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A GHG Metric Methodology to Assess Onsite Buildings Non-Potable Water System for Outdoor Landscape Use

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Abstract: This paper documents a water:energy greenhouse gas (GHG) metric methodology for a decentralized non-potable water system that was developed as part of a Professional Doctorate in Engineering (DEng) research project by the first author. The project identified the need to investigate the challenges in changing the use of potable water to recycled water for landscape irrigation (LI) and for water features (WFs) at a medical facility case study (MFCS) in Abu Dhabi (AD) (the capital city of the United Arab Emirates (UAE)). The drivers for the research project were based on the need for AD to decrease desalinated potable water as well as reduce the environmental impact and operational costs associated with the processing and use of desalinated water. Thus, the aim of the research discussed and presented in this paper was to measure the impact of using recycled and onsite non-potable water sources at the MFCS to alleviate the use of desalinated potable water and reduce associated energy consumption, operational costs, and GHG emissions (latterly in terms of carbon dioxide equivalent (CO_2e), for LI and WFs. The analysis of three case scenarios at the MFCS compared different approaches to alleviate energy use, costs, and GHG impacts for the use of recycled water in LI and WFs against a baseline. The findings led to a proposed sustainable water conservation and reuse (SWC) strategy, which helped save 50% desalinated potable water for LI use by soil improvement, building water system audits, and alternate non-potable water reuse. The recommendations for this paper are to develop a SWC strategy forming the basis for a water protocol by the competent authority for regional medical facilities including an assessment methodology for building decentralized non-potable water systems to measure their energy, GHG emissions and financial impact.

Keywords: water recycling; landscape irrigation; climates change; greenhouse gas metric; maintenance

1. Introduction

1.1. Research Background

The climate of the United Arab Emirates (UAE) is classified as Arid (B), Desert (W), and Hot Arid (h) (Bwh) by Köppen and Geiger [1], which makes it a hot desert type climate. The mean yearly temperature, relative humidity (RH), and rainfall for Abu Dhabi (AD) is 27.6 Celsius ($^{\circ}\text{C}$), 63%, and 62.1 mm (mm), respectively [2]. Still in October 2019, 13 Arab countries were among the world's 19 most water-scarce countries [3,4]. Per capita, water availability in eight Middle East countries is below 200 m^3 per year including the UAE [5] (see Figure 1). Therefore, with such an arid climate, there is a

significant need to investigate and implement all opportunities for recycling and reusing water in the built environment and their associated landscapes in AD.



Figure 1. Declining per capita water availability: A growing threat in Middle East North Africa (MENA) [5] in [6].

The medical facility case study (MFCS) was a 364-bedroom hospital that opened in 2015 with 50% of its footprint dedicated to landscaping (33,354 m²), and the design aspirations were to target 100% non-clinical/non-potable water use for landscape irrigation (LI) and use in water features (WFs) from treated air conditioning (A/C) condensate water. Peak condensate formation occurs during the hottest and most humid months of each year (April to November) with the minimum condensate formation rates occurring in the winter and spring months between December and April [7]. This is because the MFCS does not need to be cooled in winter and spring as much as in summer.

Hence, therein lies a problem since for five months per year (December–April) there is a predicted non-potable water deficit and desalinated potable water is required for use in LI and WFs, which is expensive and has significant associated carbon emissions from the desalination process of seawater. Thus, the research set out to investigate any additional sources of water use/harvesting that could be recycled for reuse in LI and WFs at the MFCS to mitigate the use of potable water use during the five months of the year when no treated condensate water is available [6].

In order to investigate alternate sources of water for recycling and reuse, the research project used a mixed methods approach after Creswell and Creswell [8] to collect data on water sources available at the MFCS. The water and energy data were used to develop a sustainable water conservation and reuse (SWC) strategy (that includes the reduction of water consumption for LI by soil improvement, building water system audits, and the use of additional non-potable water sources), forming the basis of a water conservation protocol, thus enabling the MFCS to meet the five-month potable water shortfall. The results also include a greenhouse gas (GHG) metric in terms of kilograms of carbon dioxide equivalent (kgCO_{2e}) per cubic meter (m³) to assess the carbon savings by using recycled water for LI and WFs use.

1.2. Healthcare Context for Water Conservation

To the authors' knowledge, there has been no published literature since April 2008 on water research for use in LI or WFs, or energy research related to the healthcare sector [6]. As such, the gap in knowledge that this paper is addressing are non-potable water standards for irrigating landscapes and use in WFs for the healthcare estates in AD, UAE (ibid.). Furthermore, the research discussed is relevant to healthcare estates in climates similar to AD. In the United States of America (USA) in 2002, water consumption ranged from 260 m³ to 1128 m³ per year, per patient bed for hospitals in the size range of 133 to 510 beds [9]. That is, 0.71 m³ and 2.21 m³ per day, per bed respectively. However, a hospital's water use varies widely depending on type, size, geographical location, and water use equipment and practices. The MFCS records indicated an amount of 2.97 m³ of water consumption per patient bed per day (see Figure 2) in 2016 (395,916 m³ ÷ 364 beds ÷ 366 days), which means that the

water use for the LI alone in 2016 represented a substantial quantity (36%) of the total water demand. Thus, a significant opportunity exists to conserve water for outdoor use, whilst at the same time reusing non-potable water for LI and WFs to achieve zero-potable water outdoor use [6].

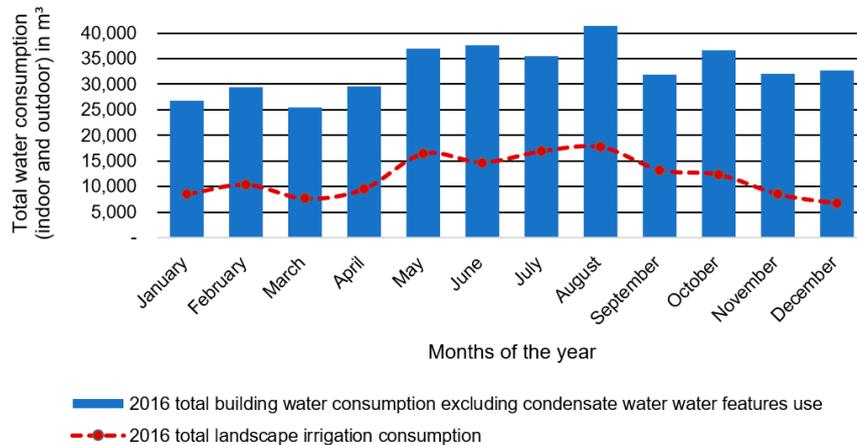


Figure 2. Medical facility case study (MFCS) total building water use against LI consumption based on 2016 Abu Dhabi Distribution Company (ADDC) water bills [6,10].

1.3. The Context of the Water Energy Nexus in Abu Dhabi

AD has embarked on a massive United States (US) five-billion-dollar program, based on the aquifer storage and recovery approach [11]. This program is to build capacity so that local aquifers can be used as strategic reserves for desalinated water [12]. The peak demand forecast for water will more than double by 2030 [13]. The Emirate of AD's annual water consumption is estimated to be 2.49 billion m³ and is expected to reach 5.86 billion m³ by 2020 [14].

In the UAE, groundwater has been extracted at over 13 times the annual recharge rate [15] in [16]. However, water use varies between the emirates. In AD, 72% of the groundwater is mainly used for agriculture irrigation, followed by desalination (24%) in residential and commercial buildings as domestic water. Plus, four percent is used for treated sewage effluent (TSE), residential district cooling, public park LI and in WFs such as fountains, but not for crop cultivation [16]. In 2012, desalinated water demand in AD exceeded local production, where 201.3 million m³ had to be imported from Fujairah, a northeastern emirate (ibid.).

Different factors have made the UAE dependent on desalination water. First, the increased water demand of a fast-growing population; second, the low (less than 100 mm/year) average precipitation; third, a very high evaporation rate (two to three m³ per year) (ibid); and fourth, the limited recharge of the groundwater [4,17]. For this reason, AD has no choice but to supply domestic water from seawater desalination [17] using techniques such as multi effect distillers (MED), reverse osmosis (RO), and multistage flash (MSF) [18,19]. The main technology used in the UAE is thermal desalination with MSF (57%) because it is more energy efficient and can produce higher quality water (ibid.). MED are used at 6% for desalinating water and RO at 37% [19,20]. However, as shown in Table 1, the technique of desalination is still highly energy intensive: RO and MSF technologies use between four-kilowatt hour per cubic meter (kWh/m³) to 7.5 kWh/m³ average and up to 15.40 kWh/m³, respectively [20]. In addition, MSF and RO technologies also have a very high cost of 1.10–1.25 United States dollars (USD) per m³ and 0.68–0.82 USD/m³, respectively, in comparison to 0.05 USD/m³ for fresh water sources [21].

The water supplied to AD Island (the location of the MFCS) is produced at the Arabian Power Company (AMPC), Taweelah Asia Power Company (TAPCO), Gulf Total Tractebel Power Company (GTTPC), and Emirates CMS Power Company (ECPC), as detailed in Table 2 [18]. Desalination plants, which mainly use MSF thermal desalination technology (74%) consume energy at a rate of 15.40 kWh/m³ [20], bringing the cost of water production between 1.10 to 1.25 USD/m³ (ibid).

This provides evidence that the value of water production is not tied to the subsidized (50% discount) commercial and residential AD water tariff, which is AED 4.11/m³ [10] after discount, which is equivalent to USD 1.12/m³ [22].

Table 1. Desalination techniques against financial and environmental impacts [20].

Description	MSF	MED	RO
Water cost production (USD/m ³)	1.10–1.25	0.75–0.85	0.68–0.82
Energy use (kWh/m ³)	15.40	7.5	4–7
Volume of saline feed water per m ³ of fresh water	4	3	2–2.5

Table 2. Desalination plants serving AD Island [18].

Abu Dhabi Water Supply	Desalination Technique Used	Water Production Share by Company
AMPC	MSF	2%
TAPCO	MSF	18%
GTTPC	MSF + MDF	10%
ECPC	MSF	6%

Desalination plants have been optimized since 1990–2000, although the process efficiency is still under investigation through pilot programs [11] such as an adsorption desalination system producing pure water with no need for fossil fuel use (ibid.). Thus, in 2017, the process of desalination was still highly energy intensive [13,14,21], hence impacting on the natural environment, and contributing ultimately to climate change. As highlighted in Table 1, it takes 4 m³ of saline feed water for the MSF technology to generate 1 m³ of distillate water [20]. Energy consumption and potential effects on the marine environment of brine disposal are the two largest aspects of environmental impact [14,23–26].

Approximately 60% of the AD wastewater is planned to be returned to the sewer by 2030 to be recycled for reuse in applications such as irrigation [27] in [28]. This strategy forms part of the AD government’s aims to not permit potable water to be utilized for irrigation purposes, and so alleviate stress on the existing water infrastructure [29] in [28]. As such, it will be mandatory to use treated sewage effluent (TSE) for irrigation (ibid.). To date (2019), to the authors’ knowledge, there is no TSE infrastructure near the MFCS location, and the timing for this to happen is presently unknown to the community [30] in [28]. The International Energy Agency (IEA) [31] reported that in 2014, almost 10% of the Middle East’s (including AD) electricity consumption was used to extract, distribute, and treat water and wastewater including the use of large quantities of oil equivalent of thermal energy for irrigation pumps and gas in desalination plants (see Figure 3).

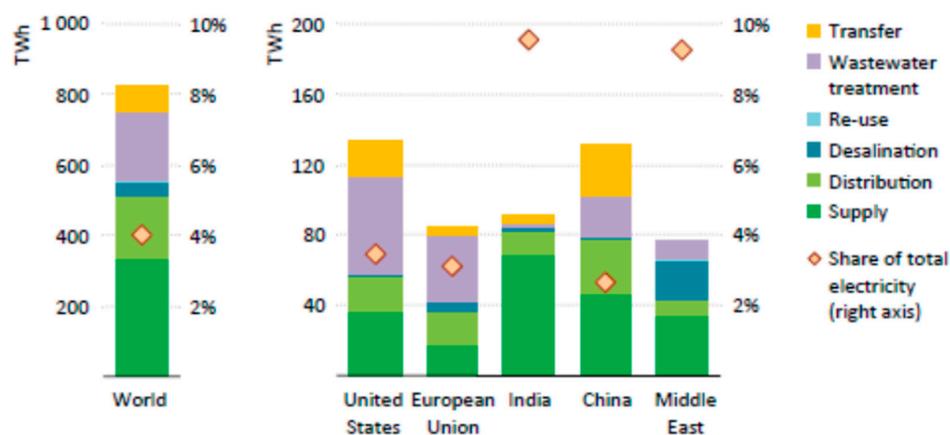


Figure 3. Electricity consumption in the water sector by process and region in 2014 [31]. Supply includes water extraction from groundwater and surface water as well as water treatment. Transfer refers to large-scale inter-basin transfer projects.

Water systems can save energy by reducing the amount of water that must be withdrawn, treated, and distributed [32], especially in locations like AD, where the technique of desalination is highly energy intensive [20]. Figure 4 illustrates the energy consumption to treat and move water from the source to the end-user [29,31].

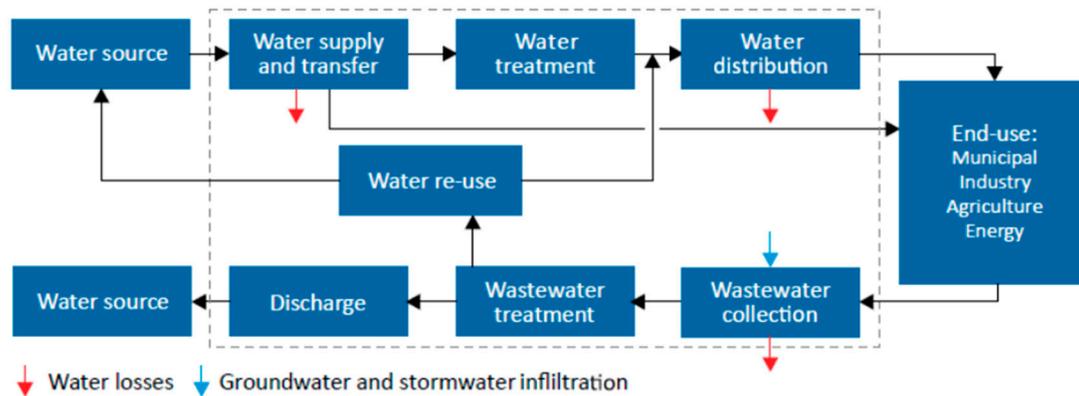


Figure 4. Energy need in each step of the water process [31].

Irrigation is the primary water consumption worldwide [33]. In arid regions where the mean annual precipitation (P) is substantially less than the characteristic potential evapotranspiration (ET_0), the appropriate selection of plants and efficient irrigation systems can conserve a great amount of urban irrigation water [34]. In addition, wasting water in sectors such as landscaping in arid regions is further aggravating water scarcity and emphasizing the need to develop ways to improve irrigation efficiency (ibid). This improvement cannot solely depend on improving the efficiency of water pumps without changing the price of electricity or irrigation practices to avoid a water consumption increase and further depletion of aquifers [31].

1.4. Greenhouse Gas (GHG) Emissions and Decarbonization

Electricity consumption associated with water and wastewater operations are a major contributor to GHG emissions [35–39]. Internationally recognized GHGs, regulated under the United Nations (UN) Kyoto Protocol [40], linked to the UN Framework Convention on Climate Change (UNFCCC) [41], are composed of long-lived and short-lived GHGs. Long-lived GHGs are mostly CO_2 and nitrous oxide (N_2O), which can remain in the atmosphere for hundreds of years [42]. Short-lived GHGs are mostly methane (CH_4), hydrofluorocarbons (HFCs), perfluorocarbons (PFCs), sulfur hexafluoride (SF_6), and nitrogen trifluoride (NF_3), and they remain in the atmosphere for much shorter periods, from days to decades [42,43]. Most of the emissions embedded in water are usually from CO_2 , N_2O , and CH_4 [35]. The level of global warming is determined by the cumulative emissions of CO_2 over time and the annual emissions of short-lived GHGs. To stabilize the climate to below 3 degrees Celsius ($^{\circ}C$), as stipulated by the UNFCCC [41], carbon neutrality or decarbonization will be needed by 2100 [43]. The energy intensity (responsible for long-lived gases emissions) of the Middle East and Africa region including the UAE increased by 41% from 1970 to 2010 [44]. The highest key category of GHG emissions in the Emirate of AD comes from the energy industries accounting for 46.8% [45]. Both the key driver and key category are the consumption of fossil fuels [44,45]. The atmospheric concentration of CO_2 keeps increasing as long as emissions are positive, and it decreases if emissions are brought to zero, depending on the cumulative emissions over time. Thus, to stabilize long-lived gas concentrations, both CO_2 and N_2O are required to be brought to zero and short-lived GHGs (CH_4 , HFCs, PFCs, SF_6 , NF_3) are to be kept constant [43].

In 2019, three water challenges prevail in AD. First, the energy intensity of desalination; second, access to TSE; and third, high irrigation demand.

1.5. Gaps Analysis Leading to New Body of Knowledge

In addition, electricity consumption associated with water and wastewater operations are a major contributor to GHG emissions [35–39]. For GHG emissions embedded in water, most are usually from CO₂, methane (CH₄), and nitrous oxide (N₂O) [35]. The energy intensity of non-potable water supply sources (other than desalination water) and decentralized water systems “are unknown and is a knowledge gap that requires further research” [36] as “There is no standardized methodology or framework for the assignment of values to water streams at present” [46]. Additionally, the design of methodologies to account for these GHG emissions have not been transparently available [35]. This knowledge gap is summarized in Table 3.

Table 3. Onsite non-potable water systems for the greenhouse gas (GHG) benchmarking knowledge gap.

Existing Standards Related to Water and Energy Carbon Footprint Management	Scope	Address Both Energy Intensity and Water Reduction for Onsite Non-Potable Water Systems? (Yes or No)
International Standard Organization (ISO), 14046: 2016 Environmental management Water Footprint Principles, requirements and guidelines [47]	Applicable to products, processes and organizations and based on lifecycle assessments (LCA’s) to accurately quantify the water used, in a verifiable and consistent manner.	No. It addresses Water Consumption Reduction only.
ISO 50001:2017 Energy management systems. Requirements with guidance for use [48]	ISO 50001 requires the demonstration of continual improvement through the reduction in utilization of energy.	No. It does address all energy systems of an organization including heating boilers and sanitary facilities.
Water Usage Effectiveness (WUE) [46]	A metric to quantify water required for operating and cooling equipment for cloud computing industries and data centers.	No. It addresses Water Consumption Reduction only for specific industries.
Embedded Resource Accounting (ERA) [49]	It generalizes ecological, water, and carbon footprint methods by accounting for the net direct and indirect impacts of processes on arbitrarily defined resource stocks.	No. It is a generalized footprint methodology, which is used to derive footprints including water footprint [46].
Water Energy Greenhouse Gas Metric (WEG) [35]	This establishes a series of WEG intensity metrics to enable water suppliers and consumers in Southern California to assess the GHG impact of their urban and agricultural water products.	No. The recycled water treatment and distribution and wastewater collection, treatment, and disposal are outside the scope of the WEG Guidance. The operational boundary ends at point-of-delivery, or end-of-pipe.
GHG Protocol Corporate Value Chain (Scope three) Accounting & Reporting Standard [50]	The Scope Three Standard is the method to account for emissions from 15 categories of scope three activities (All other non-scope two indirect anthropogenic GHG emissions that occur in the value chain), both upstream and downstream of their operations. Unlike scope 1 and 2, scope three is not subject to verification by a third party.	No. Onsite non-potable water supply and water recycling GHG emissions are not defined.

1.6. Original and Significant Contribution to New Body of Knowledge

The key original and significant contributions to change in practice from the author’s research undertaken as part of her D.Eng. project are to propose a sustainable water conservation and reuse (SWC) strategy forming the basis for a water protocol, specific to arid climate regions such as AD, and which addresses the following. The development of a calculation methodology using equations from the literature to estimate and compare energy consumption in desalinated water and onsite generated non-clinical non-potable water resources for WFs and LI reuse. This is to measure the financial viability through a benefit cost ratio analysis, and to measure the systems’ GHG emissions impact with the design and development of a water: energy GHG metric with these units, kilograms of CO₂ equivalent per m³ (kgCO_{2e}/m³).

2. Materials and Methods

2.1. A Mixed Method Research

After initial water usage analysis in 2016 and 2017 through the development of a water balance [6,28,51,52], it was found that the MFCS was wasting large quantities of water, leading to a potential water deficit. For example, the LI was consuming (in January 2018) 46% more water than the estimated demand based on the Abu Dhabi Municipality (ADM, Abu Dhabi, UAE) standard [53], and after soil improvement. Additionally, the water consumption of the WFs exceeded Seguela et al.'s [51] calculations of the water demand by 80%. Second, the reverse osmosis reject water (RORW) and the fire sprinkler pump test water were deemed suitable to be used as makeup-water to the existing condensate water for LI and WF use, subject to tertiary treatment [6]. Figure 5 illustrates the project research methodology in relation to the impact calculation of the MFCS.

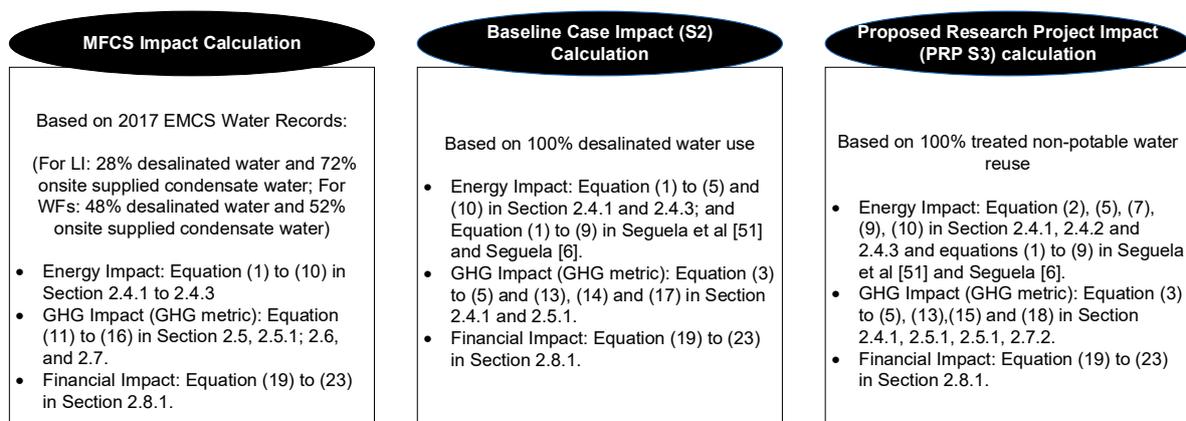


Figure 5. Summary of the energy, environmental and financial impact calculations.

2.2. Medical facility case study (MFCS) Water System Description

Referring to Figure A1 and Table A1 in Appendix A, which links to the MFCS non-potable water system configuration diagram in [51] and [6], four pump sets (P1) divert, store, and convey both the condensate water and the desalinated makeup water to the water storage tanks to serve the site. For each of the eight plant rooms serving the WFs, one pump (as part of the P4 pump set) is used to recirculate the water and one or two pumps (as part of the P4 pump set and depending on the ozone plant room configuration) are used to operate the water treatment system and distribute the water to the WFs. An additional one pump set (P5) and two pump sets (P2) are used to distribute the water to the LI as well as an additional pump (P3) to distribute desalinated makeup water to the WFs. The water system uses a total of 26 pumps to operate a combined 3289 m² (1587 m³ capacity average per month) of decorative WFs and to irrigate 33,257 m² of landscape. The energy calculations of the treated non-potable water system will be based on the 2017 Energy Monitoring and Control System (EMCS) records (WF and LI water consumption). The peak power demand, the daily energy use, and the seasonal energy demand calculation method for the site has been discussed in [51] as Equations (6)–(9), respectively. All physical and operational characteristics of the outdoor water system were updated and are detailed in Table A1 in Appendix A.

The main electrical consumption accounted for in the MFCS energy calculations are the pumps and the water treatment systems' power consumption. More than 85% of the total energy used for water systems is drawn by the energy for pumping water [54] and its associated water treatment system [55]. Real energy use for a given water system can vary widely, according to its source configuration [54], however, the largest energy use is by far pumping (ibid.).

The LI system operates 13 hours (h) per day according to the landscape contractor irrigation schedules (5 a.m.–12 p.m.; 6 p.m.–12 a.m.). The WF system's operating hours are based on the EMCS

pump trends, which showed that pump set (P3) runs for nine minutes (mins) and 75 s (s) every 20 min, which is 10.67 h per day ($8.89 \text{ min} \times 3 \text{ times} (20 \text{ min} \times 3 = 1 \text{ h}) \times 24 \text{ h}/60$ (60 min in one hour)). The water demand for the landscape irrigation and the water features were calculated by using Equations (1)–(4) in [51].

2.3. MFCS Energy and GHG Impact Boundaries

First, to set operational boundaries and inventory the MFCS activities with respect to direct and indirect emissions (Scope 1, Scope 2, and Scope 3, see Figure 6 for emission targets), the General Reporting Protocol (GRP) [42] was used, which follows both the GHG Protocol Corporate standard [50,56], and the International Standard Organization 14064 [57,58]. Figure 6 provides an overview of the relationship between the three scopes and the activities that generate direct and indirect emissions along the value chain of the MFCS [42].

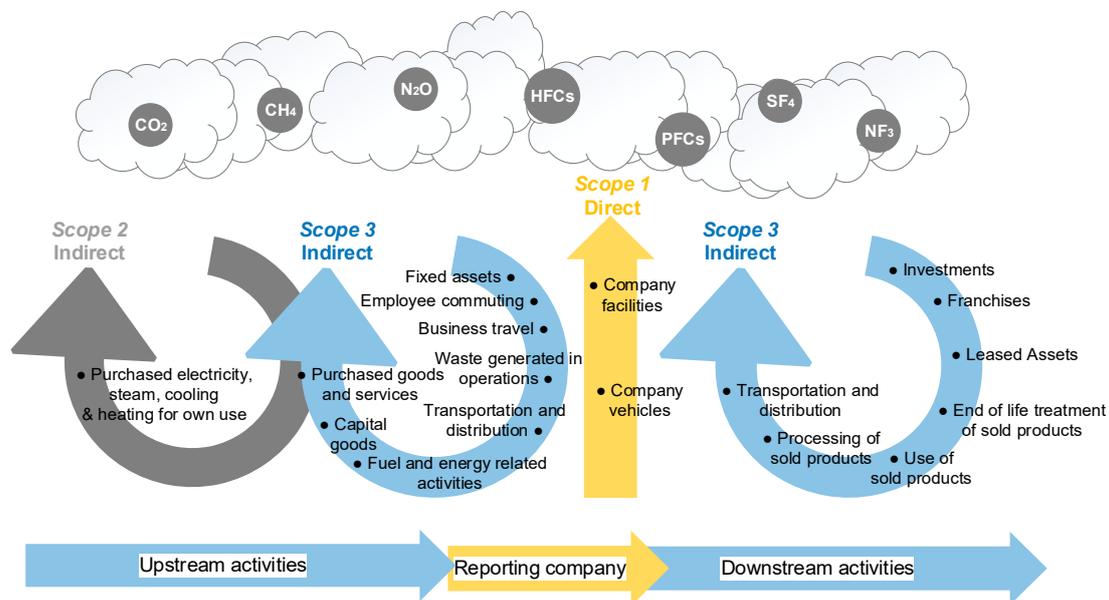


Figure 6. Overview of the GHG protocol scopes and emissions across the value chain [50].

The MFCS indirect emissions expressed in tons of carbon dioxide equivalent (tCO_2e) are accounted in scope two with respect to purchased electricity occurring from upstream activities such as the electrical consumption by onsite pumps and water treatment systems [42,57–59]. Scope 1 is excluded because there are no onsite fossil fuels used for the operation of the MFCS water system. In addition, Scope 3 includes the other non-scope two indirect anthropogenic activities [50]. The GRP [42] does not include the calculation methodologies for Scope 3 emissions, and instead refers to the World Resource Institute (WRI) World Business Council for Sustainable Development (WBCSD) GHG Protocol Corporate standard [50]. However, onsite non-potable water supply and water recycling are not clearly defined in the latter protocol. Thus, considering the above findings, in relation to Section 1.4 including Table 3, a methodology is proposed, which first includes the energy needed by the onsite MFCS non-potable water system to power each step of the water need for outdoor use, adapted from The Climate Registry (TCR) [35]. Second, it includes the end-use of non-potable water and thus the onsite recycled water treatment and distribution needed. Third, the energy use against water consumption is addressed including the consideration of volume reducing factors such as the LI soil enhancement intervention outcome [6] and the WFs' water demand calculation [51].

2.4. MFCS Energy Impact Calculation Method

The energy demand per day (kWh) for the WFs is the results of Equation (5) in [51], the energy demand (kWh) per day for the LI is the result of Equations (6)–(9) (ibid.). The power (kW) and energy (kWh) demand for LI was developed from Equations (6)–(9) as adapted from Kay and Hatcho [60] in Seguela et al. [51], which were specifically developed for crop irrigation. In addition, the power (kW) and energy (kWh) demand for the WFs were developed from the swimming pool calculation methods [61,62] as per Equation (5) in Seguela et al. [51], with the addition of the pumps’ frequency of use. It is estimated that the transfer pumps are used 30% of the time, and the backwash pumps 10% of the time.

These calculation methods are like the basic theoretical pump power and pump energy intensity calculation methods of Conway and Rothausen [63], Cheng [64], and Chiu et al. [65]. However, these, like the MFCS calculations, do not include factors for pump power standby-mode and pump power start-up [66,67] due to the lack of information on the number of start-up operations per pump and the power rate for standby mode (see Table 4 for the different calculation methods analyzed by the author). According to Vieira et al. [67] and Ward et al. [68], 60% to 69% more energy is used when considering pump standby-mode and pump power start-up in the equation. However, these authors did not consider the shutdown mode for system maintenance, which may also influence the results. Thus, according to the Table 4 literature review [51], the proposed MFCS calculation is a simple method.

Table 4. MFCS energy in water calculation methods.

Literature Review	Method for Calculating Pump Energy Intensity	Water End-Use
<ul style="list-style-type: none"> ■ [67] ■ [66] 	<ul style="list-style-type: none"> ■ Pump Input Power (kW) ■ Pump Flow rate in cubic meter per hour (m³/h) ■ Pump Start-up (kWh/start-up) ■ Number of start-up operations (start-up/day) ■ Power rate of standby mode (kW) ■ Standby mode (hours/day) ■ Rainwater consumption (m³) 	Rainwater reuse for toilet flushing and laundry supply in single-story detached house
<ul style="list-style-type: none"> ■ [68] 	<ul style="list-style-type: none"> ■ Volume pumped during constant flow operation (m³) ■ Volume pumped during start-up (m³) ■ Start-up energy factor (%) ■ Motor pump power rating (kW) for efficiency calculation ■ Motor input power (kW) for efficiency calculation ■ Pump capacity (m³/h) 	Rainwater reuse for toilet flushing in office building
<ul style="list-style-type: none"> ■ [65] ■ [64] 	<ul style="list-style-type: none"> ■ Liquid density in kilogram per cubic meter (kg/m³) ■ Gravitation acceleration in meter per second squared (m/s²) ■ Total head (m) ■ Flow Rate in cubic meter per second (m³/s) ■ Motor efficiency (%) ■ Pump efficiency (%) 	Rainwater reuse for single family one-story house
<p>Calculation adapted from Forrest and Williams [61] and Gallion et al. [62] Equations (1)–(5) in Seguela et al. [51]</p>	<ul style="list-style-type: none"> ■ Electricity input (kWh) (Equation (5)): <ul style="list-style-type: none"> - Pump power (kW) - Use frequency (%) - Pumping shut down during maintenance in hours per day and days per year ■ Total water consumption (m³) which considers: <ul style="list-style-type: none"> - WFs water precipitation, evaporation, backflush and refill (Equations (1)–(4)) 	Water features (WFs)

Table 4. Cont.

Literature Review	Method for Calculating Pump Energy Intensity	Water End-Use
Kay and Hatcho [60] for Equations (6)–(9) in Seguela et al. [51]; Conway and Rothausen [63] for Equation (7) (ibid.)	<ul style="list-style-type: none"> ■ Peak power demand (kW) (Equation (6)) - Acceleration of gravity (9.81 m/s²) - Pump discharge (m³/s) - Pressure/head (m) - Pumping plant efficiency (%) ■ Overall seasonal energy demand (kWh) (Equation (7)) - Volume of water (m³) - Pressure/head (m) - Water density (367 = 3600 (s/h) ÷ 9.81 (m/s²)) - Pumping plant efficiency (%) ■ Average daily hours (kWh): (Equation (8)) - Overall seasonal energy demand (kWh) - Crop duration (days) - Pump power (kW) ■ Energy demand per day (kWh): (Equation (9)) - Peak power demand (kW) - Maximum daily pumping hours 	Landscape irrigation (LI)

The energy impact calculation method followed the MFCS GHG operational boundaries (Section 2.3) set by TCR [42] in line with the WRI/WBCSD [50] GHG Protocol Corporate standard and ISO 14064 Standard [57,58] with respect to GHG direct and indirect emissions (Scope 2 and Scope 3).

2.4.1. Scope Two

To calculate the electrical consumption (kWh/month), Equation (1) was used for the water feature (WF) system and Equation (2) for the landscape irrigation (LI) system.

$$\text{WF System Energy demand (kWh/month)} = \text{number of days in a month} \times \text{kWh/day energy consumed} \quad (1)$$

$$\text{LI System Energy demand (kWh/month)} = \text{number of days in a month} \times \text{kWh/day energy consumed} \quad (2)$$

Calculations (1) and (2) are based on Equations (1)–(5) and (6)–(9) results respectively [6,51], which were reviewed by the MFCS building services engineer. The energy intensity (kWh/m³) of the WF system can be calculated using Equations (3) and (4) for the LI system.

$$\text{WF System Energy intensity (kWh/m}^3\text{/month)} = \frac{\text{Equation (1) results}}{\text{Total water consumption (m}^3\text{)}} \quad (3)$$

$$\text{LI System Energy intensity (kWh/m}^3\text{/month)} = \frac{\text{Equation (2) results}}{\text{Total water consumption (m}^3\text{)}} \quad (4)$$

The total energy demand (kWh/month) for the MFCS water system, WF and LI combined, will be the addition of Equations (1) and (2) as per Equation (5).

The MFCS WF and LI water system energy demand in kWh per month will be the results of Equation (5).

$$\text{MFCS WF and LI Energy demand in kWh/month} = \text{Equation (1) results} + \text{Equation (2) results}, \quad (5)$$

and the total energy intensity (kWh/m³) of the MFCS water system (WF and LI combined) will be calculated using Equation (6).

$$\text{MFCS Energy Intensity (kWh/m}^3\text{/month)} = \frac{\text{Equation(5) results}}{\text{Total water consumption (m}^3\text{)}} \quad (6)$$

2.4.2. Scope Three

To calculate the energy demand of the desalinated water used at the MFCS for the WFs system and the LI system (kWh/month), Equation (7) will be used based on 15.40 kWh/m³ [20] for the desalinated water extraction and diversion energy intensity.

$$\text{Energy demand (kWh/month)} = (\text{m}^3 \text{ desalinated water used/month}) \times (15.40 \text{ kWh/m}^3), \quad (7)$$

The energy demand for the extraction, diversion, and treatment of the non-potable water is set to 0 kWh/month (Scope 3) because the condensate water, the reverse osmosis reject water (RORW), and the fire sprinkler pump test water are generated regardless of recycling. The energy demand for its treatment and distribution is included in the water system electrical consumption (Scope 2).

2.4.3. Scope Two and Three Combined

The energy intensity (kWh/m³) for the WF and LI system, using 38% desalinated water and 62% non-potable water including the water system electrical consumption will be calculated using Equations (8) and (9), respectively.

$$\text{WF Energy Intensity (kWh/m}^3) = \frac{\text{Equation (7) results} + \text{Equation (1) results}}{\text{Total water consumption (m}^3)} \quad (8)$$

$$\text{LI Energy Intensity (kWh/m}^3) = \frac{\text{Equation (7) results} + \text{Equation (2) results}}{\text{Total water consumption (m}^3)} \quad (9)$$

The total energy intensity (kWh/m³) for the combined WF and LI system using 38% desalinated water and 62% non-potable water including water system electrical consumption will be calculated using Equation (10).

$$\text{MFCS Energy Intensity (kWh/m}^3) = \frac{\text{Equation (7) results} + \text{Equation (5) results}}{\text{Total water consumption (m}^3)} \quad (10)$$

These calculations consider the relationship between the total energy consumed against the total water consumed. The GHG emissions calculation in Scope 2 is based on the results from Equations (1) and (2). The GHG emissions for Scope 3 will be based on 38% desalinated water and 62% non-potable consumption in m³ as per the 2017 EMCS water records.

2.5. MFCS GHG Impact Calculation Method

The steps of the onsite non-potable water use cycle were developed by the author for each water type proposed for reuse. Each m³ extracted, diverted, conveyed, treated, and distributed has an energy expenditure (kWh/m³) and a GHG effect expenditure (tCO_{2e}/m³) [69]. The energy intensity for Scopes 2 and 3 will be converted to GHG using the baseline emission factor from [70]. The results will be a GHG metric for onsite non-potable water use by water type as per Equation (11) [35].

$$\text{Water Energy GHG intensity (kgCO}_{2e}) = \frac{\text{Total GHG (kgCO}_{2e})}{\text{Total water consumption (m}^3)} \times 1000 \quad (11)$$

First, calculation-based methodologies [42] will be used to quantify Scope 2 emissions (onsite pumps and treatment systems power consumption used to move and treat both desalinated water and non-potable water sources) based on activity data and the EAD [70] and IEA [31] emission factors,

which are directly given in CO_{2e} equivalent units. This means that the global warming potential (GWP) is equal to 1 CO_{2e} [57,58,71] as Equation (12).

$$\text{GHG emissions} = \sum_{\text{gas}} (\text{emissions}_{\text{gas}} \times \text{GWP}_{\text{gas}}) \quad (12)$$

Second, Scope 3 emissions will be calculated based on the Water–Energy GHG Guidance [35] and WRI/WBCSD [50] protocol. Electricity consumption associated with the production of desalinated water falls under Scope 3 because the fuel and energy related activities to produce this water type are not included in Scopes 1 and 2 [35,50]. Whereas, non-potable water supply such as RORW, food waste effluent wastewater, A/C condensate water, and fire sprinkler pump test water fall within Scope 3 as energy:water decarbonization, which is currently not defined by the GHG protocol standards [50,56] nor the GRP standards [35,42].

Calculation Process for Scope Two and Scope Three

For Scope 2, the formula for calculating the total GHG emissions of the non-potable water system for electricity is calculated by using Equation (13) [42,57,58], where the GHG emission factor (EF) from electricity generation in the UAE is 0.64337 kgCO_{2e}/kWh [31]. This greenhouse gas emission factor (GHGEF) excludes transmission and distribution losses between the power station and the end-user (ibid.)

$$\text{Electricity generation (kWh)} \times \text{GHG}_{\text{EF}} (\text{IEA, 2016}) (\text{tCO}_{2e}/\text{kWh}), \quad (13)$$

The electricity consumption in kWh is the power demand of the water system for all scenarios (MFCS, Baseline Case (S2), Proposed Research Project (PRP S3) because power will be needed to distribute the water to the point of consumption regardless of the water type used. The only exception is the ultraviolet (UV) disinfection treatment system which was excluded for scenario two (Baseline Case S2). The kWh/month will be the result of Equation (5).

For Scope 3, the GHG emissions for desalinated water is calculated by using Equation (14) [70] where the GHGEF for water consumption in AD is 0.0151 tCO_{2e}/m³ [69]. The GHG water:energy decarbonization is calculated by using Equation (15) [50] with the same GHGEF [70].

$$\text{Desalinated Water Consumption (m}^3\text{)} \times \text{GHG}_{\text{EF}} (\text{EAD, 2012}) (\text{tCO}_{2e}/\text{m}^3), \quad (14)$$

$$\text{Non-Potable Water Consumption (m}^3\text{)} \times \text{GHG}_{\text{EF}} (\text{EAD, 2012}) (\text{tCO}_{2e}/\text{m}^3), \quad (15)$$

2.6. MFCS Calculation Evaluation against Alternative Scenarios (S2 and PRP S3)

The MFCS water system uses 32% makeup desalinated water and 68% condensate water. To evaluate the impact on energy use and costs and the associated GHG emissions, the latter was compared to a baseline (Scenario 2) and to the propose research project (Scenario 3). The parameters of the MFCS and the alternative scenarios are summarized in Table 5.

Table 5. MFCS parameters against alternative scenarios (S2 and PRP S3).

	MFCS Scenario 1	Baseline Case Scenario 2 (S2)	Proposed Research Project Scenario 3 (PRP S3)
Initial investment (design and construction)	Water tanks, piping, flow meters, pumps, EMCS connection, UV disinfection and Ozone treatment systems.	Pumps, EMCS connection, and ozone disinfection treatment system.	Water tanks, piping, flow meters, pumps, EMCS connection, UV disinfection, and ozone treatment systems.
Annual landscape maintenance	<ul style="list-style-type: none"> ■ Soil conditioner B. 		<ul style="list-style-type: none"> ■ Soil conditioner B.
Annual water system maintenance	<ul style="list-style-type: none"> ■ Chlorine; laboratory analysis; tank disinfection. 	<ul style="list-style-type: none"> ■ Chlorine; ■ Laboratory analysis. 	<ul style="list-style-type: none"> ■ Chlorine; ■ Laboratory analysis; ■ Tank disinfection; ■ Chemigation.
Annual water type consumption	<ul style="list-style-type: none"> ■ Combined desalinated and non-potable water sources: WFs: 52% condensate water; 48% makeup water; LI: 72% condensate water; 28% makeup water. 	100% desalinated water consumption: <ul style="list-style-type: none"> ■ WF water demand is based on the 2017 EMCS records. ■ LI water demand is based on ADM [53] standard with no soil improvement. 	100% mixed non-potable water supply (condensate, fire sprinkler pump test water, RO reject water): <ul style="list-style-type: none"> ■ WFs demand is based on Seguela et al.'s [28] water demand calculation. ■ LI water demand is based on demand after soil improvement.
Additional parameters	<ul style="list-style-type: none"> ■ Soil improvement partially implemented; 13 hours (h) run time irrigation controller per day, 10.67 h for the WF system. 	<ul style="list-style-type: none"> ■ 13 h run time irrigation controller per day; ■ 10.67 h for the WF system. 	<ul style="list-style-type: none"> ■ Soil improvement 100% implemented; ■ 8 h run time irrigation controller per day; ■ 6 h for the WF system; ■ Leaks detected and repaired; ■ Hydraulic review recommendations 100% implemented; ■ 365 days/year operations for the RORW pump and 1 day operation per year for the fire sprinkler pump test water.
For all three scenarios			
Annual electrical consumption	Based on Seguela et al. [51] calculation method; except for scope three desalinated water use based on 15.40 kWh/m ³ [20]		
Annual energy tariff	AED 0.21/kWh, equivalent to USD 0.057/kWh [22]		
Annual water tariff	The calculation will ignore the water and energy subsidies AED 8.23/m ³ equivalent to USD 2.24/m ³ [22]		
Life span of the project (assumption)	20 years		
UAE interest rate in January 2018 (Central Bank of the United Arab Emirates [72]).	4.8%		
UAE inflation rate in January 2018 [73].	2.25%		

The three scenarios (MFCS, S2, PRP S3) include the secondary treatment system energy demand to regulate the pH, and to prevent corrosion of the system if the desalinated or non-potable water source is acidic [74]. The three case scenarios, summarized in Table 5, provides the energy intensity and associated GHG impact for each segment of the water cycle onsite during operations as illustrated in Figure A1 in Appendix A. Hence, the calculation will include the energy intensity for extracting and diverting, storing, conveying, treating, and distributing water onsite in line with Scope 2 of the GRP [42] and ISO 14064 part two [58]. Plus, it will include the energy intensity for producing both desalinated and non-potable water in line with Scope 3 of the GRP [42], the Greenhouse Gas Protocol [50], and ISO 14064 [57,58], expressed in kWh/m³. The GHG emissions will be calculated on this basis.

2.7. MFCS 2017 EMCS Records

The total GHG emissions and decarbonization can be calculated by deducting the Equation (15) results from the results from Equations (13) and (14), as per Equation (16). Equation (14) will account for

the portion of desalinated makeup water consumed and Equation (15) for the portion of non-potable water consumed. The GHG emissions account for both Scopes 2 and 3.

$$\begin{aligned} \text{Total GHG emissions or decarbonization} = \\ [\text{Equation (13) results} + \text{Equation (14) results}] - \text{Equation (15) results} \end{aligned} \quad (16)$$

2.7.1. Baseline Case Scenario Two (S2)

The total GHG emissions and decarbonization can be calculated by adding the Equation (13) results to the Equation (14) results as per Equation (17).

$$\text{Total GHG emissions} = \text{Equation (13) results} + \text{Equation (14) results} \quad (17)$$

2.7.2. Proposed Research Project Scenario Three (PRP S3)

The total GHG emissions and decarbonization can be calculated by deducting the Equation (13) results from the Equation (15) results as per Equation (18).

$$\text{Total GHG decarbonization} = \text{Equation (13) results} - \text{Equation (15) results} \quad (18)$$

Table A2 in Appendix A provides a summary of the water energy GHG intensity calculation methodology for the MFCS. It is assumed that the 15.40 kWh/m³ [20] energy intensity rate for desalinating water and its associated emission factor [70] includes production, transmission, distribution and supply, and excludes the 8% water real loss provided by the Regulation Supervision Bureau (RSB) [75].

2.8. MFCS Financial Impact Calculation Method

Discounted Cash Flow Method Analysis

The primary criterion for assessing the effectiveness of energy conservation investments is the minimization of life cycle costs [76]. For a project to be considered as life-cycle cost (LCC) effective, it must have a net-present value (NPV) greater than or equal to zero, or an internal rate of return greater than the estimated discount rate [77]. Equally, the decision rule can be the choice of a scenario with the lowest LCC as per DeYong [78] in Capehart et al. [76]. For energy related projects, an LCC study should include the consideration of costs for at least the design, initial construction, energy and utilities, operations and maintenance, repairs, replacement, and salvage [79]. As the MFCS and the two alternative case scenarios do not consider, for instance, the energy for chemical production, they do not qualify as a fully completed LCC analysis. The MFCS and the two alternative case scenarios include the total cost of purchasing and operating the potable and non-potable water system over their assumed lifespan, excluding repairs, replacement and salvage and thus have been analyzed with a discounted cash flow method analysis.

The simple payback period (SPP) determines the number of years required to recover the initial investment through the project (MFCS, S2, and PRP3) return and is calculated following Equation (19) [79].

$$\text{SPP} = (\text{Initial cost})/(\text{Annual savings}) \quad (19)$$

The SPP methodology does not consider the time value of money, Capehart et al. [76] recommend using a combination of methods that include values such as the discounted cash flow method. The net present value or present worth (PW) can be used as a combination method with SPP [78]. NPV converts future cash flows by using a given discount rate and is used to convert future saving cash flows of the MFCS non-potable water system back to the present, which is then compared to the cost of the two alternative scenarios. If the NPV is positive, the investment is acceptable [80]. The NPV of the MFCS and the two alternative scenarios (S2 and PRP S3) can be calculated using a minimum attractive

rate of return (MARR) or discount rate estimated by the Equation (20) mathematical relationship below [78], based on the UAE real interest and inflation rates where i is the market interest rate; f is the inflation rate; and j is the real interest rate.

$$i = f + j + f \times j \quad (20)$$

Equation (21) (ibid., p. 141) can be used to find the present worth (P) of the MFCS against Scenarios 2 and 3 where i is the interest percentage and A is the initial investment for n years or life span of the project (Equation (21)).

$$P = A (1 + i^n) \quad (21)$$

The reciprocal relationship between P and A is symbolized by the factor $(P/A(i,n))$ and is called the uniform series, capital recovery factor [79]. The present worth factor $(1 + i^n)$ is extracted from the uniform series tables of $(P|A, i, n)$ in Capehart et al. [76] to estimate the annual savings of the MFCS against the two alternative scenarios over 20 years.

The results are then generated and compared by using Equations (22) and (23) for the MFCS and the two-alternative scenarios.

$$\text{NPV} = \text{initial cost} - \text{PW of water savings } [P = A (1 + i^n)] + \text{PW of annual costs } [P = A (1 + i^n)] \quad (22)$$

$$\text{Benefit/cost ratio (BC)} = \text{Equivalent costs/Equivalent costs} \quad (23)$$

where the benefits are the annual savings and the equivalent costs are the maintenance in addition to the energy and water costs. When the BC is greater than 1, the project is deemed economically attractive [78]. The total cost will include the estimated costs of installing and operating a system (including energy and water costs, and maintenance) as per the MFCS operation mode (use of non-potable water and makeup potable water) against a potable water system (S2) and a non-potable water system (PRP S3).

3. Anticipated Results

Discussing the detailed results is not within the scope of this paper. However, a summary is given of the anticipated results at the MFCS if a full implementation of the methods discussed above is undertaken: water system energy impact, the environmental impact, and the financial impact calculation.

3.1. MFCS Water System Energy Impact

The MFCS results establish the energy consumption calculation method for a water system using 38% desalinated makeup water and 62% treated non-potable water (LI and WF water consumption combined) as per the EMCS water consumption records (February 2017–January 2018). Seguela et al. [51] established the energy consumption based on a 4200 m³ average per month for the LI (2016 records). The water consumption was revised according to the EMCS records for 2017 where an 8783 m³/month average of condensate water and 4599 m³/month average of desalinated makeup water were used for the WFs and the LI. In addition, Seguela et al. [51] calculated the energy consumption for the LI based on one-hour operation per day. The landscape contractor updated the irrigation controller schedules in September 2017, which brings the run time for the irrigation to 13 h per day. Additionally, both the WF and the LI calculations excluded the water treatment systems' energy consumption. Thus, the energy calculation results have been revised since Seguela et al.'s [51] publication. The Forrest and Williams [61] calculation method for swimming pools, adapted here for the WFs, is based on the open and closed season (days and hours of operation), the power (kW) used per pump, and the water consumed. In addition to these, Seguela et al. [51] added the frequency of use in percentage per pump to align to the MFCS' mode of operation. The WF pump power and flow rate (kW and m³/h) to satisfy the maximum anticipated operating conditions are variables that have been decided at the design stage by the mechanical engineer [54]. For the LI, the Kay and Hatcho [60] calculation

method considers the pumps' peak power demand (based on the existing pump size), the pumps' frequency of use, in addition to the quantity of water used. Thus, it is also possible to analyze and compare the MFCS results for LI with different variables such as various irrigation controller times and the various quantities of water used to observe changes in energy use. Seguela et al. [51] revised calculation considers the portion of water type consumed by the site for the 12-month period (February 2017 to January 2018).

3.2. MFCS Environmental Impact calculation

The LI and the WF system uses 38% desalination makeup water and 62% condensate water as recorded by the EMCS. The proposed MFCS calculation method will provide the environmental impact this mixed use of water will have on the environment in terms of GHG emission or decarbonization in $\text{kgCO}_2\text{e}/\text{m}^3$.

The environmental impact calculation includes decarbonization (Scope 3) from the condensate water used by the WF and the LI system less the GHG emissions emitted using makeup desalinated water; and less the GHG emissions emitted by the MFCS electrical system (Scope 2) of the treated non-potable water.

3.3. MFCS Financial Impact Calculation

As discussed in Section 2.8, the NPV converts the value of the future cash flow of the MFCS and the two alternative case scenarios (S2 and PRP S3) by using the estimated discount rate (16%) up to the value in 2018 [77]. The NPV converts the worth of the future cash flows for each scenario by using the estimated discount rate (16%) to the value in 2020, as the rate was determined in 2018.

This analysis does not take into consideration all cost variables such as the water treatment systems' spare parts or maintenance replacement (for example UV disinfection system cartridge filters) and MEP equipment salvage. However, the analysis provides an indication of the cost benefits of a system using a combination of non-potable water and desalinated water over 20 years (i.e., 2018–2038). Comparing the MFCS to a baseline case (Scenario 2, S2) and the proposed research project (Scenario 3, PRP S3) will help to evaluate the values of these three case scenarios.

4. Discussion

The contributions to knowledge and professional practice for building owners, engineers, facility managers, and other practitioners engaged in maintaining and managing building estates that use LI and WFs are discussed below. In addition, the limitations to the research are also discussed.

4.1. Contributions from the GHG Metric Methodology for Onsite Non-Potable Water Systems

Electricity consumption associated with water and wastewater operations are a major contributor to GHG emissions [35–39]. In addition, and this remains to the authors' knowledge in 2020, the energy intensity of non-potable water supply sources (other than desalination water) and decentralized water systems "are unknown and is a knowledge gap that requires further research" [36]. Moreover, the design of methodologies to account for these GHG emissions have not been transparently available [35]. Thus, another contribution to knowledge and professional practice is the design and development of a GHG metric to determine the environmental impact of reusing non-clinical and non-potable water sources onsite, compared with the use of potable desalinated water for LI and WF use. The authors developed a calculation methodology to determine the energy intensity of onsite generated non-potable water sources, compared with desalinated potable water for outdoor WFs and LI use, by applying this method to:

- First, a mixture of condensate water and desalinated water (MFCS scenario);
- Second, desalinated water (Baseline Scenario 2, S2);

- Third, a case for additional non-potable water sources used as makeup water to the main water source (condensate water) such as fire sprinkler pump test water and RORW (Scenario 3, PRP S3).

This methodology was developed as a result of the results of a GHG metric ($\text{kgCO}_2\text{e}/\text{m}^3$), which specifically includes the energy impact from outdoor water demand, water type supply, and onsite distribution systems to help evaluate water conservation strategies. The metric determines GHG emissions (–) or sinks (+) in water for outdoor use and is presented in Table A2 in Appendix A, where it can be used to evaluate the three case scenarios (MFCS, S2, and PRP S3). The use of 100% non-potable water sources combined with water demand control, and an efficient onsite distribution system can be a powerful asset for decarbonization.

4.2. Contributions and Target Audience

The original and significant contribution to change in professional practice and knowledge will be most useful to building and estate owners, facility managers, and landscape contractors, who are responsible for saving water for outdoor use, increasing non-potable water use against potable water, and minimizing costs and GHG emissions during operations. In addition, the contributions could form part of the design of a decentralized non-potable water system intended for existing and new building landscapes and WFs.

4.3. Research Limitations

4.3.1. Estimation of Cost and GHG Calculations

The reporting of GHG emissions implies the use of appropriate methodologies and the use of country-specific emission factors that are publicly available, and that have been published following a rigorous peer-reviewed process [42]. In the UAE, the accuracy of the GHG emissions inventory is uncertain for three reasons: (1) data access is a constraint; (2) the use of generic emission factors is potentially unsuitable; and (3) the processes associated with emissions is incompletely understood [16]. For instance, the available data format, which suits government planning purposes, does not necessarily address all information required by the IPCC [59] methodology [16]. Due to these limitations, future research could be undertaken to provide further evidence and thus meet the IPCC methodology.

4.3.2. Energy Calculations

The pumps' energy intensity calculated for the WFs and the LI water diversion, storage, conveyance, treatment, and distribution did not take into consideration the pumps standby mode and start-up [66,67]. This is because the energy consumption for pump start-up and standby mode, and the number of start-up operations per day were not known and would have required additional funding (not available to the authors) to contract the building engineer to undertake this work. In addition, it is not known if the energy intensity of the desalinated water production ($15.40 \text{ kWh}/\text{m}^3$) includes both of these factors.

4.4. Recommendations

The DEng change project has demonstrated that a water supply, specifically coming from a non-potable water source, can be used as a decarbonization strategy in Abu Dhabi, which could also be transferred to countries located in arid climates that have limited access to natural resources and depend on desalinated water.

The following recommendations from the authors are therefore to encourage the local authority to develop a sustainable water conservation and reuse (SWC) strategy, forming the basis for a water protocol including an assessment methodology to measure the impact of decentralized buildings' non-potable water systems GHG emissions and their financial viability with the design and development of a water:energy GHG metric in $\text{kgCO}_2\text{e}/\text{m}^3$, as summarized in Figure 7. This proposed calculation method, using equations [35,51,60–62,69,76–79] from the literature, fills the knowledge gap with regard

to assigning values of building water streams (Figure A1 in Appendix A) while accounting for the energy intensity of non-potable water supply sources for a decentralized water system.

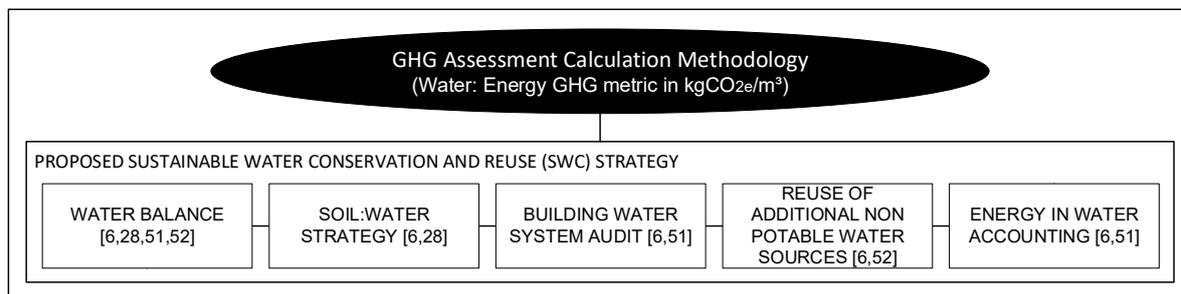


Figure 7. Summary of the Water Conservation Protocol for a decentralized system.

The findings for collecting water and energy data to produce the calculations can be summarized as follows:

- A water balance to allow for the comparison of an onsite system as opposed to the use of municipal desalinated potable water. The water consumption records are to be collected and analyzed daily via sub flow meters connected to the EMCS. Additionally, these water data are to be compared with water bills to cross check the accuracy of the collected data and establish cost savings. This action research benefit is to help provide an account for the effect of non-potable water on landscape for water efficiency and water deficit offset feasibility analysis [6,28,51,52].
- Establishing an irrigation water budget to create a baseline for LI irrigation demand against a suitable irrigation rate and irrigation controller schedule [6,28].
- Conducting water and soil quality tests and building water system audits for implementation of a soil water strategy that could reduce substantial water consumption [6,28].
- In addition to air conditioning condensate water, account for additional non potable water supply suitable for reuse as makeup water by conducting a building water audit [6,51,52].
- Accounting for the building operational boundaries for equipment electrical consumption serving the water systems [6,51].

These recommendations apply to the design and construction industry as well as to the building operations and maintenance industry who are willing to improve their outdoor water conservation programs to save on cost and minimize environmental impact.

5. Conclusions

The case study presented is a medical facility in AD and the existing treated non-potable water system for LI and WF use has been discussed. The MFCS, which uses 62% condensate water and 38% desalinated makeup water on average for both the LI and the WF system, was compared to a baseline and to the proposed research project.

The findings have led to a proposed sustainable water strategy, which could be legislated and mandated by the competent authority for regional medical facilities as part of a water conservation protocol with a water:energy GHG Metric ($\text{kgCO}_2\text{e}/\text{m}^3$), to assess the water systems of building estates that serve outdoor LI and WFs.

The proposed calculation method will contribute to developing the energy and financial impact from an outdoor water demand, the supply of the water type, and onsite distribution systems in terms of GHG emissions or sinks in water for outdoor use, and provide an indication of the cost benefits of a system using a combination of non-potable water and potable desalinated water.

The next steps are to publish the anticipated results of the three case scenarios, which are being developed for another paper.

Author Contributions: Conceptualization, G.S.; Methodology, G.S.; Software, G.S.; Formal analysis, G.S.; Investigation, G.S.; Resources, G.S.; Writing—original draft preparation, G.S.; Writing—reviewing and editing in all sections; Supervision J.R.L.; and G.K. All authors have read and agreed to the published version of the manuscript.

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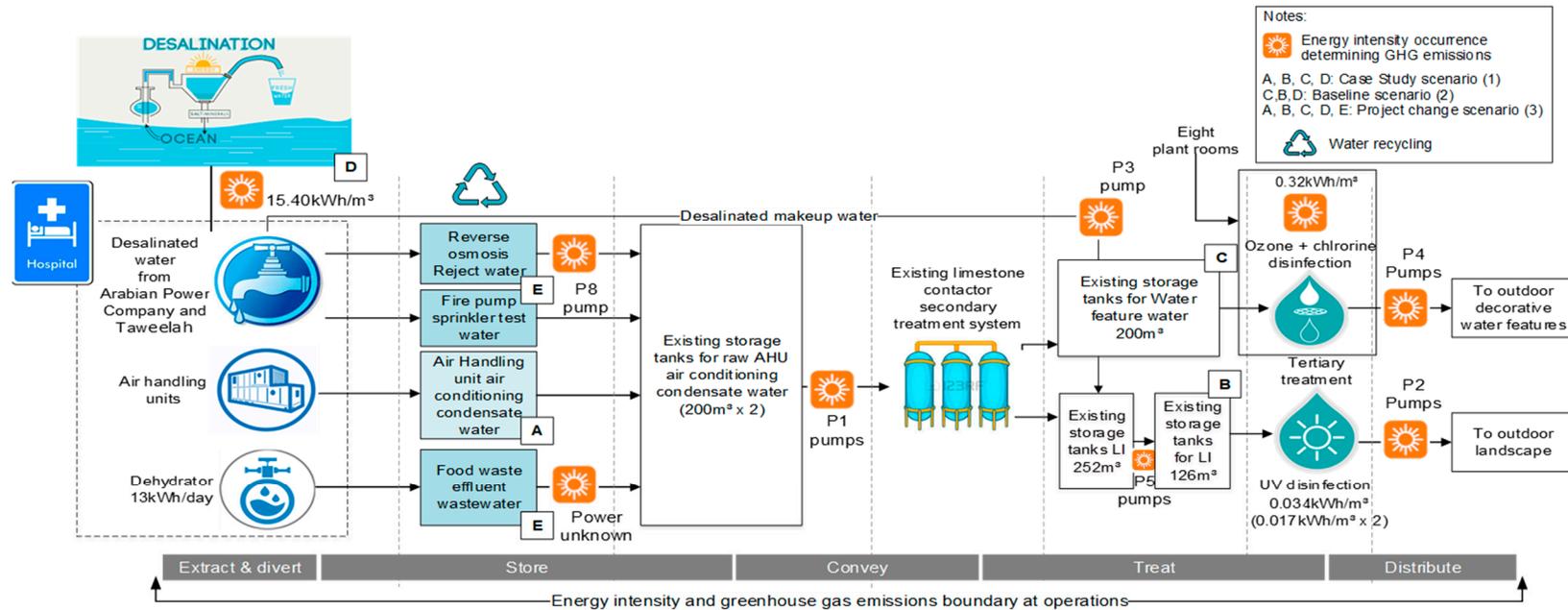
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Conflicts of Interest: The authors declare no conflict of interest.

Abbreviations

AC CW	Air Conditioning condensate water
AD	Abu Dhabi
ADM	Abu Dhabi Municipality
AED	Emirati Dirham
D.Eng	Doctorate in Engineering
EAD	Abu Dhabi- Environment Agency
EMCS	Energy Monitoring and Control System
GHG	Greenhouse gas
IPCC	Intergovernmental Panel on Climate Change
LI	Landscape Irrigation
MED	Multi Effect Distillers
MFCS	Medical Facility Case Study
MSF	Multistage flash
RO	Reverse Osmosis
S2	Baseline case scenario 2
PRP S3	Proposed research project Scenario 3
TCR	The Climate Registry
TSE	Treated Sewage Effluent
UAE	United Arab Emirates
WF	Water feature
WFs	Water features

Appendix A. Methodology



Notes on water treatment systems:

1. 0.32 kWh/m³ accounts for ozone generation, drying of the feed gas cooling of the ozone generator, injection units and instrumentation control [55]
2. 0.017 kWh/m³ accounts for the production of radiation and heat [55,81].

It is assumed the same quantity of energy will be used by the cartridge filters unit.

Figure A1. MFCS, S2, and PRP S3 calculation boundaries. Figure A1 is linked to Table A1 and the MFCS non-potable water system configuration diagram in Seguela [6] and Seguela et al. [51].

Table A1. Updated MFCS main operation input summary [6].

Input Summary				Mean Average	
1. Physical characteristics					
Outdoor elements				WFs	LI
Area (m ²)				3289	36,310
2. Operational parameters					
Pumps (h/day)				11.7	13
Backwash period (No per month)—assumption				4	n/a
Backwash duration (mins)—assumption				15	n/a
Refill period (years)				0.5	n/a
3. Environmental Conditions					
Season (length) in days				351 (14 days for maintenance)	365 (2017); 366 (2016)
Rainfall (mm) average per month				3.80 mm (November to April); 0 mm (May to October); (SCAD, 2017)	
Evaporation (mm) average per month				215 mm (November to April); 0 mm (December to March); (SCAD, 2017)	
4. Existing Water System Components					
Pump Description	Pump Power (kW)	Pump Flow (m ³ /h)	Pump Usage per day (%)	WFs	LI
Number of pumps					
(P1) Pumps Set A	4	17	30	1	
(P1) Pumps Set B	11	64	10	1	
(P1) Pumps Set C	4	17	30	1	
(P1) Pumps Set D	11	64	10	1	
(P2) Pumps Set power	18.5	64	100	-	1
(P2) Pumps Set power	Not known	10	100	-	1
(P3) WE Pump Set	7.5	45.5	100	1	-
(P5) Pumps Set power	11	63.3	100	-	-
(P4) Ozone Filter Pump	5.5	Not known	100	5	-
(P4) Ozone Display Pump	30	Not known	100	4	-
(P4) Ozone Filter Pump	2.2	Not known	100	2	-
(P4) Ozone display Pump	37.5	Not known	100	1	-
(P4) Ozone display Pump	3.7	Not known	100	1	-
(P4) Ozone display Pump	11.2	Not known	100	1	-
Ozone Disinfection		0.31 kWh/m ³ [55]		40.15 kWh/day	-

Table A2. MFCS non-potable water use cycle segments adapted from The Climate Registry [42].

Water Product	Five Major Water Use Cycle Segments to Model GHG Emissions at Operations					GHG Protocol Scope [35,42,57,58]	Total GHG Emissions/Sinks in tCO _{2e}	Energy Demand in kWh Per Year	Energy Intensity in kWh/m ³	Volume of Water Used in m ³	GHG Metric for Onsite Non Potable Water Use in (kgCO _{2e} /m ³)
	1. Extract and Divert	2. Place into Storage	3. Conveyance	4. Treatment	5. Distribution						
Medical Facility Case Study (MFCS)											
Desalinated potable water use onsite as makeup water	These steps are included in the final emission factor generated by EAD [70]					3	Equation (14)	Equation (7)	15.40 [20]	Make up water used onsite monitored by EMCS records	Equation (11)
Air conditioning condensate water (A/C CW)	No emission other than scope 2 below					3	Equation (15)	Nil	Nil	Onsite generated and used and monitored by EMCS records	
38% makeup desalinated water and 62% condensate water (AC CW) for both WFs and LI use	Nil because the condensate water is generated regardless of condensate water recycling or not	Gravity fed into raw water storage tank	AC CW conveyed to treatment plant by pump (P1)- see Figure A1 in Appendix A	AC CW treated to secondary and tertiary treatment for WFs and LI reuse	AC CW distributed to point of delivery onsite to WFs and LI	2	Equation (13)	Equation (5)	Equation (6)	Included in scope 3 above	
Baseline Scenario 2 (S2)											
Desalinated potable water use onsite as makeup water	Included in scope 3 below	Pumped to storage. Refer to Figure A1 in Appendix A	Desalinated water conveyed to treatment plant by pump (P3)	Secondary and tertiary treatment for WFs only	Desalinated water distributed to point of delivery onsite to WFs and LI	2	Equation (13)	Equation (5)	Equation (6)	Make up water used onsite monitored by EMCS records	Equation (11)
Desalinated potable water use	These steps are included in the final emission factor generated by EAD [70]					3	Equation (14)	Equation (7)	15.40 [20]	Included in scope 2 above	
Proposed Research Project Scenario 3 (PRP S3)											
Reverse Osmosis Reject Water (RO RW)	Nil because the reject water is generated regardless of reject water recycling or not	Pumped to raw A/C CW storage tank. Assume a transfer pump consuming 0.11kWh/day (P8) Figure A1 and Table A1 in Appendix A.	Mixed with A/C CW in raw condensate water tanks (no extra power needed)			3	Equation (15)	Nil	Nil	Equation (4) in [6]	
						2	Equation (13)	Part of Equation (5) below	Part of Equation (6) below		
Food waste Effluent wastewater (FEW) [6]	Dehydrator power (13 kWh per day) [6]	Pumped to storage. Assume a small transfer pump (power unknown)	Mixed with A/C CW in raw condensate water tanks (no extra power needed) [6]			3	Equation (15)	Nil	Nil	Estimate (85%-95%) of food weight [6]	
						2	Equation (13)	Part of Equation (5) below	Part of Equation (6) below		
Air conditioning condensate water (A/C CW)	Nil because the condensate water is generated regardless of condensate water recycling or not	Gravity fed into raw water storage tank	AC CW conveyed to treatment plant by pump (P1) Figure A1 and Table A1 in Appendix A	AC CW treated to secondary and tertiary treatment for WFs and LI	AC CW distributed to point of delivery onsite for WFs and LI use	2	Equation (13)	Equation (5)	Equation (6)	Onsite generated used and monitored by EMCS records	Equation (11)
			No emission other than scope 2 above			3	Equation (15)	Nil	Nil	Onsite generated monitored by EMCS records	
Fire Sprinkler Pump Test Water (FSPTW)	Nil because the water is used for testing the fire pumps regardless of fire sprinkler pump test water recycling or not.	Conveyed to storage through existing pump	Mixed with A/C CW in raw condensate water tanks (no extra power needed)			3	Equation (15)	Nil	Nil	Equation (1) in [6] Equation (2) in [6] Equation (3) in [6]	

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