

SUPPLEMENTARY MATERIAL

Table 1: Description of equations used for performance analysis of selected models to predict permeate flux in ultrafiltration processes

Equation	Description	Nomenclature	Models tested with this equation	Reference
$\mu = 8,8E-4 + 1,2E-5 Cb + 1,41E-7 Cb^2 + 8,7E-10 Cb^3$	Equation used for viscosity estimation	μ = Viscosity Cb = Bulk concentration	- Shear-Induced (Davis) - Dynamic (Song) - Kenden & Katchalsky - Wijmans <i>et al</i> - Hagen-Poiseuille - De & Bhattacharya - Ho & Zydny	[1]
$\frac{Cb}{Cbo} = \frac{Vo}{Vo-V}$	Equation used for estimations of feed concentration and permeate volume	Cb = Bulk concentration Cbo = Feed concentration V = Total permeate volume Vo = Initial volume	- Shear-Induced (Davis) - Dynamic (Song) - Hagen-Poiseuille - De & Bhattacharya	[2]
$D = \sum D_i Z_i$	Equation used for diffusivity estimation	D = Diffusivity D_i = Diffusivity of solid i Z_i = Weight fraction of suspended solid i i = Refers to each existing solid in the juice	- Shear-Induced (Davis) - Wijmans <i>et al</i> - De & Bhattacharya	[1]
$\rho = 999,7 + 5,1E-1 Cbo + 2,1E-3 Cbo^2$	Equation used for density estimation	ρ = Density Cbo = Feed concentration	- Shear-Induced (Davis) - Dynamic (Song) - Kenden & Katchalsky - Wijmans <i>et al</i> - Hagen-Poiseuille - De & Bhattacharya - Ho & Zydny - Mondal & De - Yee <i>et al</i>	[1]
$\epsilon = N \frac{\pi}{4} d_p^2$	Equation used for porosity estimation	ϵ = Porosity N = Pore density d_p = Pore diameter	- Wijmans <i>et al</i> - Hagen-Poiseuille - De & Bhattacharya	[3]
$J = \frac{ \Delta P - \Delta \pi }{\mu R_m}$	Equation used to determine osmotic pressure ($\Delta \pi$)	J = Flux of permeate ΔP = Transmembrane pressure μ = Viscosity R_m = Hydraulic resistance	- Kenden & Katchalsky - Wijmans <i>et al</i>	[4]

$Sh = \frac{kd}{D}$	Sherwood number used for estimation of the mass transfer coefficient	Sh = Sherwood number k = Mass transfer coefficient d = Diameter module D = Diffusivity	- Wijmans <i>et al</i> - De & Bhattacharya	[5]
$r_p = 180 \frac{(1-\varepsilon)^2}{a_p^2 \varepsilon^3}$	Carman-Kozeny' equation used to determine the specific resistance (r_p)	ε = Porosity of the concentration polarisation layer a_p = Average solute particle diameter	Wijmans <i>et al</i>	[6]
$R_p = r_p \delta_p$	Resistance of concentration polarisation layer (R_p)	r_p = Specific resistance δ_p = Thickness of concentration layer	- Wijmans <i>et al</i> - Ho & Zydny	[6]
$\delta_p = \frac{k}{D}$	Thickness of concentration layer (δ_p)	k = Mass transfer coefficient D = Diffusivity	- Wijmans <i>et al</i> - De & Bhattacharya	[3]
$\delta_* = \left(\frac{144 D L C_b^*}{\left(3 + \frac{1}{n}\right) U_o d^2 C_g^*} \right)^{1/3} x^{1/3}$	Equation used for estimation of the non-dimensional thickness of the concentration boundary layer (δ_*)	D = Effective diffusivity of the gel forming solutes L = Module lenght C_b^* = Non-dimensional bulk concentration n = Flow behavior index U_o = Maximum fluid velocity (centerline velocity) d = Module diameter C_g^* = Non-dimensional gel layer concentration X^* = x/L (x =distance along x-axis)	De & Bhattacharya	[7]
$Sh = 1,145 \left(3 + \frac{1}{n}\right)^{1/3} \left(Re^* Sc^* \frac{d}{L}\right)^{1/3} \left(e^{(-2/3)\alpha C_0(C_g^* - C_b^*)}\right)^{0.1}$	Sherwood number – Hollow fiber configuration	Re= Reynolds number Sc = Schmidt number C_b^* = Non-dimensional bulk concentration C_g^* = Non-dimensional gel layer concentration L = Module lenght d = Module diameter n = Flow behavior index	De & Bhattacharya	[7]
$Sh = 1,816 \left(Re^* Sc^* \frac{d}{L}\right)^{1/3} \left(e^{(-2/3)\alpha C_0(C_g^* - C_b^*)}\right)^{0.14} \left(\frac{C_g^*}{C_b^*}\right)^{1/3}$	Sherwood number – Tubular configuration	Re= Reynolds number Sc = Schmidt number C_b^* = Non-dimensional bulk concentration	De & Bhattacharya	[8]

		$C_g^* = \text{Non-dimensional gel layer concentration}$ $L = \text{Module length}$ $d = \text{Module diameter}$ $n = \text{Flow behavior index}$		
$R_g = \beta(1-\varepsilon_g)\rho_g H$	Gel layer resistance (R_g)	$\rho_g = \text{Gel layer density}$ $H = \text{Gel layer height}$ $\varepsilon_g = \text{Gel layer porosity}$ $\beta = \text{Specific gel resistance}$	De & Bhattacharya	[7]
$R_{CPB}^* = \exp(k_1 t) - 1$	Equation used for estimation of the non-dimensional complete pore blocking resistance (R_{CPB}^*)	$k_1 = \text{Complete pore blocking constant}$ $t = \text{Time}$	Mondal & De	[9]
$R_c^* = \frac{R_p}{R_m}$	Equation used for estimation of the non-dimensional cake resistance (R_c^*)	$R_p = \text{Resistance of concentration polarisation layer}$ $R_m = \text{Hydraulic resistance of membrane}$	Mondal & De	[9]

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