



Article

# Mayenite-Based Electride C12A7e<sup>-</sup>: A Reactivity and Stability Study

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**Abstract:** Ru supported on mayenite electride,  $[Ca_{24}Al_{28}O_{64}]^{4+}(e^-)_4$  a calcium aluminum oxide denoted as C12A7e<sup>-</sup>, are described in the literature as highly active catalysts for ammonia synthesis, especially under conditions of low absolute pressure. In this study, we investigated the application of recently reported plasma arc melting synthesized C12A7e<sup>-</sup> (aluminum solid reductant) as supports of Ru/C12A7e<sup>-</sup> catalysts in ammonia synthesis up to pressures of 7.6 MPa. Together with the plasma-arc-melting-based catalyst support, we investigated a similar plasma-synthesized C12A7e<sup>-</sup> (graphite solid reductant) and a vacuum-sintering-based C12A7e<sup>-</sup>. Complementary to the catalytic tests, we applied <sup>2</sup>H solid-state NMR spectroscopy, DRUVVis-spectroscopy, thermal analysis and PXRD to study and characterize the reactivity of different plasma-synthesized and vacuum-sintered C12A7e<sup>-</sup> towards H<sub>2</sub>/D<sub>2</sub> and H<sub>2</sub>O. The catalysts showed an immediate deactivation at pressures > 1 MPa, which can be explained by irreversible hydride formation at higher pressures, as revealed by reactivity tests of C12A7e<sup>-</sup> towards H<sub>2</sub>/D<sub>2</sub>. The direct formation of C12A7:D from C12A7e<sup>-</sup> is proven. It can be concluded that the application of Ru/C12A7e<sup>-</sup> catalysts at the industrial scale has limited prospects due to irreversible hydride formation at relevant pressures > 1 MPa. Furthermore, we report an in-depth study relating to structural changes in the material in the presence of H<sub>2</sub>O.

**Keywords:** mayenite; electride; calcium aluminates; catalyst support; ruthenium; ammonia synthesis; catalyst deactivation; hydride ions

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#### 1. Introduction

Ammonia synthesis is one of the major processes in the chemical industry and the established Haber–Bosch process is already more than 100 years old [1–3]. For industrial applications, Fe-based catalysts are mainly used, which trace back also to the early studies of Mittasch [4]. In industrial conditions, this process is typically carried out in a

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temperature range of 673 to 773 K and pressures of above 15 MPa [5]. Another catalyst family that has also found industrial use is Ru as an active metal supported on carbon with promoters: these types of catalyst can be applied and are of general interest as they are more active compared to Fe-based catalysts at lower temperatures, therefore offering a process-advantage [6]. For Fe-based catalysts,  $N_2$  dissociation is considered as the rate-determining step of the reaction happening on seven coordinated Fe-sites [7–9]. For the Ru-based catalyst, a similar structure sensitivity is reported, and step sites of the Ru surface are considered as favorable sites while the  $N_2$  dissociation is also assumed as a rate-determining step [10–14]. However, Ru-based ammonia synthesis catalysts typically suffer from poisoning by  $H_2$  limiting the performance at higher pressures, which is explained by the competitive adsorption of  $N_2$  and  $H_2$  on Ru [6,15,16].

Overcoming the aforementioned challenges, and accordingly improving the potentials of Ru-based catalysts, the group of Hosono reported that Ru supported on a novel support material, namely, may enite electrides— $[Ca_{24}Al_{28}O_{64}]^{4+}(e^{-})_4$ —in combination, results in catalysts that are described as highly active for ammonia synthesis [17,18]. The electride support material  $[Ca_{24}Al_{28}O_{64}]^{4+}(e^{-})_4$ , denoted as C12A7e<sup>-</sup>, was reported to be stable up to 673 K under atmospheric conditions. C12A7e<sup>-</sup> is based on the mayenite structure, as first reported by the group of Hosono [19–21]. Mayenite is a calcium aluminum oxide, which can be described by a positively charged framework of 12 cages  $[Ca_{24}Al_{28}O_{64}]^{4+}$  with anions distributed inside the cages compensating for the charge, in case of the oxygen mayenite  $[Ca_{24}Al_{28}O_{64}]^{4+}(O^{2-})_2$ , denoted as C12A7 [22–27]. For the mayenite structure, several anionic species are reported, e.g., OH<sup>-</sup> [28–30], H<sup>-</sup> [19,29,31–34], N<sup>3-</sup> [35], NH<sub>2</sub><sup>-</sup> [35,36] and NH<sup>2-</sup> [37]. Mayenite-based electrides  $[Ca_{24}Al_{28}O_{64}]^{4+}(2 \times \delta)e^{-}(2 - \delta)O^{2-}$  show interesting properties depending on the electron concentration N<sub>e</sub>. The material can, in fact, be an insulator (colorless,  $\delta = 0$ ,  $N_e = 0$  cm<sup>-3</sup>), semi-conductor (green color,  $\delta < 1$ ,  $N_e$  < 1 imes 10<sup>21</sup> cm<sup>-3</sup>) or metallic conductor (very dark or black,  $\delta$  > 1,  $N_e$  > 1 imes 10<sup>21</sup> cm<sup>-3</sup>) with a maximum possible  $N_e = 2.3 \times 10^{21}$  cm<sup>-3</sup> [20–22,38]. The metallic conducting C12A7e<sup>-</sup> exhibits a work function of 2.4 eV [39].

Due to the "promoting" properties of the electride support, the group of Hosono reported that the rate-determining step of ammonia synthesis over Ru/C12A7e<sup>-</sup> was not the dissociation of N<sub>2</sub>, but rather the subsequent formation of N-H<sub>x</sub> species. At the same time, it was observed that the nature of the reaction mechanism depends on the electron concentration of the mayenite electride support [31,40]. The group concluded that a metallic conducting electride is required for superior activity, and its action is explained as an "electronic promoter" for Ru, and that the  $H_2$  poisoning could be overcome by the reversible incorporation and release of H<sup>-</sup> into the electride structure [17,18,31,40]. The reported turnover frequency (TOF) of 0.98 s<sup>-1</sup> for this catalyst is more than one order of magnitude higher than that of comparable, conventional Ru-Ba/activated carbon or Ru-Cs/MgO catalysts [18]. However, they reported the catalytic test results only for pressures up to 1.3 MPa [17,18], which is considerably lower than industrially relevant conditions [5]. A recent work of Kammert et al. investigated the role of hydrogen for this catalyst in detail with in situ neutron-scattering techniques and found that the suggested reversible incorporation and release of H<sup>-</sup> in the mayenite structure does not play a major role in the mechanism in contrast to the findings of the group of Hosono [17,32]. They further applied steady-state isotopic transient kinetic analysis with isotopically labelled nitrogen to determine the number of reactive nitrogen intermediates on the catalyst surface, reporting that the promoting effect of the electride support enables much higher coverages of Ru by adsorbates compared to use of the oxygen mayenite support (coverages 84% vs. 15%, respectively) [32]. Thus, the promoting properties of the electride are crucial for the enhanced performance of the material to prevent poisoning by H<sub>2</sub> and not a reversible uptake and release of hydrogen in the mayenite structure.

The synthesis of metallic conducting C12A7e<sup>-</sup> was initially achieved by the reaction of C12A7 with Ca at 973 K for 240 h in evacuated silica tubes [21]. Later, other solid-reductants or synthesis procedures were applied, as reviewed by Kim et al., Salasin et al.,

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or Khan et al. [20,22,38]. Potential scalable synthesis procedures of powdered C12A7e-, readily applicable as catalyst supports with high electron concentrations, were only recently reported. This includes stoichiometric synthesis from CaO, Al<sub>2</sub>O<sub>3</sub>, Al at 1373 K for 8 h under Ar [41], or plasma-arc-melting synthesis with the addition of solid reductants like Al or graphite, which yielded C12A7e<sup>-</sup> within less than 1 min [42]. The synthesis of the stoichiometric hydride C12A7:H is possible starting from C12A7 by reaction with CaH<sub>2</sub> or TiH<sub>2</sub> at 1073 K for > 120 h in sealed silica tubes [29,34]. Non-stoichiometric hydrides, still containing O<sup>2-</sup>, OH<sup>-</sup> or e<sup>-</sup>, were reported for the reaction of C12A7 or C12A7e<sup>-</sup> with gaseous  $H_2$  [19,29,31–34]. The hydrogen uptake of Ru/C12A7e<sup>-</sup> and C12A7e<sup>-</sup> by temperature-programmed absorption, as studied by Kitano et al., showed that, for the Ru-containing sample, the uptake occurs at lower temperatures, with a maximum of ca. 100 K lower at about 750 K, compared to the pure C12A7e<sup>-</sup> [31]. It should be noted that, in temperature-programmed desorption experiments, it was found that H<sub>2</sub> was also released at lower temperatures for the Ru/C12A7e<sup>-</sup> sample compared to C12A7e<sup>-</sup> and at lower temperatures than the absorption [31]. The mayenite materials are typically hygroscopic, while the reaction of C12A7e<sup>-</sup> with H<sub>2</sub>O was only recently reported by Jiang et al., showing the formation of  $Al_2Ca_4(OH)_{12}$  and slight amounts of  $Al(OH)_3$  [43]. Thus, potential stability issues of the Ru/C12A7e<sup>-</sup> catalyst towards H<sub>2</sub>O were not frequently reported. To the best of our knowledge, the only records are a review and a study on a new potential electride support for ammonia synthesis Y<sub>5</sub>Si<sub>3</sub>—but no detailed information on the nature of the water instability of the mayenite electride materials is provided in these publications [17,44].

To date, the studies of the catalytic performance of Ru/C12A7e $^-$  reported in the literature were only conducted under model laboratory conditions with low pressures of less than 1.3 MPa [17,18,31,32,40]. Studies under relevant industrial operation conditions, especially higher pressures, of the catalyst in ammonia synthesis, are desirable to evaluate its potential in industrial applications. In the present study, we first report the application of Ru/C12A7e $^-$  catalysts under ammonia synthesis conditions close to atmospheric, and at elevated pressures, to investigate all industrial-relevant operation conditions. The mayenite electride support materials were obtained by plasma-arc melting of mayenite starting materials, as reported here [42]. We further investigated the C12A7e $^-$  support material through reactivity studies towards  $H_2/D_2$  under atmospheric pressure and higher pressure to better understand the issues concerning the catalyst stability and potential deactivation mechanism by hydride formation. The studies are complemented by hydrothermal reactivity experiments of C12A7 and C12A7e $^-$  to assess the stability towards  $H_2O$ .

# 2. Results and Discussion

In this study, we investigated the activity, reactivity, and stability of different C12A7e<sup>-</sup> samples prepared by two different synthetic routes. The relevant samples are summarized in Table 1 and can be divided into four groups: 1. Plasma-synthesized C12A7 and C12A7e<sup>-1</sup> samples (a)-(d), 2. Vacuum-sintering-based sample (e), 3. Ru supported on C12A7 and C12A7e<sup>-</sup> (f)–(i) based on samples of the plasma treatment route (I), and 4. hydride (j) and deuteride (k) of the vacuum-sintering-based C12A7e<sup>-</sup>. The prepared C12A7e<sup>-</sup> samples (c)-(e) are of dark green color, which can be attributed to semiconducting close to metallicconducting C12A7e<sup>-</sup> samples according to the literature and a previous study on plasma-treatment-based C12A7e<sup>-</sup> (electron concentration N<sub>e</sub> from approximately 0.1 to  $1.2 \cdot 10^{21}$  cm<sup>-3</sup>) [20–22,38,42]. The plasma-treatment-based samples (a) and (d) are used for reactivity and stability experiments under hydrothermal conditions. (d) and (e) were tested regarding their reactivity towards hydrogen and possible hydride/deuteride formation. Catalytic activity tests were performed for the plasma-based samples (g) and (h), while sample (i) was used to investigate whether the electride properties are still present after Ru deposition. The samples (j) and (k) were obtained from high-pressure hydrogenation experiments in the DSC or autoclave.

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Sample <sup>1</sup>	Color of Powder	Solid Reductant		
(a) C12A7	colorless	-		
(b) C12A7e <sup>-</sup> (5Al)	light green	5 wt.% Al		
(c) C12A7e <sup>-</sup> (20Al)	dark green	20 wt.% Al		
(d) $C12A7e^{-}$ (3C)	dark green	3 wt.% graphite		
(e) C12A7e <sup>-</sup> (SSR)	dark green	-		
(f) Ru/C12A7	gray	-		
(g) $Ru/C12A7e^{-}$ (5Al)	gray	5 wt.% Al		
(h) Ru/C12A7e <sup>-</sup> (20Al)	dark gray	20 wt.% Al		
(i) Ru/C12A7e <sup>-</sup> (3C)	dark gray	3 wt.% graphite		
(j) C12A7:H	colorless	-		
(k) C12A7:D	colorless	-		
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**Table 1.** C12A7e<sup>-</sup> samples studied in this work.

In the following sections, we will first discuss the deposition of Ru on plasma-synthesized C12A7e<sup>-</sup> samples, followed by the catalytic testing of those materials in ammonia synthesis. This is complemented by reactivity and stability studies of the electride materials concerning hydrogenation and hydrothermal conditions.

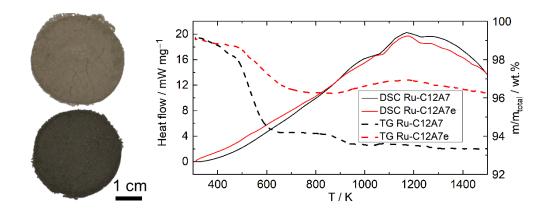
## 2.1. Ruthenium Deposition

The deposition of Ru was carried out as adapted from the literature procedure of Kitano et al. [18]. Four different Ru-loaded samples (f)–(i), based on C12A7 and C12A7e<sup>-</sup> prepared by plasma synthesis (a)–(d), are discussed in this work. For catalytic tests, the Al-based samples (g) and (h) were used, while the pure C12A7 (f) and the graphite-based electride (g) were used to test if the material still qualified as an electride after Ru deposition. The quantitative Ru deposition on the samples was confirmed by XRF analysis. After Ru deposition, the color changed from colorless to gray in case of samples (a) and (f), where the pure oxygen mayenite C12A7 was present. For samples with Ru deposited on C12A7e<sup>-</sup>, the color changed to dark gray. The obtained powders of samples (f) Ru/C12A7 and (i) Ru/C12A7e<sup>-</sup> (3C) are shown in Figure 1, illustrating the color difference between the respective supports. Both samples were also studied by STA analysis in synthetic air, with the DSC and TG curves shown in Figure 1. For both samples, a mass loss can be observed starting at about 500 K, while the mass loss is greater for the Ru/C12A7 sample compared to the C12A7e<sup>-</sup>-based one. We expect this mass loss to be caused by either not fully decomposed Ru<sub>3</sub>(CO)<sub>12</sub> precursors or by the release of adsorbed H<sub>2</sub>O, or both. At about 900 K, the TG curves for the two samples differ, as the Ru/C12A7e<sup>-</sup> sample shows a mass uptake with a maximum of about 1150 K. This mass uptake can be assigned to the transformation of C12A7e<sup>-</sup> to C12A7. The maximum and the temperature region are well in line with previous studies on plasma-treatment-based C12A7e<sup>-</sup> and the literature values [42,45–47], indicating that the C12A7e<sup>-</sup> is still present after Ru deposition. In the DSC curves, no clear signal for both samples can be observed.

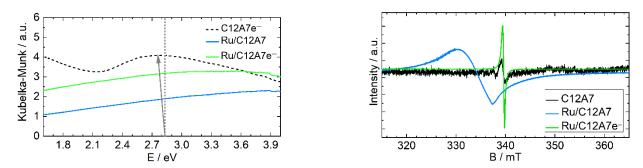
To further investigate the presence of C12A7e<sup>-</sup> after Ru deposition, the samples (f) Ru/C12A7 and (i) Ru/C12A7e<sup>-</sup> (3C) were characterized by DRUVVis and EPR spectroscopy, as shown in Figure 2. The DRUVVis spectra are shown together with the spectra of the initial C12A7e<sup>-</sup> sample (d). One cannot observe the typical peak at around 2.83 eV for C12A7e<sup>-</sup> for the Ru-containing sample (i) [21]. However, it should be noted that the Kubelka–Munk intensity for the Ru/C12A7e<sup>-</sup> sample is significantly higher compared to the Ru/C12A7-based material. Based on the DRUVVis results, we cannot analyze the electron concentration of the Ru-containing samples and, also from DRUVVis, an unambiguous presence of C12A7e<sup>-</sup> after Ru deposition cannot be concluded.

<sup>&</sup>lt;sup>1</sup> (a)–(d) are prepared via plasma treatment and (e) is prepared via the solid-state reduction route. Samples (f)–(i) containing Ru are based on the plasma-synthesized samples (a)–(d). Samples (j) and (k) are the mayenite hydride and deuteride phases prepared from sample (e), respectively.

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**Figure 1.** (**Left top to bottom**): photographs of (f) 1.2 wt.%-Ru/C12A7 and (i) Ru/C12A7e<sup>-</sup> (3C) powders after Ru deposition. (**Right**): DSC (heat flow, exothermic up, solid) and TG (m/m<sub>total</sub>, dashed) curves under synthetic air for (f) shown in black and (i) shown in red. 10 mg of sample each was heated with a ramp of  $10 \text{ K} \cdot \text{min}^{-1}$  from RT to 1573 K.



**Figure 2.** (**Left**): Kubelka–Munk-transformed DRUVVis spectra for Ru-impregnated samples: blue (g) Ru/C12A7, green (i) Ru/C12A7e $^-$  (3C) and dashed (d) C12A7e $^-$  (3C). The dotted line at 2.83 eV corresponds to the absorption peak maximum for  $N_e = 1 \cdot 10^{18}$  cm $^{-3}$  [21]. The arrow indicates the shift with increasing  $N_e$ . (**Right**): first derivative EPR spectra for samples (a) C12A7 (black), (f) Ru/C12A7 (blue) and (i) Ru/C12A7e $^-$  (green) samples, intensities are not normalized.

The EPR spectra of the samples (f) and (i) are shown, together with the spectra of the pure C12A7 sample (a). The Ru/C12A7e $^-$  exhibits the typical EPR signal for the semiconducting electride at 339.5 mT. The normalized intensity  $I_{\rm N}$  of the signal is 410, which is significantly lower compared to the range from 2500 to 4825, as reported for pure C12A7e $^-$  (3C) samples obtained from plasma treatment [42]. For sample (f) Ru/C12A7, a different signal at lower magnetic field strength of 334.5 mT is observed, which cannot be attributed to C12A7e $^-$ .

Based on the results obtained from STA, DRUVVis and EPR analysis, it can be concluded that after Ru deposition on the plasma-synthesized C12A7e $^-$  samples, the material still corresponds to the semiconducting C12A7e $^-$ . However, the electron concentration seems to have decreased, as indicated by the  $\rm I_N$  of the EPR spectra and the absence of a clear absorption peak within the DRUVVis experiments. PXRD (Figure S2) of the samples (g) and (i) after Ru deposition do not show changes compared to the used C12A7 and C12A7e $^-$  samples, while no distinct Ru reflections could be observed, indicating X-ray-amorphous deposition of the Ru on the support material, which could be confirmed as shown in the TEM image in Figure S1.

# 2.2. Reactivity Studies of C12A7 and C12A7e<sup>-</sup>

#### 2.2.1. Catalytic Studies of Ru/C12A7e<sup>-</sup>

The catalytic activity of the two Ru/C12A7e<sup>-</sup> catalysts (g) and (h) was tested in ammonia synthesis. Both catalysts are based on plasma-synthesized C12A7e<sup>-</sup> with Al

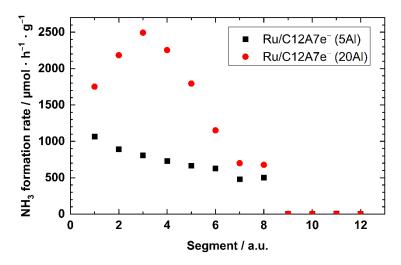
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used as a solid reductant. Sample (h) exhibited a higher electron concentration compared to (g), as indicated by the color difference, while sample (g) is a semiconducting material, and (h) is expected to be semiconducting close to metallic conduction, as reported in the literature [42,45-47]. The two samples were tested under different reaction conditions of ammonia synthesis, denoted as segments, with varied reaction temperatures and pressures, as listed in Table 2. The tested temperatures ranged from 593 to 673 K, and the pressure from 0.1 up to 7.6 MPa. The NH<sub>3</sub> formation rate for all testing conditions of the two catalysts is shown in Figure 3.

**Table 2.** Reaction conditions for catalytic experiments of two 1.2 wt.% Ru/C12A7e<sup>-</sup> catalysts based on plasma synthesized C12A7e<sup>-</sup>, (g) Ru/C12A7e<sup>-</sup> (5Al) and (h) Ru/C12A7e<sup>-</sup> (20Al).

Segment	1	2	3	4	5	6	7	8	9	10	11	12
T/K	673	653	633	623	613	603	593	633	633	633	633	633
p/Mpa	0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	1.1	3.1	6.1	7.6

5 g catalyst, 350–500  $\mu$ m sieve fraction, 5 mL catalyst bed volume, total flow 4.0126 mol·h<sup>-1</sup>, 3:1 H<sub>2</sub>:N<sub>2</sub>.



**Figure 3.** NH<sub>3</sub> formation rate of two different plasma-synthesized 1.2 wt.%  $Ru/C12A7e^-$  catalysts in ammonia synthesis, black (g)  $Ru/C12A7e^-$  (5Al) and red (h)  $Ru/C12A7e^-$  (20Al). The testing conditions for each segment are summarized in Table 2.

For segments with reaction pressures of 0.1 Mpa, both samples are highly active catalysts in ammonia synthesis. However, their specific activity appears to be different. While the sample with lower electron concentration (g) Ru/C12A7e $^-$  (5Al) has its maximum activity at 673 K, with an NH $_3$  formation rate of 1066  $\mu$ mol  $h^{-1}$  g $^{-1}$ , the catalyst (h) exhibits its highest activity at 633 K, with 2493  $\mu$ mol  $h^{-1}$  g $^{-1}$ . This rate is well in agreement with the value reported by Kitano et al. of 2730  $\mu$ mol  $h^{-1}$  g $^{-1}$  for an Ru/C12A7e $^-$  catalyst with a similar loading of 1.2 wt.% Ru [31]. In the first reported application of the material for NH $_3$  synthesis, by the group of Hosono et al., they reported a rate of 2760  $\mu$ mol  $\cdot$   $h^{-1}$  · g $^{-1}$  for a 1.2 wt.% Ru/C12A7e $^-$  sample at 673 K, which is a slightly higher activity than the Ru/C12A7e $^-$  (20Al) sample discussed here [18]. Comparing the Ru/C12A7e $^-$  (5Al) and (20Al) we can observe differences in their activity, which we attribute to the different electron concentration of the material, based on the color appearance of the precursor C12A7e $^-$ . This observation is in line with the previous studies of Kanbara et al., who showed the dependence of the activity of Ru/C12A7e $^-$  catalysts for NH $_3$  synthesis on the electron concentration of the C12A7e $^-$  support [40].

A remarkably different behavior of the Ru/C12A7e<sup>-</sup> (5Al) and (20Al) samples compared to studies of the group of Hosono can be observed for tests at higher pressures. In the available reports, test results of the materials were only reported for pressures up to

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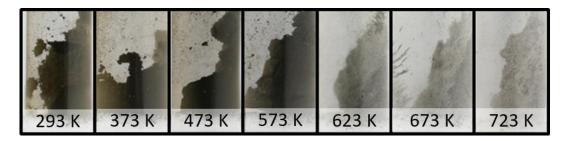
1.3 Mpa at 673 K [17,18]. As soon as Ru/C12A7e<sup>-</sup> (5Al) and (20Al) were tested at 633 K and higher pressures of >1.0 Mpa, an immediate decrease in the NH<sub>3</sub> formation is observed, as shown in Figure 3, for both catalysts. Kitano et al. reported an increase in activity by increasing the pressure from 0.1 to 1.0 Mpa at 673 K [18]. From the catalytic testing results, we assume that the immediate deactivation is caused by the transformation of an mayenite electride to a mayenite-based hydride phase (C12A7:H), where, instead of electrons, the cages are occupied with H<sup>-</sup> ions. This behavior contrasts with the studies of the group of Hosono at low pressures. The group investigated the H<sub>2</sub> uptake of the catalyst material by reaction with H<sub>2</sub> (H<sub>2</sub>(75 kPa), Ar(25 kPa), 633 K) and during reaction conditions (H<sub>2</sub>(75 kPa), Ar(25 kPa), 633 K), which suggested that only 1% of the electrons react with hydrogen to H<sup>-</sup> under reaction conditions, while under H<sub>2</sub>/Ar conditions 50% of the electrons are exchanged after 40 h [31]. With H<sub>2</sub> uptake experiments and kinetic studies, they concluded that H<sub>2</sub> is reversibly incorporated into the cages of the mayenite structure and prevents the poisoning of Ru with H2 under these reaction conditions, concluding that the Ru/C12A7e<sup>-</sup> catalyst is stable for NH<sub>3</sub> synthesis [17,18,31]. Kammert et al. studied the H<sub>2</sub> and D<sub>2</sub> uptake of Ru/C12A7e<sup>-</sup> by in situ neutron diffraction and steady-state isotopic transient kinetic analysis. They concluded that H<sub>2</sub> and D<sub>2</sub> in the cages are not likely to participate in the reaction mechanism, as only a minor exchange is observed, and a rather high possible coverage of adsorbed species on Ru is the reason for the poisoning resistance and enhanced activity [32]. However, their experiments were not carried out at pressures higher than 0.1 Mpa. In combination with these findings, we tend to explain the immediate loss of activity upon higher pressures as caused by the irreversible transformation of the mayenite electride into a mayenite-based hydride C12A7:H, causing a loss of the promoting properties of the electride for Ru, and thus causing an irreversible H<sub>2</sub> poisoning in the reaction. Based on these findings, we conclude that, despite Ru/C12A7e<sup>-</sup> showing a promising and remarkable performance at ambient pressure for ammonia synthesis, as pioneered by the group of Hosono, for application under industrial-relevant conditions of higher pressures of >1.0 Mpa, no sustained activity retention is observed. The catalyst exhibits stability issues due to bulk structural transformation, and thus the material is probably not suitable for application in the established ammonia synthesis process. To further understand the reactivity of the C12A7e<sup>-</sup> support, and to obtain a better understanding of the stability issues from a materials basis, in the following sections we discuss reactivity studies on  $H_2$  and  $H_2O$ .

# 2.2.2. Reactivity towards Forming Gas and Hydrogen

The reactivity of C12A7e $^-$  towards hydrogen was tested in a broad range of temperatures (i) in a tube furnace system in the presence of forming gas at 0.1 Mpa; (ii) by simultaneous thermal analysis (STA) in the presence of forming gas at 0.1 Mpa; (iii) in a DSC experiment under  $H_2$  up to 6.7 Mpa; (iv) by autoclave reaction with deuterium gas at 6 Mpa and 773 K.

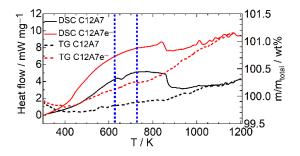
Initial reactivity tests of C12A7e $^-$  towards hydrogen were performed in a tube furnace system at temperatures up to 723 K and 0.1 Mpa in a 95%  $N_2/5\%$  H $_2$  atmosphere. The experiments were carried out with the plasma-synthesized C12A7e $^-$  (d), and the resulting pictures of the powder after treatment at different temperatures are shown in Figure 4. Starting from 623 K, one can observe a decolorization of the powder from dark green to grayish, which becomes more significant at higher temperatures. A similar experiment was carried out for the C12A7e $^-$  (d) sample by heating in  $N_2$  instead of  $N_2/H_2$  atmosphere, where no detectable decolorization compared to the  $N_2/H_2$  atmosphere could be observed. A similar grayish color for C12A7:H is reported by Jiang et al. [33], while an onset of  $H_2$  consumption in temperature-programmed absorption studies is observed at similar temperatures by Kitano et al. [31], as indicated by the color change in Figure 4 for the present study.

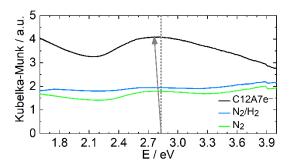
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**Figure 4.** Reactivity test series of (d) C12A7e<sup>-</sup> (3C) under forming gas  $(95\% N_2/5\% H_2)$  atmosphere inside the quartz-glass tube. From left to right: pictures of the sample after heating for each 1 h at the respective temperature.

The reactivity of the plasma synthesized C12A7 (a) and C12A7e $^-$  (d) was further investigated by simultaneous thermal analysis (STA). STA experiments were carried out under a forming gas atmosphere (95% N<sub>2</sub>/5% H<sub>2</sub>). The results are shown in Figure 5 (left). For both samples, a mass uptake in the TG could be observed, though the uptake is larger for the C12A7e $^-$  sample. The difference between both samples is pronounced in the region where the color change, as shown in Figure 4, takes place for the C12A7e $^-$  sample. The DSC curves for both samples do not show any significant signals in the region from 300 to 800 K. From the TG results, we conclude that the reaction of C12A7e $^-$  with H<sub>2</sub> starts at 600 K. Thus, the STA results support the findings of the initial reactivity studies.





**Figure 5.** (**Left**): DSC (heat flow, exothermic up, solid) and TG (m/m<sub>total</sub>, dashed) curves under forming gas (95% N<sub>2</sub>/5% H<sub>2</sub>) for (d) C12A7e<sup>-</sup> (3C) shown in red and (a) C12A7 shown in black. 10 mg of sample each were heated with a rate of 10 K · min<sup>-1</sup> from RT to 1173 K. The dotted blue lines indicate the region of the color change for C12A7e<sup>-</sup> as shown in Figure 4. (**Right**): Kubelka–Munk-transformed DRUVVis spectra for (d) C12A7e<sup>-</sup> (3C) shown in black and the resulting powders after reactivity tests at 723 K under forming gas (blue) and N<sub>2</sub> (green). The dotted line at 2.83 eV corresponds to the absorption peak maximum for N<sub>e</sub> =  $1 \cdot 10^{18}$  cm<sup>-3</sup> [21]. The arrow indicates the shift with increasing N<sub>e</sub>.

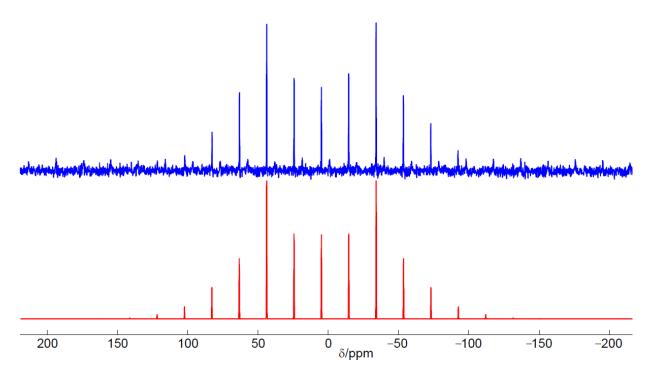
The samples studied in the tube furnace under  $N_2/H_2$  and  $N_2$  atmosphere were characterized by DRUVVis, as shown in Figure 5 (right). For the sample which was treated in  $N_2/H_2$  atmosphere, no clear absorption band of around 2.8 eV can be identified. This indicates a strong decrease in the electron concentration and loss of the electride properties. The sample treated under  $N_2$  atmosphere still exhibits the absorption band around 2.8 eV, as in the initial C12A7e<sup>-</sup>; however, the intensity is decreased, and the band is not as pronounced as before. The intensity decrease indicates a reduction in the electron concentration, as reported by Matsuishi et al. [21].

Complementary to the initial reactivity tests with plasma-synthesized C12A7e $^-$  (d), the reactivity towards  $H_2$  was tested for the vacuum-sintering-based C12A7e $^-$  (e) sample at higher pressures. For this purpose, initial tests were carried out in a DSC experiment under  $H_2$  pressure (5.0 to 6.7 MPa, up to 700 K), while the C12A7:D sample was prepared in an autoclave synthesis (6.0 MPa, 773 K). The hydrogenation in the DSC apparatus did not show any thermal effects, similar to the results we obtained for the plasma-synthesized samples, as shown in Figure 5 (left). However, the color change from green vacuum-sintered (e) C12A7e $^-$  to colorless (j) C12A7:H clearly indicates a reaction during the DSC

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experiment. The reaction of green vacuum-sintered C12A7e $^-$  with deuterium led to a small change in the lattice parameter from a = 11.9790(2) Å for sample (e) C12A7e $^-$  to a = 11.9874(1) Å for the colorless sample (k) C12A7:D (Figures S3 and S4) used in  $^2$ H solid-state NMR spectroscopy. The color change directly indicates the reaction of the C12A7e $^-$  with deuterium gas, which is accompanied by the loss of the electride properties.

To clarify the presence of deuteride anions within C12A7:D,  $^2$ H NMR studies were performed. The  $^2$ H solid-state NMR spectrum of C12A7:D in Figure 6 shows a quadrupolar line shape with an isotropic chemical shift of 4.8 ppm, a quadrupolar coupling  $C_Q$  of 16 kHz and an asymmetry parameter  $\eta$  of 0. The quadrupolar parameters indicate a covalent character of the deuteride, while the coupling strength is rather weak. The latter suggests a non-cubic symmetry around the hydride (deuteride) ion, giving rise to the quadrupolar coupling. There are indications for a minor site with a large quadrupolar coupling of 145 kHz and an isotropic chemical shift of -1 ppm, which we assign to an OD $^-$  group, such as mayenite hydroxide. The observed chemical shifts compare well with the literature data [29]. Therefore, we assume the sample to be mayenite hydride (deuteride) with some minor amount of OD $^-$  groups in the clathrate cages. Mayenite hydride may thus be synthesized not only by the known routes, from C12A7/C12A7e $^-$  and CaH $_2$  [34] or C12A7 and TiH $_2$  [29], but also by direct hydrogenation of C12A7e $^-$  at elevated hydrogen gas pressures.

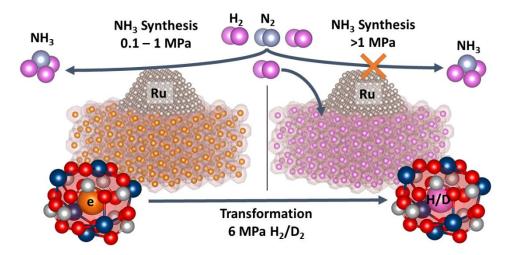


**Figure 6.** <sup>2</sup>H-NMR spectrum of the deuteride sample from the hydrogenation experiment in the autoclave (k) C12A7:D (blue) together with the fitted spectrum (red).

Kammert et al. investigated the reaction of Ru/C12A7e $^-$  with H $_2$ /D $_2$  at atmospheric pressure, but showed no complete exchange of e $^-$  by H $^-$  [32]. They instead found that, under atmospheric pressure, the amount of H $^-$  incorporated in C12A7e $^-$  increases by raising the temperature from 673 to 873 K, concluding that, under reaction conditions, the electride properties are maintained, as the C12A7e $^-$  does not completely react with H $_2$  [32]. The group of Hosono proposed that H $^-$  is incorporated in small amounts into the cages at the initial stages of ammonia synthesis, but the cage H $^-$  ions are readily released by the following reaction: H $^- \to H^0 + e^-$  [17,18]. However, our findings from the catalytic activity tests and the reactivity studies towards H $_2$  at higher pressures support the initial assumption that the catalyst deactivation is caused by the formation of C12A7:H

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under ammonia synthesis conditions at higher pressures. The results from the catalytic activity tests and reactivity studies are schematically shown in Scheme 1. If ammonia synthesis is carried out at mild pressures below 1 MPa, no bulk transformation of C12A7e<sup>-</sup> to C12A7:H takes place. An increase in pressure leads to the formation of bulk C12A7:H, which is accompanied by a loss of the electride properties and, thus, loss of performance in ammonia synthesis.



**Scheme 1.** Illustration of the pressure-dependent behavior of the Ru/C12A7e<sup>-</sup> catalyst during ammonia synthesis (top part) and the C12A7e<sup>-</sup> during hydrogenation experiments (bottom part). For graphical illustration, each cage contains an electron or hydride/deuteride, while maximum 1/3 of the cages are occupied in the stoichiometric compounds.

It can be speculated that, at low pressures, the mechanism proposed by the group of Hosono [17,18,31,40], involving a partial and dynamic exchange of hydrogen between active metal and support, leads to an activity enhancement, and follows only a partial and still-reversible exchange between mayenite electride and hydride in the upper surface layers. Once the pressure is increased and the bulk phase is transformed into the hydride phase, the beneficial promoting properties are lost. With the loss of the promoting properties, the activity of the catalyst is strongly reduced, which was also found by Kammert et al. [32] and the group of Hosono [17,18,40], with mayenite type supports with no- or low-electron concentrations.

# 2.2.3. Hydrothermal Reactivity Tests

The hydrothermal reactivity was tested for plasma-synthesized samples (a) C12A7 and (d) C12A7e $^-$ . To study the general stability of the mayenite structure, the Ar plasma-synthesized C12A7 sample (a) was exposed to H<sub>2</sub>O, as described in the experimental section. The PXRD of the resulting powder after each exposure time is shown in Figure 7. Even after only one hour of exposure to H<sub>2</sub>O at ambient conditions, we could observe structural changes in the material by the formation of a secondary phase identified as Al<sub>2</sub>Ca<sub>4</sub>(OH)<sub>12</sub>CO<sub>3</sub> · 5H<sub>2</sub>O (orange dashed–dotted lines in Figure 7) and an unidentified phase (red dotted lines in Figure 7), accompanied by a reduction in the intensity of the C12A7 reflections. After 5 h exposure to H<sub>2</sub>O, we could observe a complete decomposition of the C12A7 structure in the PXRD patterns by the absence of C12A7 reflections, while the reflections of the unidentified phase (red dotted lines) disappear in conjunction with the occurrence of another unidentified phase. Figure 7 also shows that, when the C12A7e<sup>-</sup> sample was exposed to H<sub>2</sub>O for 16 h, the color of the sample changed from dark green to gray, which indicates a loss of electride properties.

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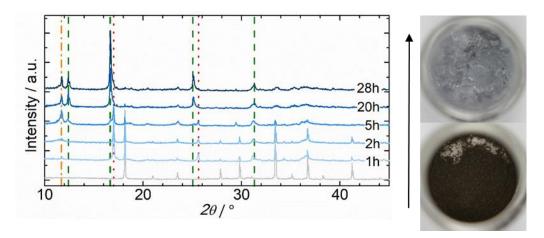


Figure 7. (Left): PXRDs for the reactivity test series of sample (a) C12A7 in  $H_2O$  under ambient conditions for different reaction times after drying at 80 °C for 30 min. The diffraction pattern before hydrothermal treatment (grey) shows only reflections of C12A7;  $Al_2Ca_4(OH)_{12}CO_3 \cdot 5H_2O$  (orange dashed–dotted), unidentified phase (green dashed), and unidentified phase (red dotted lines) are present until a reaction time of 5 h. (**Right**): Photographs of the resulting samples from the reactivity test experiment for (d) C12A7e<sup>-</sup> (3C) under  $H_2O$  at room temperature. Initial C12A7e<sup>-</sup> powder (bottom) and reacted powder (top) after 16 h under  $H_2O$ .

To exclude the potential influence of the atmosphere and for a more defined mixing, the stability experiments were additionally carried out under more controlled conditions. For this, the C12A7e<sup>-</sup> (d) sample was suspended in tetrahydrofuran (THF) under Ar atmosphere. After suspending the material for 5 min in THF, the color of the powder was still dark green and did not change compared to the initial C12A7e<sup>-</sup> sample. After the stepwise addition of H<sub>2</sub>O, the sample changed its color to white, which may indicate a decomposition of the C12A7e<sup>-</sup>. In the PXRD shown in Figure 8, a complete decomposition of the C12A7 structure and the formation of mainly katoite Al<sub>2</sub>Ca<sub>3</sub>(OH)<sub>12</sub> and some  $Al_2Ca_4(OH)_{12}CO_3 \cdot 5H_2O$ , after reaction of the  $C12A7e^-$  with  $H_2O$  in THF, can be observed. These results are similar to those found by Jiang et al. for hydrothermal reactivity experiments. They found Al<sub>2</sub>Ca<sub>3</sub>(OH)<sub>12</sub> and slight amounts of Al(OH)<sub>3</sub> by immersing the sample in H<sub>2</sub>O for 72 h or storing it under 100% relative humidity for 1 week. [43]. As we found additional aluminum calcium hydroxide phases in the experiments under ambient conditions, it could be possible that different decomposition pathways or stages of the C12A7 structure might exist under hydrothermal conditions. Hayashi et al. reported the formation of C12A7:OH upon reaction of C12A7 in a wet atmosphere without structural decomposition [28]. With respect to a potential broader application of the material in heterogeneous catalysis, the hydrothermal stability of the material might be crucial, especially for reactions where H<sub>2</sub>O is present as solvent or is produced as a reaction product. For the Ru/C12A7e<sup>-</sup> catalyst, the stability issues towards water have only been reported as an aside in a study of a water-stable electride, Y<sub>5</sub>Si<sub>3</sub> [17,44].

The results of the hydrothermal reactivity tests are summarized in Scheme 2. Upon contact with liquid  $H_2O$  and 100% relative humidity, the material exhibits a structural decomposition to calcium aluminum hydroxide phases, as shown by Jiang et al. and the results in the present study [43]. Based on the literature knowledge and our study, we conclude that an initial deactivation might be caused by an exchange of the electrons inside the cage and the formation of  $OH^-$  while, during longer exposures to  $H_2O$ , structural decomposition takes place. A more detailed investigation of the decomposition pathways of C12A7 by reaction with  $H_2O$  might be carried out by in situ PXRD studies for a more holistic picture and detailed understanding of the structural decomposition pathway.

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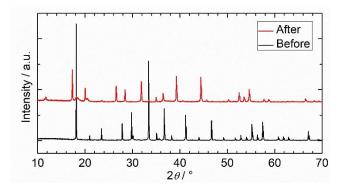
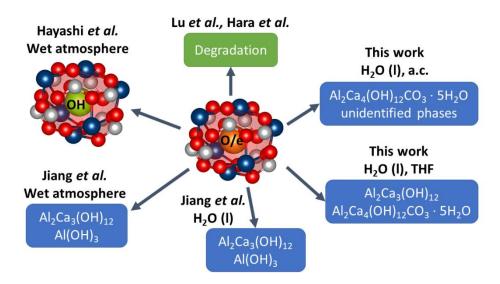


Figure 8. PXRDs for the reactivity test of (d) C12A7e<sup>-</sup> (3C) in THF with 5 mL  $H_2O$  addition after 72 h and following drying under vacuum. Initial diffraction pattern (black) shows C12A7 and minor krotite (CA) reflections. The PXRD after the experiment (red) shows mainly  $Al_2Ca_3(OH)_{12}$  reflections and minor  $Al_2Ca_4(OH)_{12}CO_3 \cdot 5H_2O$ .



**Scheme 2.** Illustration of the hydrothermal reactivity of C12A7e<sup>-</sup> as reported in the literature by Jiang et al. [43], Hayashi et al. [28], Lu et al. [44], Hara et al. [17] and the results from the present study. Ambient condition denoted as a.c. The material can either react by formation of OH<sup>-</sup> species in the cages or structural decomposition (blue boxes).

#### 3. Materials and Methods

3.1. Synthesis

#### 3.1.1. Synthesis of Electrides and Mayenite Hydrides

The electride samples used in this study were synthesized via two different procedures: (I) plasma synthesis and (II) solid-state reduction in a vacuum-sintering furnace.

Pathway (I), thoroughly detailed in a previous publication [42], consisted of mixing reagents to prepare the precursor, which was then calcined and mixed with a reductant prior to plasma treatment. The oxygen-mayenite precursor (C12A7) was prepared as reported earlier by mixing 56.91 g of Disperal P2 with 43.65 g of CaO and 150 mL of deionized  $\rm H_2O$  in a ball mill. The three reagents were mixed at 600 rpm four consecutive times, with alternating directions of rotation, each for 10 min and with a 5 min break in between. The obtained paste was calcined for 8 h at 1373 K with 10 K  $\cdot$  min  $^{-1}$  in a muffle furnace and a constant, clean dry-air flow. After the calcination step, the product was ground and characterized by powder X-ray diffraction (PXRD). For batches containing krotite (CA) and tricalcium aluminate (C3A) as the secondary phase, the product was calcined again to complete the reaction. The obtained C12A7 was mixed with a solid reductant and pressed

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into 13 mm pellets (about 0.5 g) with 10 t using a motorized pellet press. As solid reductants, Al powder (99.5% metal basis by Alfa Aesar) and graphite powder (C) (general purpose grade by Fischer Chemical) were used. Four different samples were prepared via plasma treatment of the following mixtures: (a) pure C12A7, (b) C12A7e $^-$  (5 wt.% Al), (c) C12A7e $^-$  (20 wt.% Al) and (d) C12A7e $^-$  (3 wt.% C). Plasma treatment was carried out in an arc furnace "Compact Arc Melter MAM-1" (Edmund Bühler GmbH) with a plasma intensity level of 5; see [42] for details regarding the plasma intensity. Before plasma treatment, the furnace chamber was flushed and evacuated three times with the desired gas mixture. Sample (a) was treated under Ar atmosphere, while samples (b)–(d) were treated under 95% Ar/5% H<sub>2</sub> with a chamber pressure of 0.07 MPa for both atmospheres. Sample (a) was plasma-treated three times from the top side and once from the bottom side for about 60 s each, until a homogeneous melting could be observed. Samples (b)–(d) were treated similarly, but only once from the top and bottom side, for about 60 s.

The electrides obtained from the vacuum sintering pathway (II) were synthesized as follows. C12A7 was prepared by a solid-state reaction of stoichiometric amounts of CaCO<sub>3</sub> (99%, ChemPur GmbH, Karlsruhe, Germany) and Al<sub>2</sub>O<sub>3</sub> (99.99%, ChemPur GmbH, Karlsruhe, Germany). The powders were first mixed with an agate mortar and pistil and afterwards pressed into pellets by a uniaxial hand-press (Perkin Elmer, 25 t). The pellets were heated in a chamber furnace (Nabertherm GmbH, Lilienthal, Germany) under air conditions for 16 h at 1573 K. Afterwards, they were transferred to a vacuum-sintering furnace (FCT-Anlagenbau, Sonneberg, Germany). Here, the pellets were treated under argon atmosphere at 1523 K for 4 h. The furnace chamber was heated through graphite electrical resistance, which caused the oxygen partial pressure to be extremely low, resulting in a reduction in the mayenite to the electride by loss of oxygen.

All samples obtained from plasma treatment and vacuum sintering are summarized in Table 1.

# 3.1.2. Ruthenium Deposition

Deposition of catalytic active Ru on C12A7 or (d) graphite-based C12A7e $^-$  obtained by pathway (I) was carried out with a chemical vapor deposition method by adapting the literature procedure [18]. As a ruthenium precursor, triruthenium dodecacarbonyl (Ru<sub>3</sub>(CO)<sub>12</sub>) (99%, Sigma Aldrich) was used. For impregnation, the precursors were transferred into an Ar-filled glove box. The plasma-treated C12A7 and C12A7e $^-$  powders were mixed with the desired amount of the ruthenium precursor in an agate mortar. The mixtures were then transferred into the TFM $^{TM}$ -PTFE inserts of DAB-3 autoclaves (Berghof Products + Instruments GmbH). The autoclaves were tightened by hand inside the glove box and closed outside the glove box with a torque of 40 Nm. The autoclaves were placed into a muffle furnace and heated with the following temperature program: heating to 313 K (1 h, 2 K  $\cdot$  min $^{-1}$ ), 343 K (1 h, 0.25 K  $\cdot$  min $^{-1}$ ), 393 K (2 h, 0.4 K  $\cdot$  min $^{-1}$ ) and finally 523 K (3 h, 0.9 K  $\cdot$  min $^{-1}$ ). After heating, the autoclave screws were loosened and the autoclaves were transferred into the glove box. The desired ruthenium content for all samples was 1.2 wt.%. The obtained samples are summarized in Table 1.

# 3.2. Characterization

Powder X-ray diffraction (PXRD) characterization was performed with a Bruker D8 Advance diffractometer with Bragg–Brentano geometry, a Lynxeye XE 1D-detector, a Cu-X-ray-tube with  $K_{\alpha 1}$   $\lambda$  = 154.06 pm and  $K_{\alpha 2}$   $\lambda$  = 154.44 pm and a ratio of  $K_{\alpha 1}$ : $K_{\alpha 2}$  = 2. The samples were thoroughly ground in an agate mortar and were measured on flat poly(methyl methacrylate) sample holders. PXRD were measured in a range of  $2\theta$  = 10–90° with a step size of 0.0205° and measuring time of 0.2 s · step  $^{-1}$ . Qualitative phase analysis was carried out using Match!—Version2 software (Crystal Impact GbR) with entries from the Crystallography Open Database (COD) [48] and Inorganic Crystal Structure Database (ICSD) [49]. For the Rietveld refinement of selected samples, PXRD was collected on Huber G670 Guinier diffractometers with either Cu- $K_{\alpha 1}$  or Mo- $K_{\alpha 1}$  radiation in the range

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 $4^{\circ} \le 2\theta \le 100^{\circ}$ . Samples were enclosed between kapton<sup>®</sup> foils in apiezon<sup>®</sup> grease. Lattice parameters were determined by Rietveld refinement using the software FullProf [50].

Simultaneous thermal analysis (STA) of plasma-synthesized samples was performed using a STA 449 F3 Jupiter® (NETZSCH), with a combination of thermogravimetric analysis (TG) and differential scanning calorimetry (DSC). STA experiments were carried out under nitrogen or synthetic air up to 1573 K and forming gas (95%  $N_2/5\%~H_2)$  up to 1273 K. The heating rate was generally  $10~\rm K\cdot min^{-1}$ . Typically,  $10~\rm mg$  sample were measured in corundum crucibles.

EPR spectra were recorded with a MS 100 X-Band-EPR-Spectrometer by Magnettech. The spectra were acquired at room temperature with  $B_0=340.0$  mT,  $B_{0sweep}=49.9$  mT, sweep time  $t_{sweep}=500$  s, 4096 steps, modulation amplitude MA = 0.1 mT, a microwave attenuation MWA = 10 dB and a microwave power MWP = 10 mW. The gain (GA) was adjusted for each sample. Samples were measured in 50  $\mu L$  Duran  $^{\circledR}$  glass micro pipettes by Hirschmann Laborgeräte GmbH, and were closed with wax. A normalized intensity  $I_N$  was derived for all spectra, as described in the Supplementary Information, to compare spectra of different samples.

The  $^2$ H solid-state NMR spectrum was recorded on a Bruker Avance 750 spectrometer (magnetic field 17.6 T) at a frequency of 114.94 MHz. In the one-pulse experiment, a pulse length of 2  $\mu$ s and a recycle delay of 500 s were used. The MAS spinning frequency was 2240 Hz.

Diffuse reflectance UV-Vis (DRUVVis) spectroscopy was performed using a PerkinElmer Lambda 950 spectrometer with a 150 mm Ulbricht-sphere by Labsphere. A Spectralon<sup>®</sup> white standard by Labsphere was used as a reference. The spectra were recorded in a range from 200 to 2500 nm, with 250 nm  $\cdot$  min<sup>-1</sup>, an integration time of 0.2 s and data interval of 1 nm at room temperature. Details regarding the analysis and derivation of the electron concentration  $N_e$  from DRUVVis spectra are described in the ESI.

Transmission electron microscopy (TEM) measurements were done with a FEI Osiris TEM. A 200 kV acceleration voltage was applied. The samples were prepared by dispersing the sample with EtOH between two glass object slides. A graphite-covered Cu net was used as a sample holder and was dipped into the dispersion.

X-ray fluorescence (XRF) analysis was carried out with a Bruker Tornado EDXRF with a rhodium X-ray tube. The determination of the sample composition was done by semi-quantitative phase analysis of the obtained spectra using the software QUANTAX Version 1.3.

#### 3.3. Reactivity Studies

#### 3.3.1. Catalytic Experiments

Catalytic experiments in ammonia synthesis were carried out for two different plasma-synthesized Ru/C12A7e $^-$  samples. For this purpose, 5 g (350 to 500  $\mu$ m sieve fraction, ~5 mL catalyst bed volume) of 1.2 wt.% Ru/C12A7e $^-$  based on samples (b) C12A7e $^-$  (5Al) and (c) C12A7e $^-$  (20Al) were used. The tests were performed in a fixed-bed reactor with an inner diameter of 5 mm. A total flow of 4.0126 mol  $\cdot$  h $^{-1}$  of a 3:1 mixture of H<sub>2</sub>:N<sub>2</sub> was applied in the catalytic tests. The performance of the materials was tested at different temperatures and under different pressures as listed in Table 2.

# 3.3.2. Reactivity of Electrides towards Hydrogen

The reactivity of the plasma-synthesized sample (d) C12A7e $^-$  (3C) was initially tested in an in-house constructed tube furnace system. A total of 0.5 g of the sample (d) C12A7e $^-$  (3C) was placed in a quartz glass reactor (diameter = 2 cm) with a porous silica frit. The sample and reactor were flushed for 15 min with a forming gas mixture (95%N $_2$ /5%H $_2$ , 0.1 MPa, GHSV = 5000 h $^{-1}$ ). In the following, the sample was heated with 5 K · min $^{-1}$  to the desired temperature ranging from 373 to 723 K, as summarized in Figure 4, and kept for 1 h before cooling to room temperature. After each of these steps, the sample inside the quatz tube was photographically documented. Before continuing the experiment, the

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sample was flushed again for 15 min with the forming-gas stream. In comparison to the forming-gas atmosphere, 0.5 g of the sample (d)  $C12A7e^-$  (3C) was heated under  $N_2$  to 723 K with 5 K · min<sup>-1</sup> for 1 h. Afterwards the samples were ground and analyzed by PXRD, DRUVVis and EPR spectroscopy.

Hydrogenation experiments of the vacuum sintering-based samples were carried out in a differential scanning calorimeter (DSC) Q1000 from TA Instruments (New Castle, DE, USA) equipped with a gas-pressure cell. A powdered sample of 8.9 mg well-ground dark-green vacuum sintered mayenite electride was loaded into an aluminum pan. The experiments were performed under isochoric conditions with a heating rate of 10 K  $\cdot$  min<sup>-1</sup> under 5.0 MPa hydrogen (99.999% Air Liquide) at 298 K, which increased to 6.7 MPa at the final temperature of 700 K. After the experiment, the sample (Table 1, (j) C12A7:H) was colorless.

Green vacuum-sintered mayenite electride from the synthesis pathway (II) was ground in an agate mortar and reacted with 6.0 MPa deuterium gas (99.8%, isotopic purity, Air Liquide) pressure at 773 K for 48 h in an autoclave made of Inconel alloy (Böhler L718V). The reaction yielded a colorless powder (Table 1, (k) C12A7:D).

# 3.3.3. Hydrothermal Reactivity of C12A7 and C12A7e<sup>-</sup>

For hydrothermal reactivity studies of the C12A7 material (a) based on plasma synthesis under Ar atmosphere, 0.4 g each of (a) were suspended in 4 mL deionized  $H_2O$  and stirred in a 10 mL glass vial with a magnetic stirrer bar for 1, 2, 5, 20 and 28 h at ambient conditions, respectively.  $H_2O$  was decanted and the sample was dried for 30 min at 353 K in a compartment dryer. The dried samples were ground in an agate mortar and analyzed by PXRD. Similar 0.4 g of the plasma-synthesized sample (d)  $C12A7e^-$  (3C) sample was suspended and stirred in  $H_2O$  for 16 h. To exclude a potential influence of air on the hydrothermal stability, 0.5 g of sample (d)  $C12A7e^-$  (3C) was suspended in 15 mL dry THF in a 50 mL Schlenk flask under Ar atmosphere at room temperature. The suspension was stirred for 5 min before deionized  $H_2O$  was added in 0.5 mL steps every 5 min until a total volume of 5 mL  $H_2O$  was added. The suspension was stirred for 72 h before THF and  $H_2O$  were removed under reduced pressure. The resultant solid was dried carefully using a heat gun. The obtained powder was ground and analyzed by PXRD.

#### 4. Conclusions

Plasma-synthesized C12A7e<sup>-</sup> were successfully applied as support materials for ammonia synthesis over Ru/C12A7e<sup>-</sup> catalysts. The electride properties of C12A7e<sup>-</sup> were preserved after Ru deposition. At pressures of 0.1 MPa, the Ru/C12A7e<sup>-</sup> catalysts showed comparable performance to the literature-reported activity data. However, we found an immediate deactivation at higher absolute pressures (>1.0 MPa). By reactivity studies towards H<sub>2</sub>/D<sub>2</sub> we could elaborate the reason for this deactivation. The irreversible formation of C12A7:H, accompanied by loss of the electride properties, was identified as the reason for the deactivation of the catalysts at higher pressures. The C12A7:D phase could be directly obtained by high-pressure autoclave synthesis from C12A7e<sup>-</sup> with deuterium gas. Complementary hydrothermal reactivity experiments revealed the general stability issues of the C12A7 structure and C12A7e<sup>-</sup> towards H<sub>2</sub>O by the formation of different aluminum calcium hydroxide phases. From our results, we conclude that the application potential of mayenite electrides under industrially relevant conditions is limited due to the sensitivity to water and hydrogen at elevated pressures; however, we believe that it is important to explore alternative catalyst materials with electride-like properties under industrially relevant conditions, going beyond model laboratory conditions. Model conditions, far from being industrially relevant, are suitable for fundamental studies and understanding of the catalyst, which, indeed, can lead to remarkable findings about the catalytic properties of the Ru/C12A7e<sup>-</sup> catalyst. However, an application in the established ammonia process is impeded by the observed stability limitations. Therefore, the future challenge is to better understand the nature of the promoting mechanism of electride materials and to identify

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alternative material classes with similar promoting properties to the C12A7e<sup>-</sup> electride support, but with increased stability towards the found deactivation mechanisms, i.e., irreversible hydride transformation of the bulk phase at higher hydrogen pressures and improved hydrothermal stability.

#### 5. Patents

- G. Kolios, T. Mattke, J. M. Mormul, A. N. Parvulescu, F. Rosowski, S. Schäfer, S. A. Schunk, WO002018189216A1
- G. Kolios, T. Mattke, J. M. Mormul, A. N. Parvulescu, F. Rosowski, S. Schäfer, S. A. Schunk, WO002018189218A1

**Supplementary Materials:** The following are available online at https://www.mdpi.com/2073-4 344/11/3/334/s1: Figure S1. Bright-field TEM measurement of the sample Ru/C12A7e<sup>-</sup> (20Al). Figure S2. PXRD after Ru deposition on plasma synthesized C12A7e<sup>-</sup> (3C) (red) and C12A7 (blue) samples. Figure S2. Rietveld refinement of the crystal structure of mayenite electride (vacuum sintering-based C12A7e<sup>-</sup> (e) sample. Figure S3. Rietveld refinement of the crystal structure of the deuteride of mayenite electride (C12A7:D (k) sample).

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