

# Model Adaptation and Validation for Estimating Methane and Ammonia Emissions from Fattening Pig Houses: Effect of Manure Management System

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## 1. Ammonia emission

The different variables and constant values of ammonia model (Eq. 2 of the main manuscript) are calculated as follows (Aarnink and Elzing, 1998) [33]:

$$k_{NH3} = 50.1 \cdot (v_{surface})^{0.8} \cdot (T_{surface})^{-1.4} \quad \text{Eq. S1}$$

where,

$k_{NH3}$  is the mass transfer coefficient for ammonia (m/s)

$v_{surface}$  is the air speed over the emissive surface (m/s)

$T_{surface}$  is the temperature of the emissive surface (K).

$$f = \frac{10^{pH_{surface}}}{10^{pH_{surface}} + 5 \cdot 10^{(0.0897 + (\frac{2729}{T_{surface}}))}} \quad \text{Eq. S2}$$

where,

$f$  is the fraction of unionized ammonia in the solution (-)

$pH_{surface}$  is the pH of the emissive liquid at the surface (-)

$T_{surface}$  is the temperature of the emissive surface (K).

$$H = 1431 \cdot 1.053^{(293 - T_{surface})} \quad \text{Eq. S3}$$

where,

$H$  is Henry's constant

$T_{surface}$  is the temperature of the emissive surface (K).

The  $NH_4$ -N content of the bulk slurry was calculated by assuming complete conversion of the urea in urine to  $NH_4$ -N. Knowing the total amount of excreted urea-N, the  $NH_4$ -N concentration of the bulk slurry can be calculated.

The potential excretion of  $NH_4$ -N (total of urea-N and  $NH_4$ -N) in fresh urine is calculated from the total N excretion in the fresh urine (other N compounds make up the rest of the N):

$$U_{NH_4N-pot} = -2,7 \cdot 10^{-4} + 0,87 \cdot U_{Ntot} \quad \text{Eq. S4}$$

where,

$U_{NH_4N-pot}$  is the potential  $NH_4$ -N excreted per day (total of  $NH_4$ -N and urea-N in urine) (kg/d),

$U_{Ntot}$  is the total amount of N excreted in urine (kg/d).

Measurements have revealed that in fattening pigs, approximately 11.0% (standard error (se): 0.3%) of the faeces-N exists in the form of  $NH_4$ -N. It is anticipated that this  $NH_4$ -N will not, or will only minimally, emit from the floor. Nevertheless, it remains crucial for determining the  $NH_4$ -N content of the slurry (mixed urine and faeces) in the manure pit [34].

The air velocity over the manure surface in the manure pit was calculated using the following relationship with the ventilation flow rate per square meter ( $m^2$ ) of barn area, derived from the best fit of the measured data.

$$v_{surface\_pit} = 0,091 + 14,2 \cdot vent_{m^2} \quad \text{Eq. S5}$$

where,

$v_{surface\_pit}$  is the air velocity over the evaporating surface (m/s),

$vent_{m^2}$  is the ventilation flow per  $m^2$  of barn area ( $m^3/s$  per  $m^2$  of barn area).

Measurements have shown no significant correlation between the air velocity measured above the urine-soiled floor surfaces and the ventilation flow rate per  $m^2$  of the barn area. Therefore, the air velocity is assumed to remain constant above the urine soiled area (0.146 m/s). Furthermore, the air velocity and the temperature of the emitting surface is assumed to be equal to that of the manure in the pit. The following relationship was found between the temperature of the emitting surface in the manure pit and the temperature of the outgoing air from the pig house:

$$T_{surface\_manure} = 1,85 + 0,735 \cdot T_{exhaust} \quad \text{Eq. S6}$$

where,

$T_{surface\_manure}$  is the temperature of the emitting manure surface in the basement (°C),

$T_{exhaust}$  is the temperature of the outgoing stable air (°C).

This regression line accounts for 42% of the variation in the measured surface temperature of the manure pit (Aarnink *et al.*, 2018)[34]. The surface temperature of the urine samples was comparable to the outgoing air temperature (regression coefficient equal to 1.01; se 0.02%) and was therefore set equal to this temperature in the model.

The water evaporation from the soiled floor surfaces and the manure pit has been found to be related to the vapor pressure difference in the interface of the wet surface and the air and is proportional to the size of it evaporating surface. The evaporation from the wet floor surfaces and the manure pit was estimated as follows:

$$evap_{floor} = k_{evap_{floor}} \cdot (p_{floor} - p_{air}) \cdot A_{wet-floor} \quad \text{Eq. S7}$$

$$evap_{pit} = k_{evap_{pit}} \cdot (p_{pit} - p_{air}) \cdot A_{wet-pit} \quad \text{Eq. S8}$$

where,

$evap_{floor} / evap_{pit}$  is the water evaporation from the floor or the manure pit (kg/d),

$k_{evap_{floor}} / k_{evap_{pit}}$  is the evaporation coefficient of the floor or the manure pit (kg/(m<sup>2</sup>.kPa.d)),

$p_{floor} / p_{pit}$  is vapor pressure of the wet floor surface or the pit surface (kPa),

$p_{air}$  is the vapor pressure of the air (kPa).

It is assumed here that the relative humidity of the evaporating surface of the floor and manure cellar is 100%. The vapor pressures have been calculated using Albright (1990) formulas [48]. According to Beeking *et al.* (1994) [49] is the evaporation coefficient proportional to the square root of the air velocity over the evaporating surface:

$$k_{evap} = b_{k_{evap}} \cdot \sqrt{v_{surface}} \quad \text{Eq. S9}$$

where,

$k_{evap}$  is the evaporation coefficient for the floor or manure pit (kg/(m<sup>2</sup>.kPa.d))

$b_{kevap}$  is a regression coefficient,

$v_{surface}$  is the air speed over the evaporating surface (m/s).

The regression coefficient  $b$  is based on the least squares method on the measured evaporation data. This analysis led to estimation of  $b_{kevap}$  as 7.69 (Aarnink *et al.*, 2018)[34].

## 2. Methane emission from manure pit

In this model, volatile solid was considered as a main determining factor for CH<sub>4</sub> emissions from animal manure storages divided into degradable (VS<sub>d</sub>) and non-degradable VS (VS<sub>nd</sub>) (Sommer *et al.*, 2004). In Eq. 3, the model assumes that the degradation of VS<sub>nd</sub> is 100-fold slower than the degradation of VS<sub>d</sub>. Furthermore, the VS degradability in the manure pit is corrected for the lignin content of the diet (assuming that lignin is non-degradable) and subsequently the fractions of degradable VS were calculated. The lignin content (%) as a percent of total solids is identified with Acid Detergent Lignin (ADL) (assuming that the fraction of lignin-bound nitrogen is insignificant) (Soest, 1963; Triolo *et al.*, 2011) [50,51]. The ADL content of feed ingredients were derived from CVB tables (2021) and calculated for the studied diets. The content of volatile solids of the faeces and urine are predicted by the model. The organic matter excretion in faeces was estimated based on the indigestible organic matter of the feed intake (Rigolot *et al.*, 2010) [52]. Thus the total VS content was calculated using Eq. S10 – S13.

$$F_{vs} = FI \times Feed_{OM} \times (1 - d_{COM}) \quad \text{Eq. S10}$$

$$U_{vs} = \frac{60}{28} \cdot U_{Ntot} \quad \text{Eq. S11}$$

$$VS_{total} = F_{vs} + U_{vs} \quad \text{Eq. S12}$$

$$VS = \frac{VS_{total}}{\text{total manure excretion}} \quad \text{Eq. S13}$$

where,

$F_{vs}$  is the organic matter excretion via faeces (kg/d),

$FI$  is the feed intake (kg/d),

$Feed_{OM}$  is the organic matter of the feed, input in the model (kg/kg),

$d_{COM}$  is the digestibility coefficient of the organic matter of the diet, input in the model (kg/kg),

$U_{vs}$  is the organic matter excretion via urine (kg/d),

$VS_{total}$  is the total organic matter excretion (kg/d),

$VS$  is the volatile solids content of the manure (kg/kg).

#### 4.1 Temperature correction

The  $CH_4$  production rate was measured following a measurement protocol (Petersen et al., 2016) [32] under an average temperature of all samples while the *in-situ* temperature of manure (measured during the measurement campaign on the site) might differ (according to the protocol of this study the difference should not exceed  $\pm 3$  °C); Therefore the measured rates were corrected to the exact temperature of the manure recorded at the time of sampling. The corrected methane production rate for temperature can be calculated by Eq. S14.

$$k_2 = k_1 \exp\left(\frac{-E_a}{R}\left(\frac{1}{T_2} - \frac{1}{T_1}\right)\right) \quad \text{Eq. S14}$$

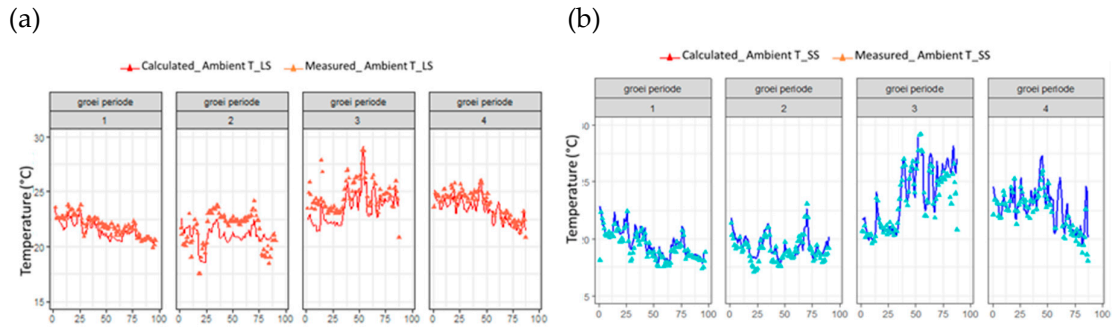
where,

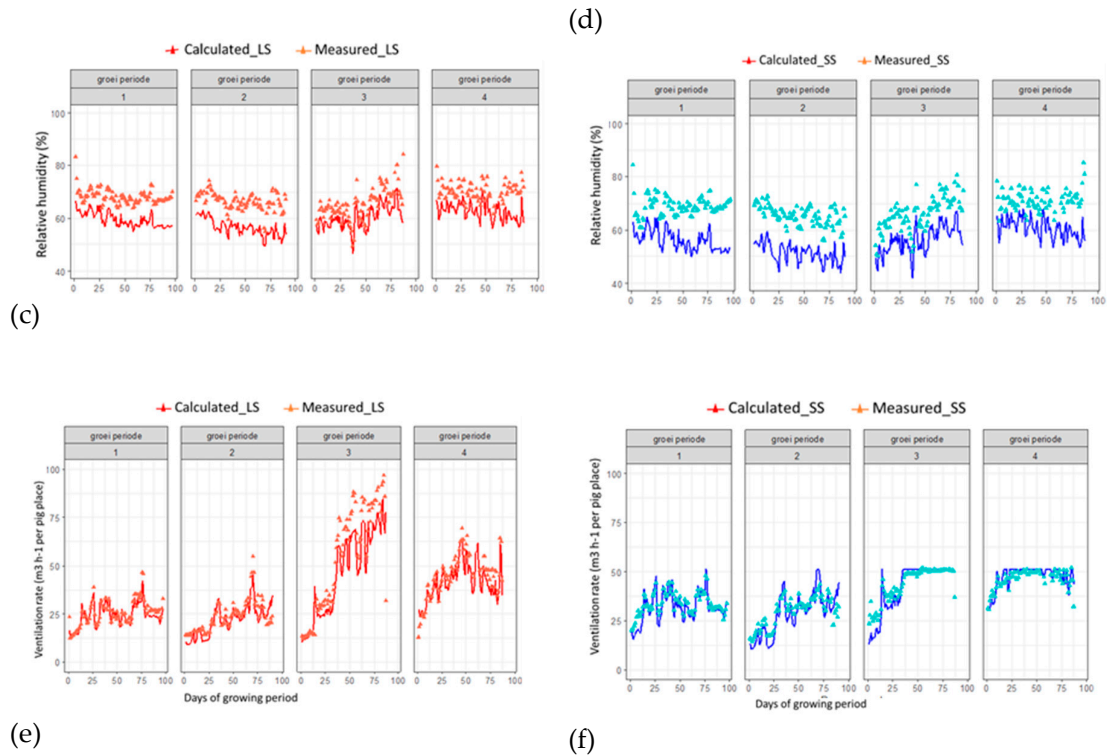
$k_2$  is the rate at in-situ temperature ( $g\ CH_4\ kg^{-1}\ VS\ d^{-1}$ ),

$k_1$  is the rate measured ( $g\ CH_4\ kg^{-1}\ VS\ d^{-1}$ ),

$T_1$  is the incubation temperature (K),

$T_2$  is the measured in-situ temperature (K) of the manure sample.





**Figure S1** Calculated (line) and continuous-measured (point) values of indoor temperature (°C), relative humidity (%) and ventilation rate (m³ h⁻¹ per pig place). The red lines and points represent the reference department and those in blue represent the trial department. Each segment indicate one growing period (GP); 8 October 2020–12 January 2021; GP2: 21 January 2021 – 20 April 2021; GP3: 27 April 2021 – 21 July 2021; GP4: 27 July 2021 – 21 October 2021.

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