental data [43,44] and CPA correlations using the binary parameter of Table 5 of the main article.

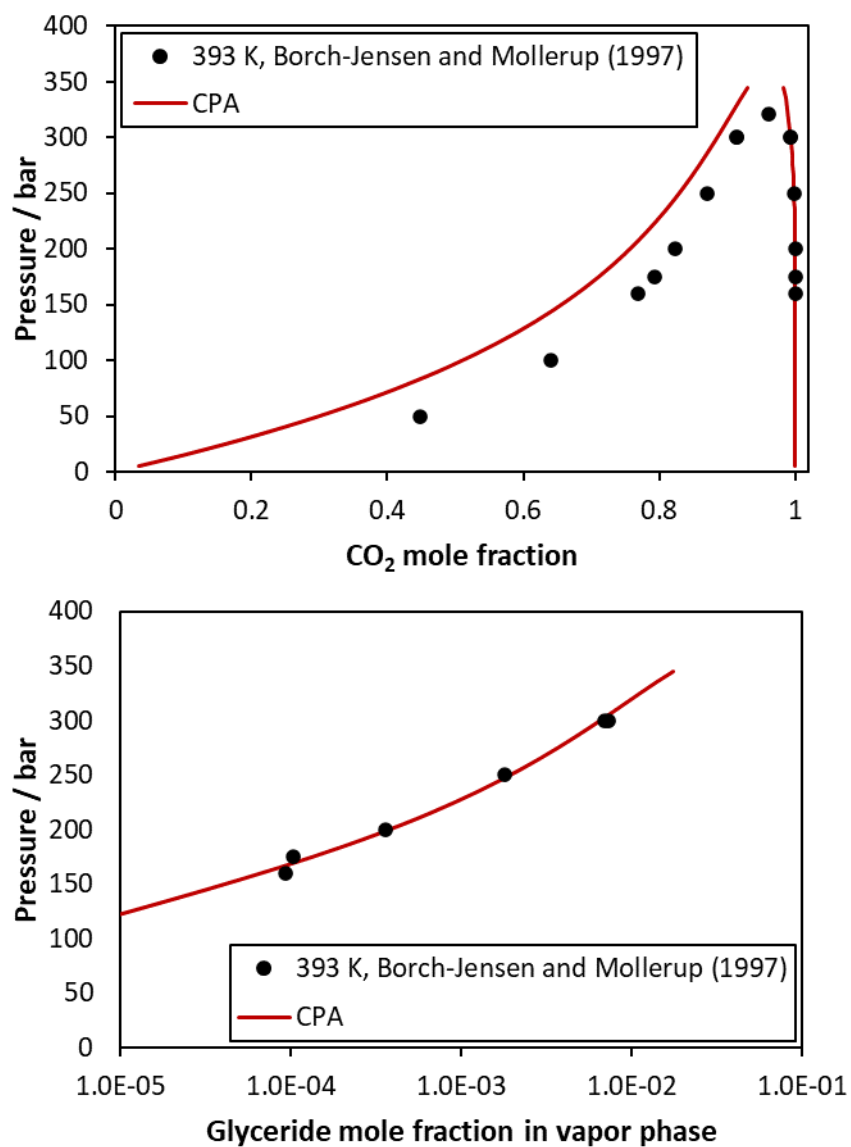


Figure S8. CO₂ - tricaprilyn VLE at 393 K. Experimental data [43] and CPA correlations using the binary parameter of Table 5 of the main article.

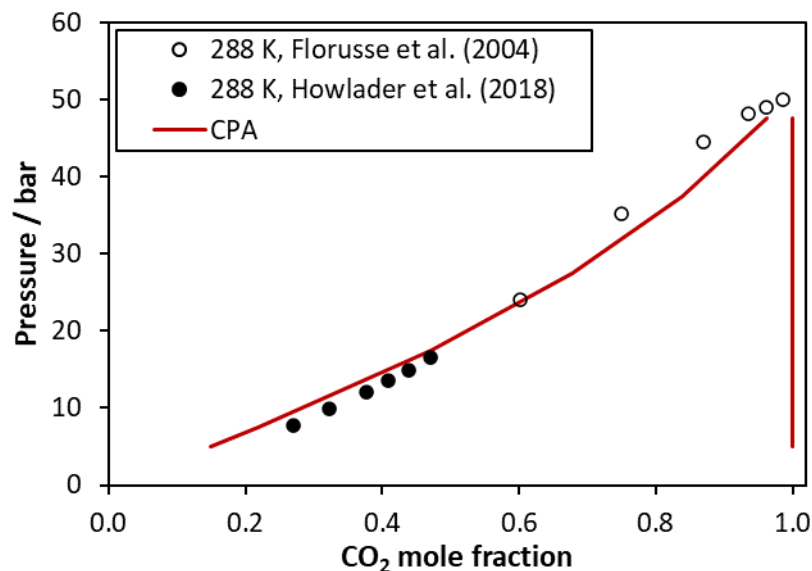


Figure S9. CO₂ - tributyrin VLE at 288 K. Experimental data [44,45] and CPA correlations using the binary parameter of Table 5 of the main article.

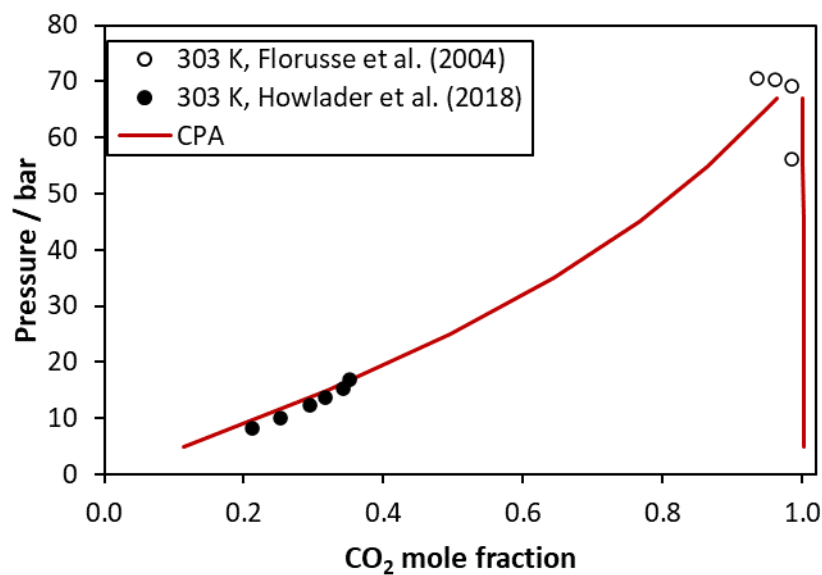


Figure S10. CO₂ - tributyrin VLE at 303 K. Experimental data [44,45] and CPA correlations using the binary parameter of Table 5 of the main article.

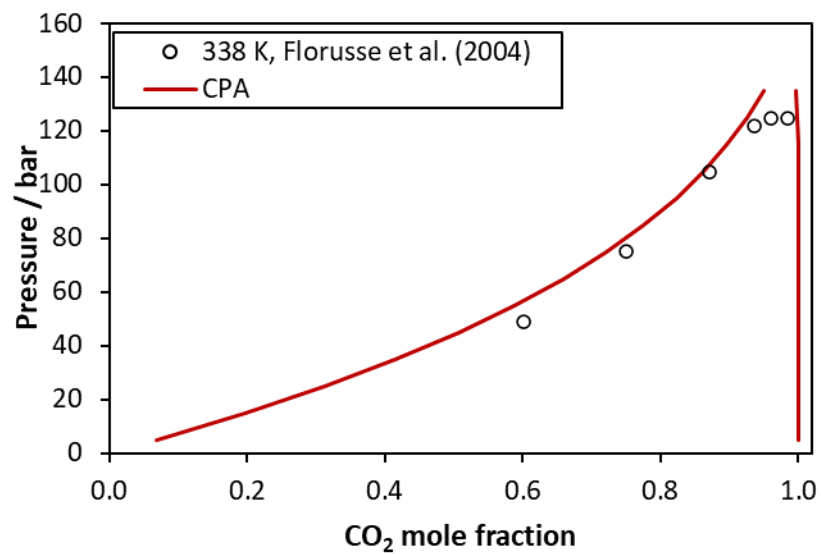


Figure S11. CO₂ - tributyrin VLE at 338 K. data [44,45] and CPA correlations using the binary parameter of Table 5 of the main article.

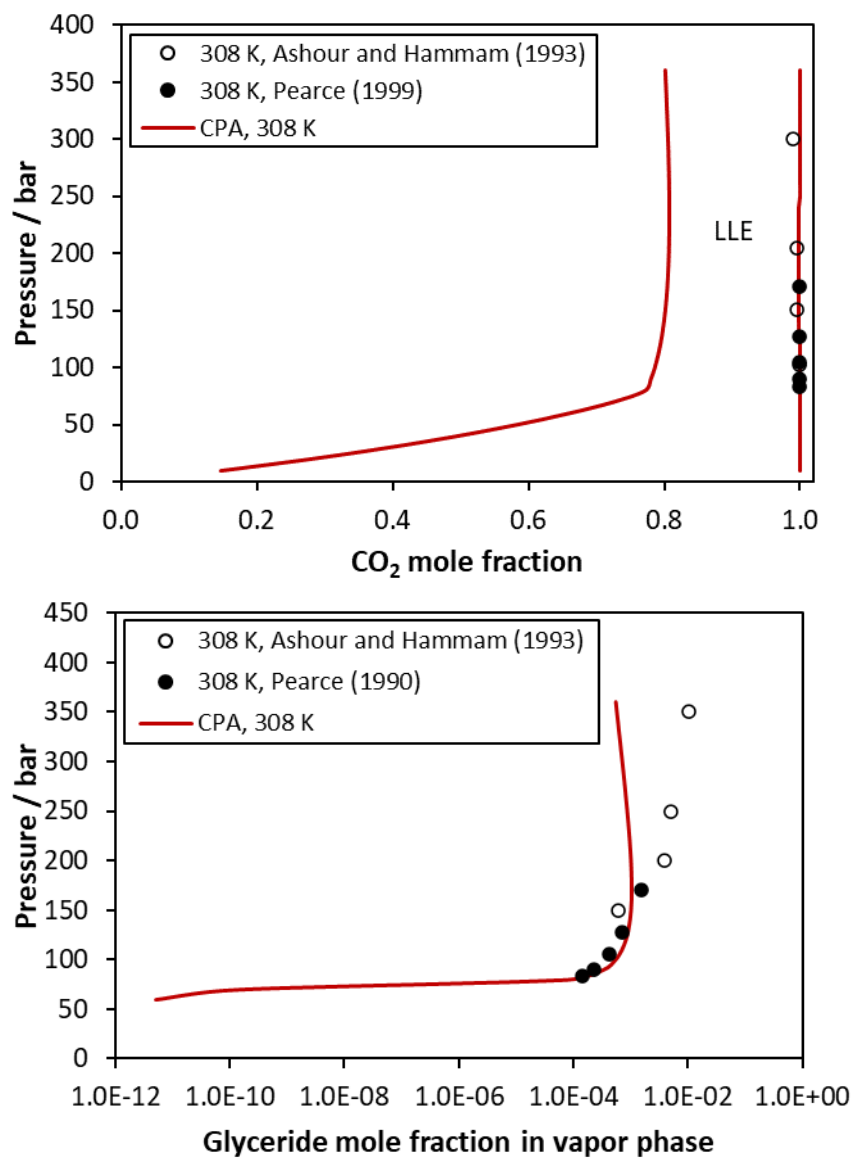


Figure S12. CO₂ - trilaurin VLE and LLE at 308 K. Experimental data [48,49] and CPA correlations using the binary parameter of Table 5 of the main article.

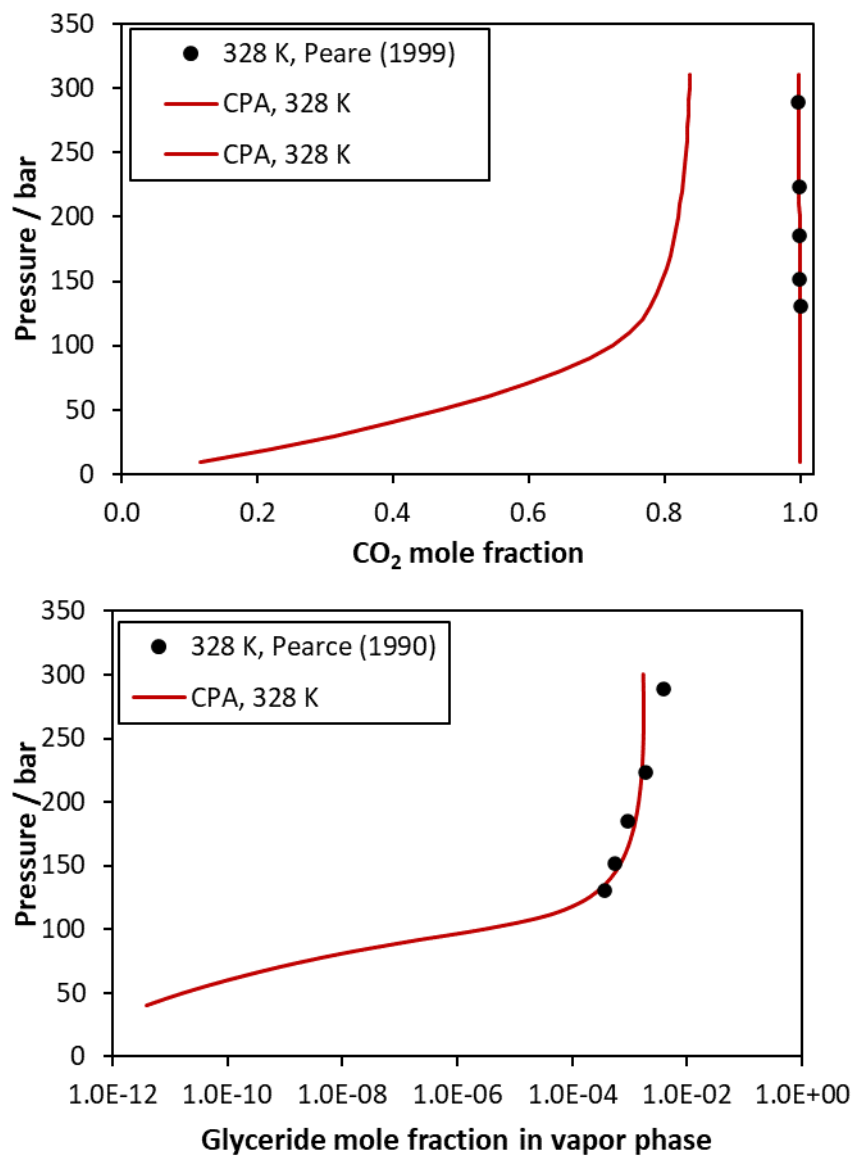


Figure S13. CO₂ - trilaurin VLE at 328 K. Experimental data [48] and CPA correlations using the binary parameter of Table 5 of the main article.

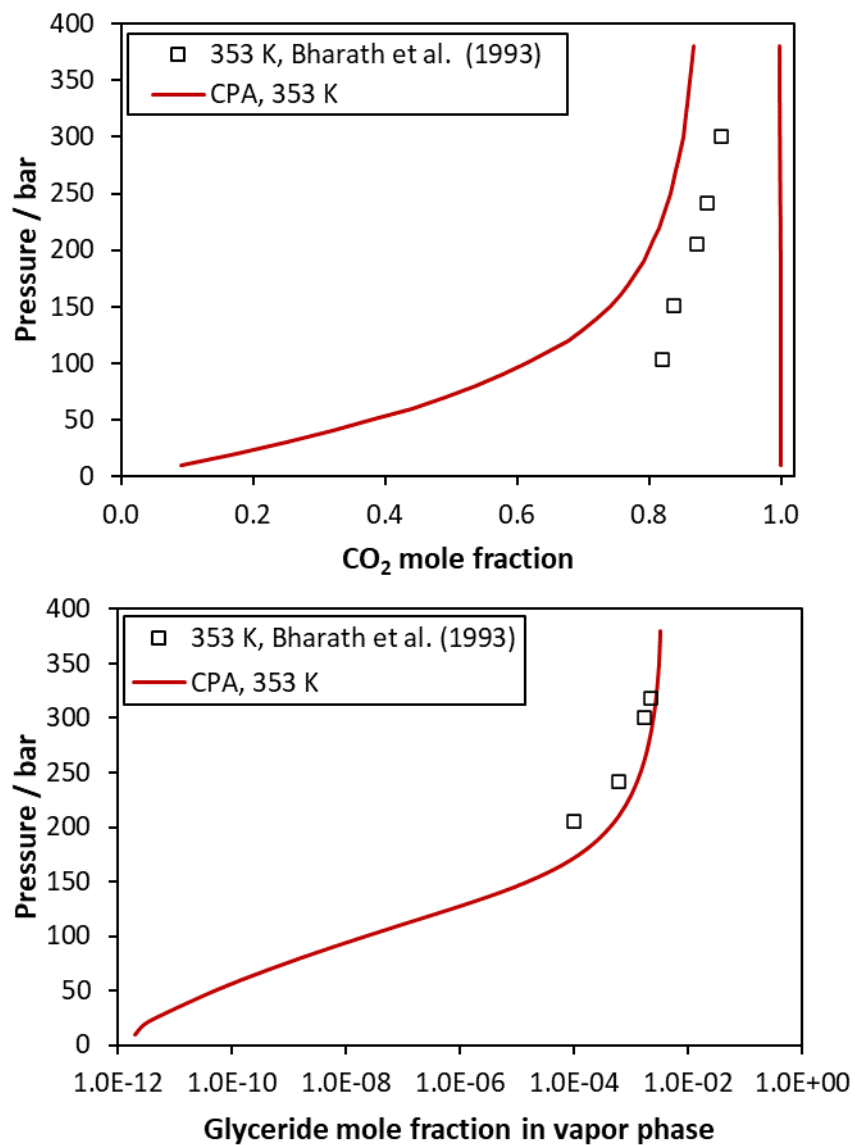


Figure S14. CO₂ - trilaurin VLE at 353 K. Experimental data [47] and CPA correlations using the binary parameter of Table 5 of the main article.

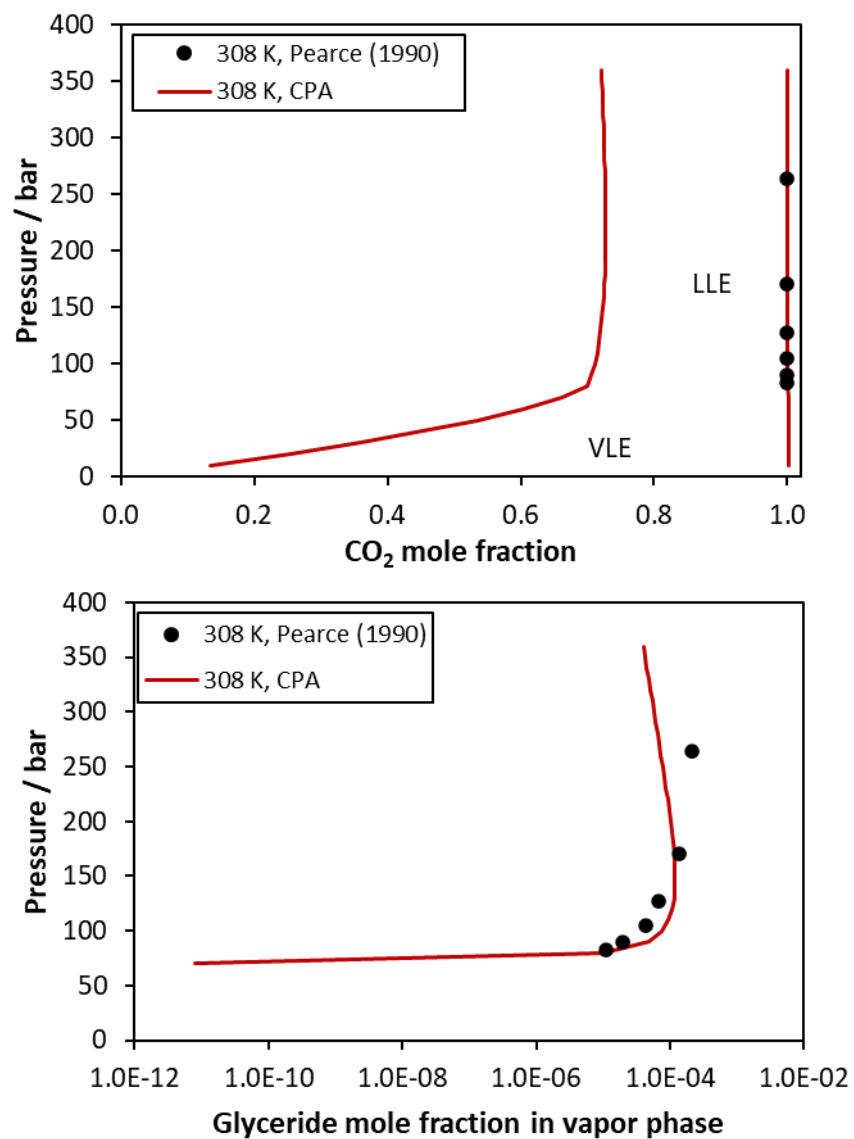


Figure S15. CO₂ – trimyrustin VLE at 308 K. Experimental data [48] and CPA correlations using the binary parameter of Table 5 of the main article.

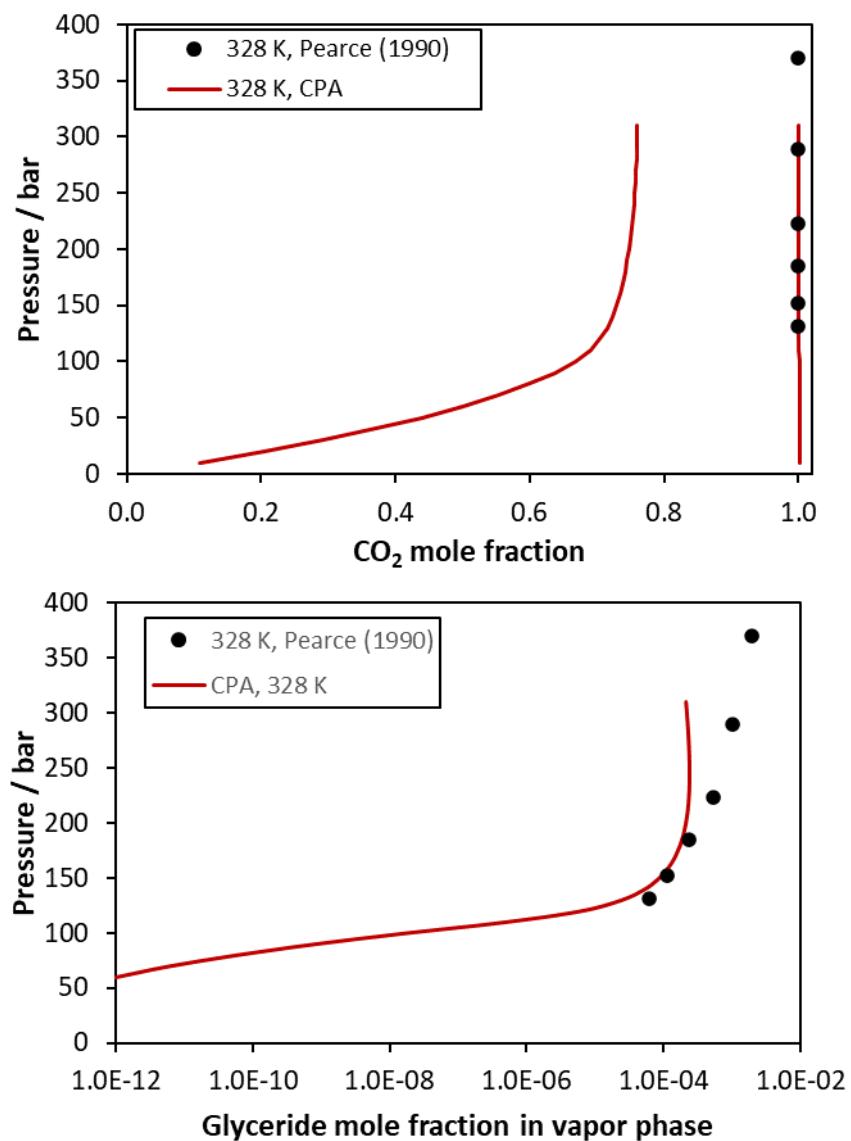


Figure S16. CO₂ – trimyristin VLE at 328 K. Experimental data [48] and CPA correlations using the binary parameter of Table 5 of the main article.

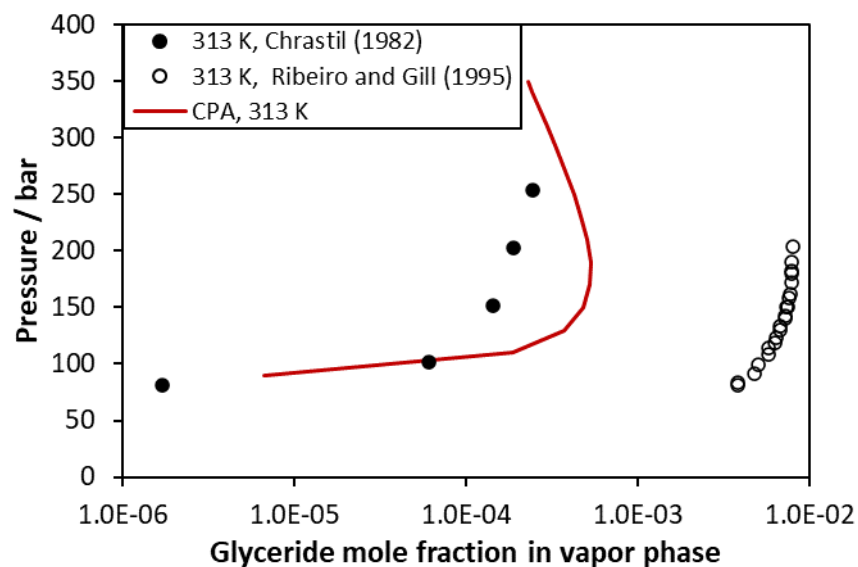


Figure S17. CO₂ – triolein VLE at 313 K (vapor phase compositions). Experimental data [53,54] and CPA correlations using the binary parameter of Table 5 of the main article.

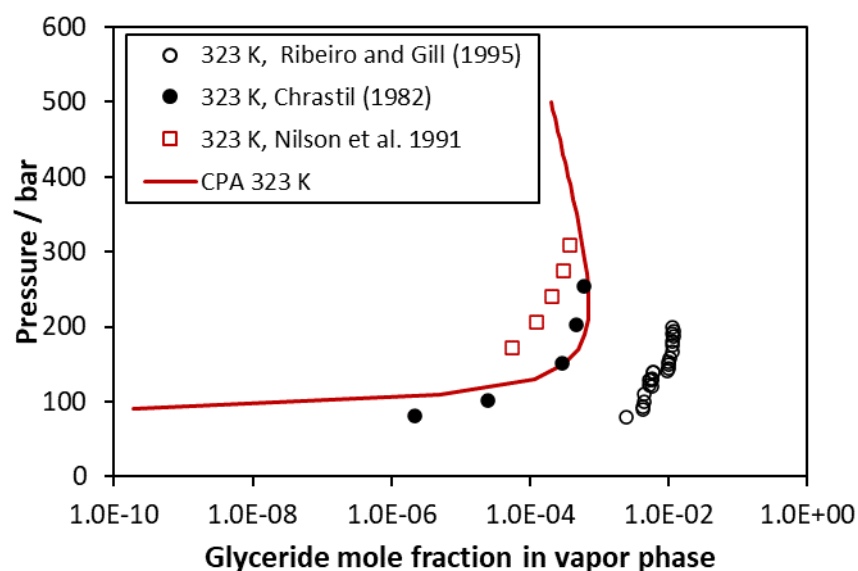


Figure S18. CO₂ – triolein VLE at 323 K (vapor phase compositions). Experimental data [50,53,54] and CPA correlations using the binary parameter of Table 5 of the main article.

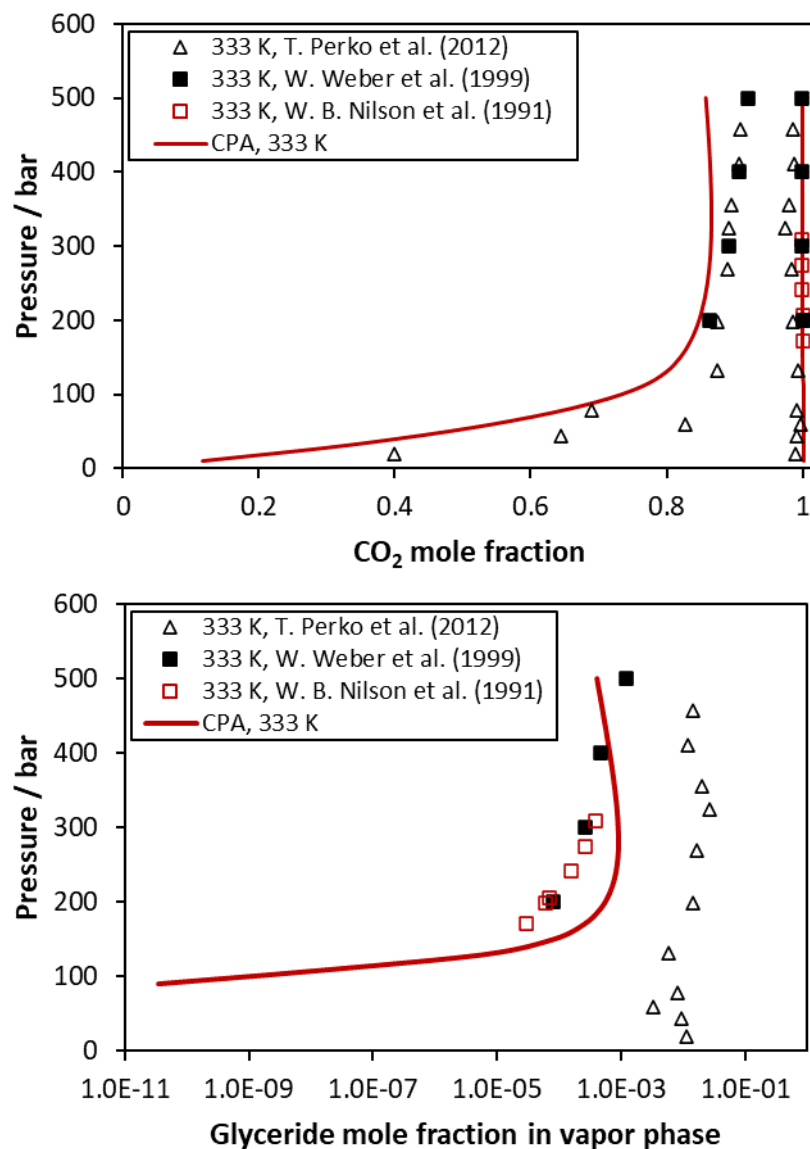


Figure S19. CO₂ – triolein VLE at 333 K. Experimental data [51-53] and CPA correlations using the binary parameter of Table 5 of the main article.

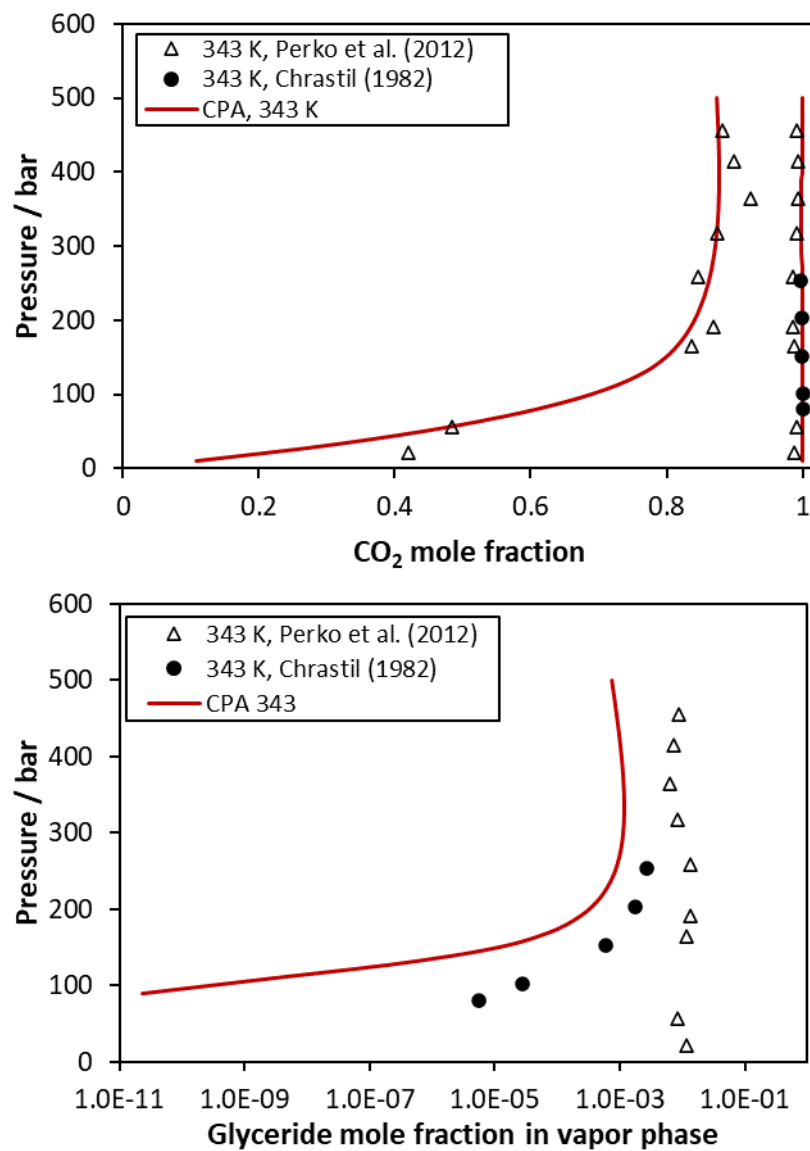


Figure S20. CO₂ – triolein VLE at 343 K. Experimental data [52,53] and CPA correlations using the binary parameter of Table 5 of the main article.