

*Electronic Supplementary Information for*

**Iridium(NHC)-Catalyzed Sustainable Transfer Hydrogenation of CO<sub>2</sub> and Inorganic Carbonates**

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## I. Experimental procedure

**General Procedure.** Commercially available reagents were received from Sigma Aldrich and TCI. Catalysts **1**, **1'**, **2**, **2'**, **3**, and **3'** were prepared as described in the literature.<sup>1</sup> Low resolution mass spectra were obtained with a magnetic sector-electric sector double focusing mass analyzer equipment. Gas chromatograph (GC) (YL6500 GC, YOUNGLIN) equipped with a column (60/80 Carboxen-1000, 1.5 ft.) was operated at an Ar carrier gas flow rate of 30 sccm. X-ray structure was obtained by Rigaku R-axis Rapid S diffractometer. pH was measured by pH meter (Starter 3100, Ohaus corporation) at 25 °C.

### Catalytic procedure of transfer hydrogenation of CO<sub>2</sub>.

CO<sub>2</sub> (5 bar), KOH (40 mmol), H<sub>2</sub>O (1.0 ml), catalysts (0.35 ppm based on the amount of iridium ion), and glycerol (21.1 mmol) were added into an autoclave. The mixture was heated at 200 °C for 20 h. Then, the reaction mixture was cooled down to ambient temperature, and diluted with H<sub>2</sub>O. The amount of formate and lactate (mmol) were calculated by <sup>1</sup>H NMR spectroscopy in D<sub>2</sub>O using isonicotinic acid as an internal standard. The reactions were run three times, and the average numbers of mmol were used. The ‘mmol’ of each product was divided by ‘mmol’ of catalysts to give TONs. The resulting TONs are divided by the reaction time (h) to afford TOFs.

### Catalytic procedure of transfer hydrogenation of inorganic carbonate.

Inorganic carbonate (K<sub>2</sub>CO<sub>3</sub>, KHCO<sub>3</sub>, and Na<sub>2</sub>CO<sub>3</sub>, 40 mmol), H<sub>2</sub>O (2.0 ml), catalysts (0.35 ppm based on the iridium ion concentration), and glycerol (42.3 mmol) were added into an autoclave. In case of Cs<sub>2</sub>CO<sub>3</sub>, H<sub>2</sub>O (3 ml) was used for stirring. The mixture was heated at 200 °C for 20 h. Then, the reaction mixture was cooled down to ambient temperature, and diluted with H<sub>2</sub>O. The amount of formate and lactate (mmol) were calculated by <sup>1</sup>H NMR spectroscopy in D<sub>2</sub>O using isonicotinic acid as an internal standard. The reactions were run three times, and the average numbers of mmol were used. The ‘mmol’ of each product was divided by mmol of catalysts to give TONs. The resulting TONs are divided by the reaction time (h) to afford TOFs.

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<sup>1</sup> Cheong, Y.-J.; Sung, K.; Kim, J.-A.; Kim, Y. K.; Jang, H.-Y. Highly efficient iridium-catalyzed production of hydrogen and lactate from glycerol: rapid hydrogen evolution by bimetallic iridium catalysts. *Eur. J. Inorg. Chem.* **2020**, 4064-4068.

## II. NMR spectra of carbonate

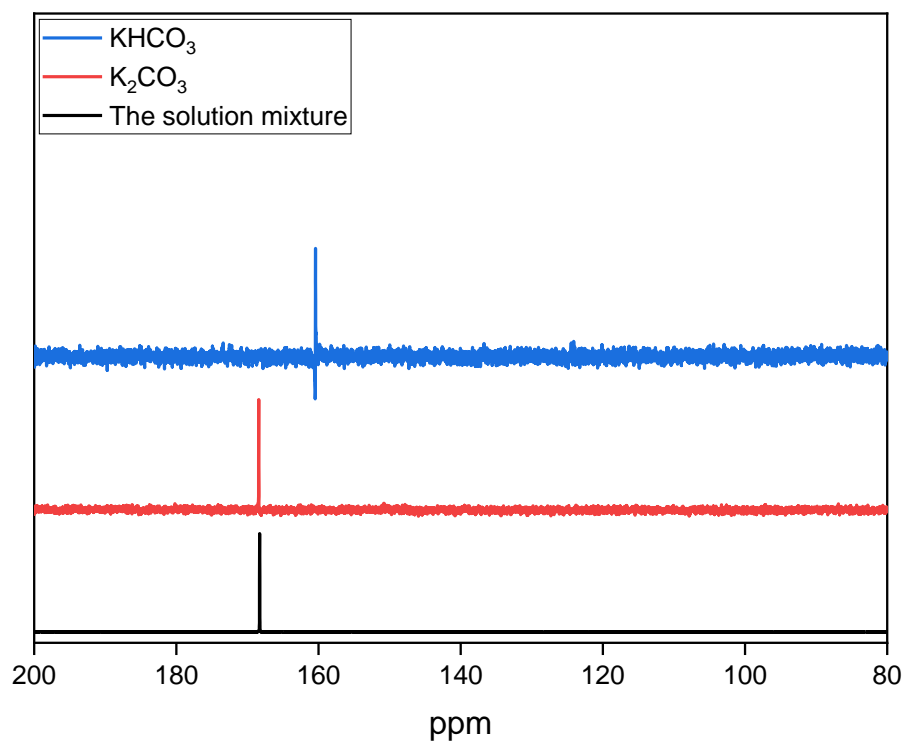


Figure S1.  $^{13}\text{C}$  NMR spectrum of the mixture of  $\text{CO}_2$  (5 bar) and KOH in glycerol (line black),  $\text{KHCO}_3$  (Line Blue) and  $\text{K}_2\text{CO}_3$  (Line Red).

### III. Residual gas analysis

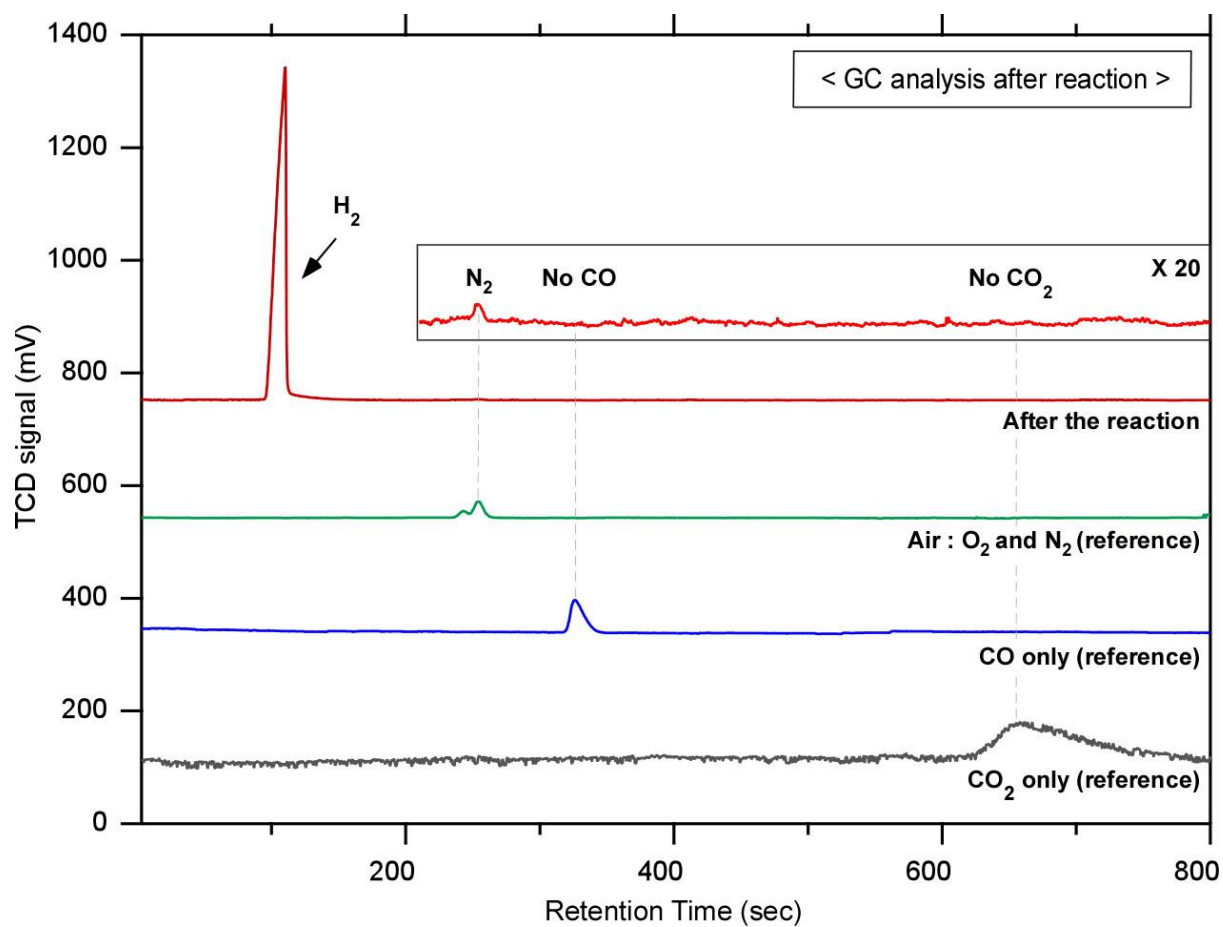
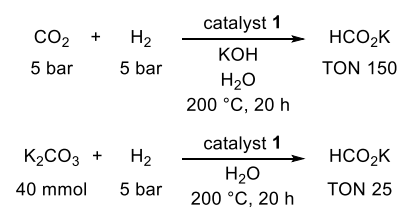


Figure S2. The GC (gas chromatography) spectrum of the gas obtained from the reaction of  $CO_2$  and glycerol (Table 1, entry 6). Only  $H_2$  generated by dehydrogenation of glycerol was identified and  $CO_2$  was not detected.

#### IV. Ir(NHC)-catalyzed hydrogenation of CO<sub>2</sub> and K<sub>2</sub>CO<sub>3</sub>



Scheme S1 The hydrogenation reaction of CO<sub>2</sub> and K<sub>2</sub>CO<sub>3</sub>. The pressure of H<sub>2</sub> (5 bar) was determined based on the observed H<sub>2</sub> pressure of transfer hydrogenation using glycerol. The reaction of CO<sub>2</sub> and H<sub>2</sub> was run with catalysts **1** (3.5×10<sup>-4</sup> mol%), and the hydrogenation reaction of K<sub>2</sub>CO<sub>3</sub> was run with catalysts **1** (7.5×10<sup>-4</sup> mol%).

## V. Transfer hydrogenation results including yields

Table S1. Transfer hydrogenation of CO<sub>2</sub> in glycerol

$$\text{CO}_2 + \text{HOCH}_2\text{CH(OH)CH}_2\text{OH} \xrightarrow[\text{temp, 20 h}]{\text{catalyst, KOH, H}_2\text{O}} \text{HCO}_2\text{K} + \text{H}_3\text{CCH(OH)CO}_2\text{K}$$

entry	catalyst (mol%)	CO <sub>2</sub> (bar)	KOH (mmol)	temp (°C)	formate (TON, TOF h <sup>-1</sup> )	lactate (TON, TOF h <sup>-1</sup> )	lactate (%)
1	<b>1</b> (3.5*10 <sup>-4</sup> )	5	20	180	3,360, 168	3,900, 195	1.3
2	<b>1</b> (3.5*10 <sup>-4</sup> )	5	40	180	1,490, 74.5	23,800, 1,190	7.9
3	<b>1</b> (3.5*10 <sup>-4</sup> )	5	40	200	15,800, 790	73,900, 3,700	24.5
4	<b>1</b> (3.5*10 <sup>-4</sup> )	1	40	200	2,110, 106	104,000, 5,200	34.6
5	<b>1</b> (3.5*10 <sup>-4</sup> )	10	40	200	12,700, 635	14,400, 720	4.7
6	<b>1</b> (3.5*10 <sup>-5</sup> )	5	40	200	200,000, <b>10,000</b>	875,000, <b>43,800</b>	29.0
7	<b>1'</b> (1.75*10 <sup>-5</sup> ) <sup>a</sup>	5	40	200	77,400, <b>3,870</b>	534,000, <b>26,700</b>	17.7
8	<b>2</b> (3.5*10 <sup>-5</sup> )	5	40	200	176,000, <b>8,800</b>	753,000, <b>37,700</b>	25.0
9	<b>2'</b> (1.75*10 <sup>-5</sup> ) <sup>a</sup>	5	40	200	70,400, <b>3,520</b>	548,000, <b>27,400</b>	16.2
10	<b>3</b> (3.5*10 <sup>-5</sup> )	5	40	200	174,000, <b>8,700</b>	683,000, <b>34,200</b>	22.8
11	<b>3'</b> (1.75*10 <sup>-5</sup> ) <sup>a</sup>	5	40	200	103,000, <b>5,150</b>	414,000, <b>20,700</b>	13.7
12	<b>1</b> (3.5*10 <sup>-5</sup> )	5	--	200	--	--	--
13	--	5	40	200	0.06 mmol	0.4 mmol	2.0

The mixture of catalysts, CO<sub>2</sub>, KOH, and H<sub>2</sub>O (1.0 ml) in glycerol (21.1 mmol) was heated at indicated temperature for 20 h. <sup>a</sup>Catalysts **1'**, **2'** and **3'** have two iridium ions in the molecule.

Table S2. Transfer hydrogenation of K<sub>2</sub>CO<sub>3</sub> in glycerol

$$\text{K}_2\text{CO}_3 + \text{HOCH}_2\text{CH(OH)CH}_2\text{OH} \xrightarrow[200\text{ }^\circ\text{C, 20 h}]{\text{catalyst}} \text{HCO}_2\text{K} + \text{H}_3\text{CCH(OH)CO}_2\text{K}$$

entry	catalyst (mol%)	formate (TON, TOF h <sup>-1</sup> )	formate (%)	lactate (TON, TOF h <sup>-1</sup> )	lactate (%)
1	<b>1</b> (3.50*10 <sup>-5</sup> )	203,000, <b>10,150</b>	7.6	414,000, <b>20,700</b>	15
2	<b>1'</b> (1.75*10 <sup>-5</sup> ) <sup>a</sup>	163,000, <b>8,150</b>	6.1	357,000, <b>17,850</b>	12
3	<b>2</b> (3.50*10 <sup>-5</sup> )	149,000, <b>7,450</b>	5.6	315,000, <b>15,800</b>	11
4	<b>2'</b> (1.75*10 <sup>-5</sup> ) <sup>a</sup>	178,000, <b>8,900</b>	6.7	342,000, <b>17,100</b>	12
5	<b>3</b> (3.50*10 <sup>-5</sup> )	164,000, <b>8,200</b>	6.1	326,000, <b>16,300</b>	12
6	<b>3'</b> (1.75*10 <sup>-5</sup> ) <sup>a</sup>	195,000, <b>9,750</b>	7.3	400,000, <b>20,000</b>	14

The mixture of catalysts, K<sub>2</sub>CO<sub>3</sub> (40 mmol), and glycerol (42.3 mmol) in H<sub>2</sub>O (2 mL) was heated at 200 °C for 20 h. <sup>a</sup>Catalysts **1'**, **2'** and **3'** have two iridium ions in the molecule.

$$\text{inorganic carbonate (40 mmol)} + \text{HOCH}_2\text{CH(OH)CH}_2\text{OH (42.3 mmol)} \xrightarrow[200\text{ }^\circ\text{C, 20 h}]{\text{catalyst 1 (3.50*10}^{-5}\text{ mol\%), H}_2\text{O (2.0 mL)}} \text{HCO}_2\text{M} + \text{H}_3\text{CCH(OH)CO}_2\text{M}$$

inorganic carbonate	pH	formate (TON, TOF h <sup>-1</sup> )	formate (%)	lactate (TON, TOF h <sup>-1</sup> )	lactate (%)
K <sub>2</sub> CO <sub>3</sub>	12.0	203,000, <b>10,150</b>	7.6	414,000, <b>20,700</b>	14.5
KHCO <sub>3</sub>	8.6	54,000, <b>2,700</b>	2.0	57,300, <b>2,870</b>	2.0
Na <sub>2</sub> CO <sub>3</sub>	11.3	14,500, <b>725</b>	0.5	53,100, <b>2,660</b>	1.9
Cs <sub>2</sub> CO <sub>3</sub> <sup>a</sup>	12.0	145,000, <b>7,250</b>	5.4	191,000, <b>9,600</b>	6.8

<sup>a</sup>H<sub>2</sub>O (3 mL) was added.

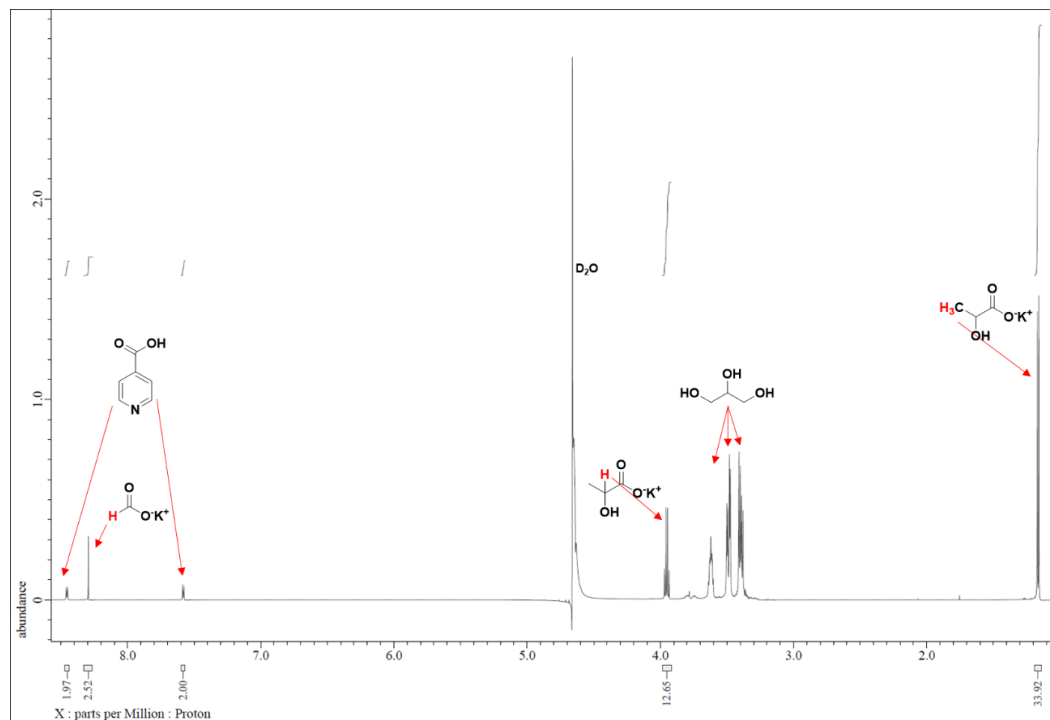
Scheme S2 Transfer hydrogenation of inorganic carbonate in glycerol

## VI. Representative $^1\text{H}$ spectra of the reaction mixtures

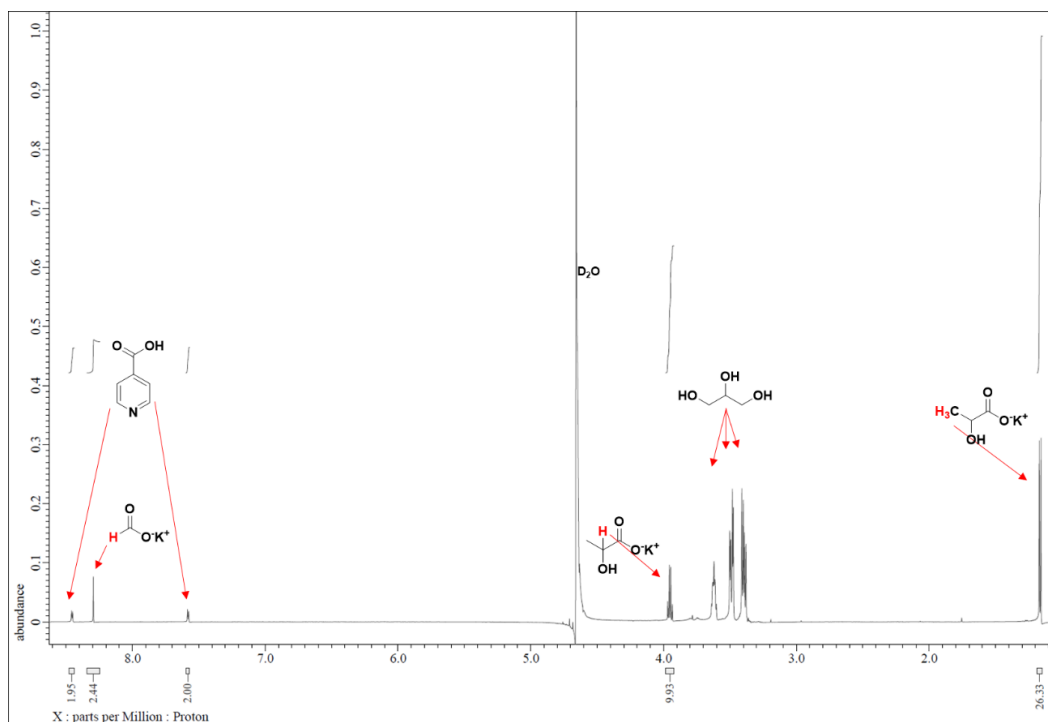
### Determination of yields of formate and lactate by $^1\text{H}$ NMR

The reaction mixture was diluted with  $\text{H}_2\text{O}$  (total volume is 40 ml). Isonicotinic acid (70 mg, 0.57 mmol) as an internal standard was added to the diluted solution. The 0.45 ml of the diluted solution and 0.15 ml of  $\text{D}_2\text{O}$  were mixed for NMR analysis. The moles of the products were calculated by integration values of the signature peak of each product based on moles of the internal standard.

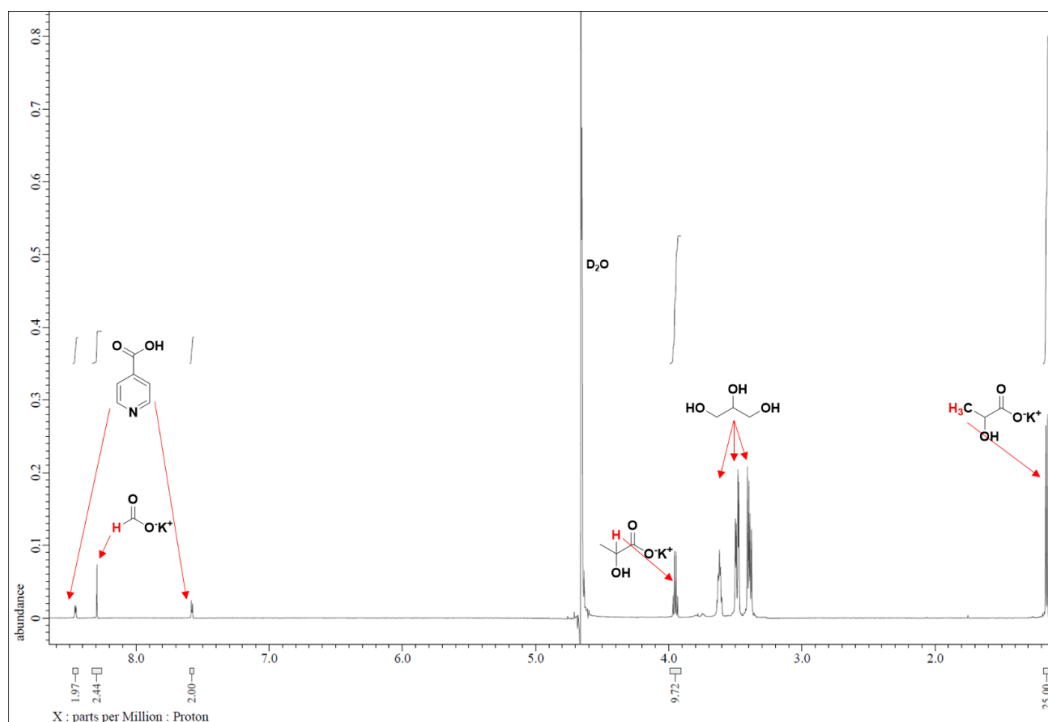
Entry 6 of Table 1 (formate  $\text{TON}_{\text{avg}} = 200,000$ , lactate  $\text{TON}_{\text{avg}} = 875,000$ )



Formate  $\text{TON} = 205,000$ , lactate  $\text{TON} = 1,030,000$



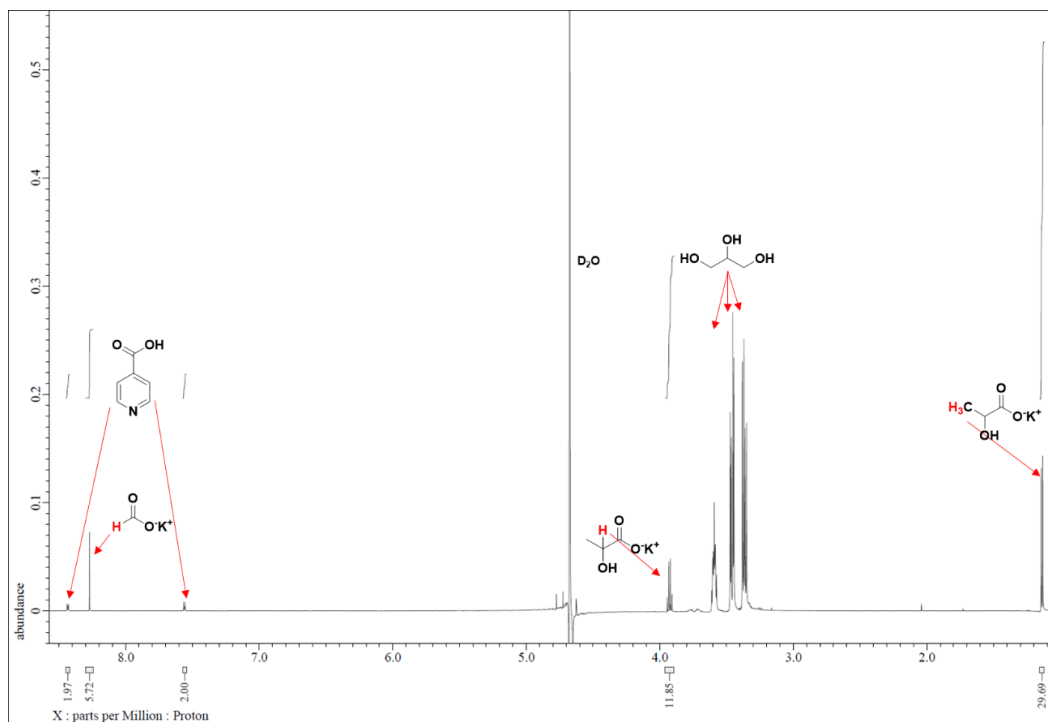
Formate TON = 198,000, lactate TON = 807,000



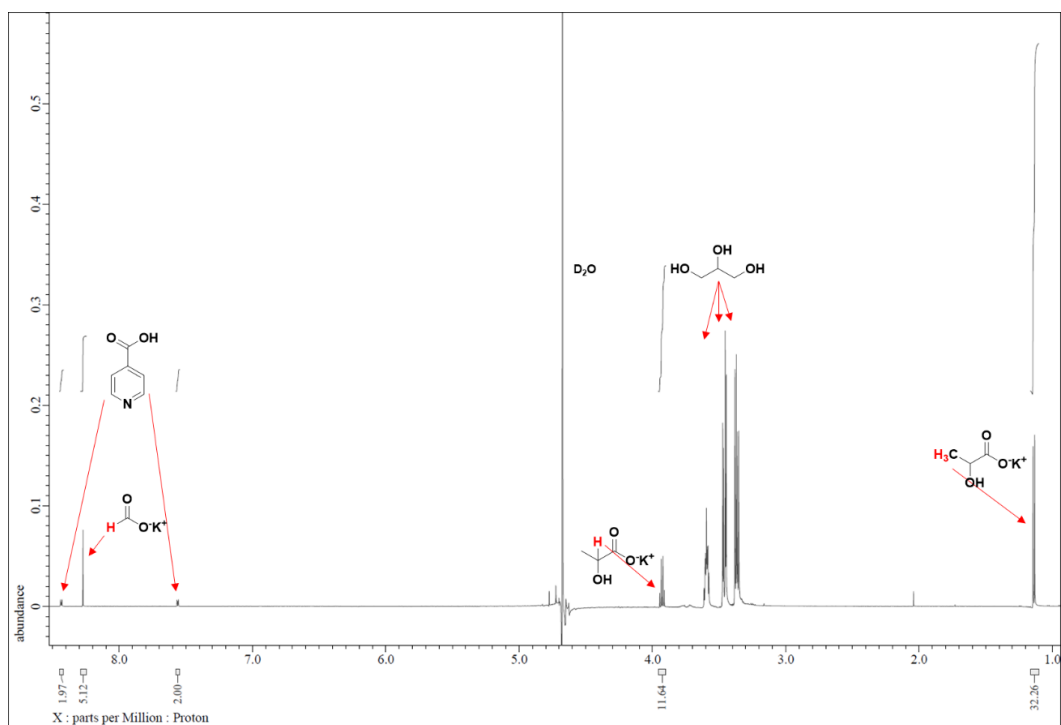
Formate TON = 198,000, lactate TON = 790,000



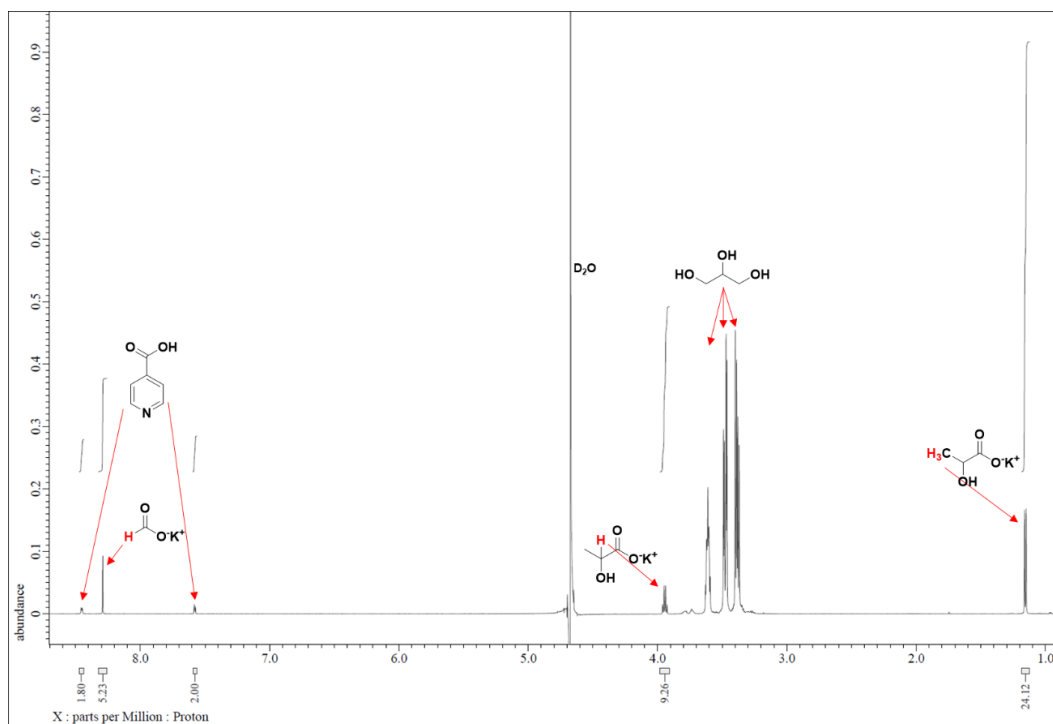
Entry 1 of Table 2 (formate  $\text{TON}_{\text{avg}} = 203,000$ , lactate  $\text{TON}_{\text{avg}} = 414,000$ )



Formate  $\text{TON} = 217,000$ , lactate  $\text{TON} = 449,000$

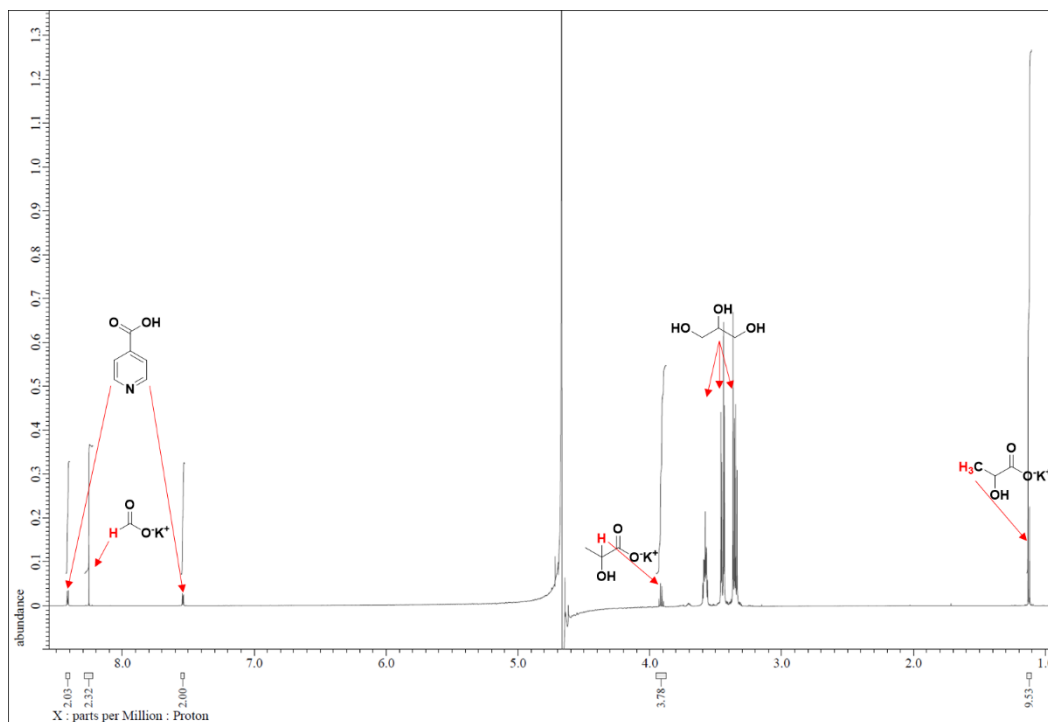


Formate  $\text{TON} = 194,000$ , lactate  $\text{TON} = 357,000$

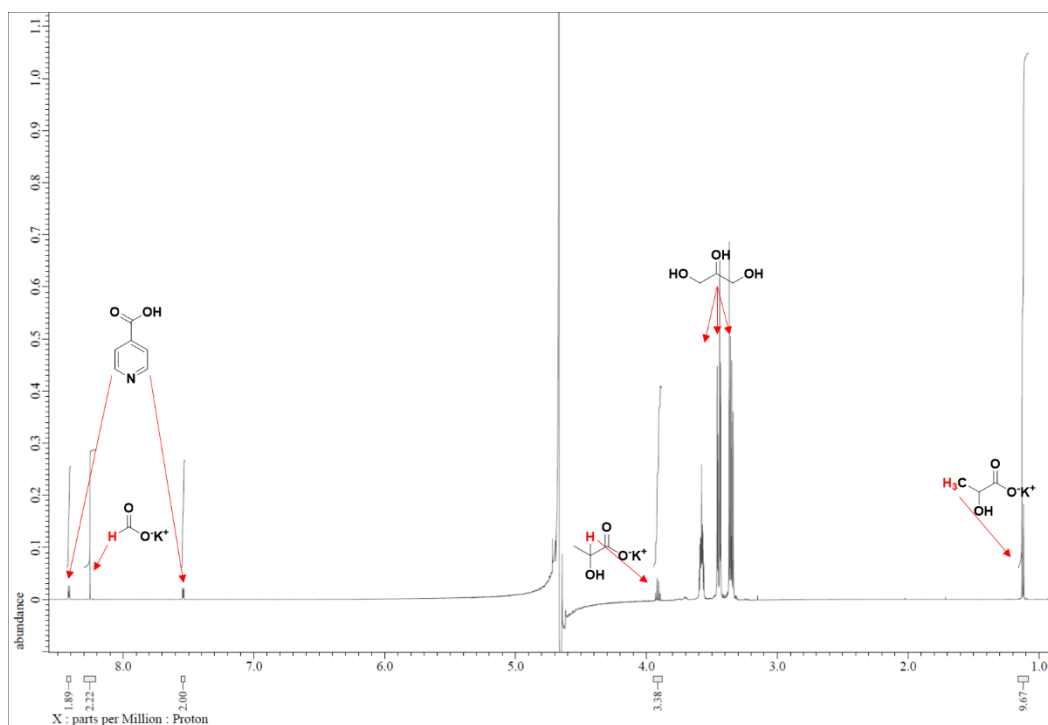


Formate TON = 198,000, lactate TON = 351,000

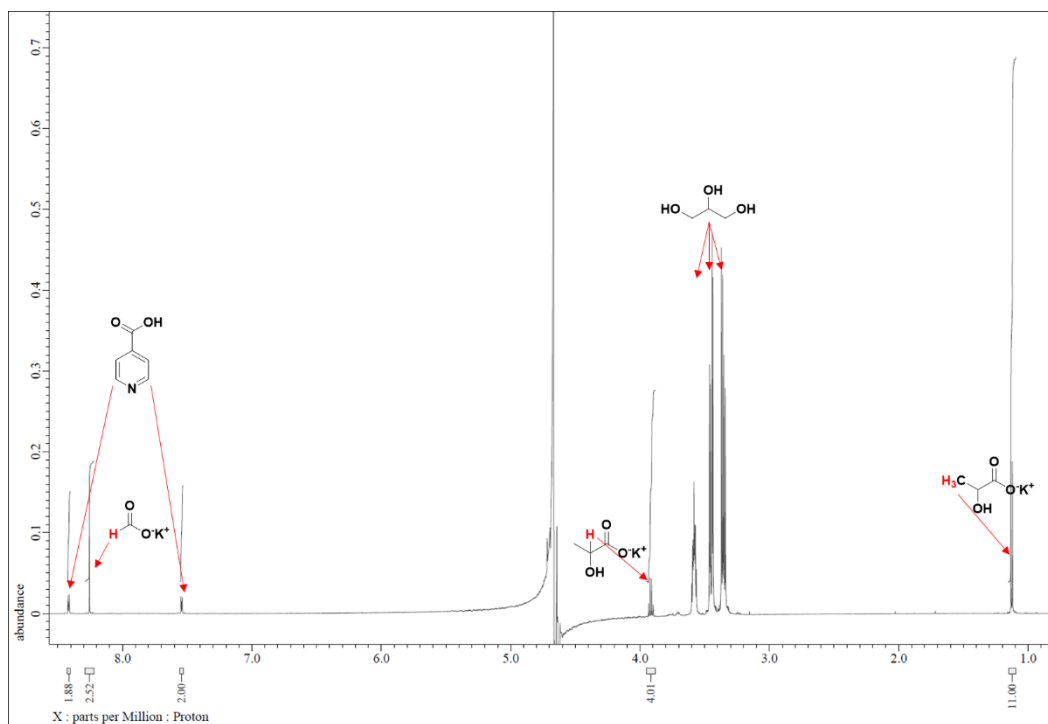
Entry 2 of Table 3 (formate  $\text{TON}_{\text{avg}} = 191,000$ , lactate  $\text{TON}_{\text{avg}} = 302,000$ )



Formate  $\text{TON} = 188,000$ , lactate  $\text{TON} = 307,000$



Formate  $\text{TON} = 180,000$ , lactate  $\text{TON} = 275,000$



Formate TON = 205,000, lactate TON = 326,000